

BOTTOM ASH TRANSPORT SYSTEM EVALUATION CARDINAL GENERATING STATION

SL-018068

Prepared for

Buckeye Power, Inc.

October 9, 2023 Project No.: A13770.006 Issue: For Use, Rev. 0

Prepared By



55 East Monroe Street • Chicago, IL 60603 USA • 312-269-2000





BOTTOM ASH TRANSPORT SYSTEM EVALUATION

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CARDINAL UNIT 1, 2, & 3

BOTTOM ASH TRANSPORT SYSTEM EVALUATION <u>ISSUE SUMMARY AND APPROVAL PAGE</u>

This is to certify that this report has been prepared, reviewed and approved in accordance with Sargent & Lundy's Standard Operating Procedure SOP-0405, which is based on ANSI/ISO/ASSQC Q9001 Quality Management Systems.

Systems.			
<u>Rev.</u> 0	Purpose of Issue Issue for Use	<u>Date</u> 10/09/2023	Sections Affected All
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	David Wu		
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0	Ken Snell	David E. Nielson



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BOTTOM ASH TRANSPORT SYSTEM EVALUATION <u>CERTIFICATION PAGE</u>

I certify that this report was prepared by me or under my supervision and that I am a registered professional engineer under the laws of the State of Ohio.

I certify that I am familiar with the 40 CFR 423 regulation requirements and the Cardinal Generating Station Facility.

Certified By:		Date:	Date:	
	David E. Nielson (P.E. No. E-89402)			



Seal:







BOTTOM ASH TRANSPORT SYSTEM EVALUATION

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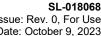
Appendices

- Bottom Ash Volume Calculation, 2020-03682 A.
- Bottom Ash System Rainfall Estimate, 2023-02951 B.
- Bottom Ash Purge Water Suspended Solids Estimate, 2023-02785 C.
- Chart on EPA-600/7-80-067, pg 17 D.

References

1. Email Correspondence from David Wu, 8:51am, October 3, 2023





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EXECUTIVE SUMMARY

The Cardinal Generating Station (Cardinal) consists of three steam electric generating units fueled by pulverized coal and is located near Brilliant, Ohio. All three units are equipped with a common bottom ash handling system which includes a CCR compliant retrofitted Bottom Ash Pond (the "Bottom Ash Pond"). The bottom ash handling system at each of the station's three units sluices bottom ash transport water (BATW) via several pipes to the Bottom Ash Pond. The primary purpose of the Bottom Ash Pond is for sedimentation of the bottom ash particles for removal and disposal. BATW is recycled to the station for reuse and for use in the plant's flue gas desulfurization (FGD) system. BATW from the Bottom Ash Pond may be discharged to the Low Volume Waste stream pond (LVW Pond), as needed, to obtain the target recirculation BATW quality. Sargent & Lundy (S&L) was retained to evaluate the Steam Electric Effluent Limitation Guideline (ELG) compliance strategy for the BATW stream in support of the facility's certification requirements in association with 40 CFR 423.19 (c).

Existing U.S. Environmental Protection Agency (EPA) ELG standards require that the total volume of bottom ash purge water discharged from the BATW system must be reduced or eliminated to the extent achievable using best management control measures (40 CFR 423.13(k)(2(i)(B)). The total volume of bottom ash purge water that may be discharged per day is determined on a case-by-case basis by the permitting authority; however, in no event shall such discharge exceed a 30-day rolling average of ten percent of the primary active wetted bottom ash system volume (the primary wetted volume or "PWV"). The primary wetted volume consists of bottom ash transport water from four (4) approved system categories, including discharge needed to maintain system water chemistry.

S&L reviewed Cardinal drawings and documents to prepare a calculation of the system's primary active wetted bottom ash system volume (primary wetted volume), evaluated the system influents and effluents, and developed a narrative description of the wastewater treatment system as it is anticipated to be configured to increase recirculation and reduce flows out of the systems. As part of this evaluation, S&L also evaluated the rainfall volume that can be managed by the system and water load under various operating conditions and how surge events affect the need for discharge. This evaluation is intended to support the technical information needed to fulfill Cardinal's initial certification requirements at 40 CFR 423.19(c) for facilities that discharge BATW pursuant to §423.13(k)(2)(i).

The total primary wetted volume of Cardinal's bottom ash water systems is summarized in Table ES-1,



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Table ES-1: Primary Wetted Volume

Bottom Ash System	Primary Wetted Volume (gallons)	Maximum Allowable Discharge (30-day rolling average gallons per day)
Combined Unit 1, 2, & 3	657,345	65,735

While Cardinal has a high recycle rate bottom ash transport system, it was never designed to function as a zerodischarge system. Modifications to the high recycle system have been implemented to minimize the need to purge water out of the system. These modifications include improvements to equipment, process controls, and operations focused on maximizing recirculation without impacting operations and maintenance.

Nevertheless, bottom ash purge water from two of the four approved categories of purge water are relevant to operation and maintenance of the Cardinal bottom ash system and support a daily discharge of up to 10% of the PWV on a 30-day rolling average basis. When the system modifications necessary to assure maximum recirculation are implemented, water chemistry becomes challenging and total suspended solids (TSS) and pH can be managed with purging to avoid impacts to system operation or maintenance. Occasionally, the ash sluicing lines must be maintained, during these maintenance events, Unit 1 & 2 boiler room sump pumps and Unit 3 ash pit pumps are routed to the LVW pond. Finally, on occasion maintenance may require complete drainage of the bottom ash system.

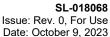
Based on an assessment of bottom ash purge water quantities, the projected BATW discharge rate on a %PWV 30day rolling average basis, calculated as the sum of the discharges for each bottom ash purge water category, is summarized in Table ES-2.

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Table ES-2: The 30-Day Rolling Average Discharge Volume as a Percent of Primary Active

Type of Discharge Event	Units 1, 2, and 3
Exceeding 10-year, 24-hour (or longer duration) storm event See 40 CFR $\S423.13(k)(2)(i)(A)(1)$	0%
Regular discharge needs to maintain water balance due to wastewater inflows See 40 CFR $\S423.13(k)(2)(i)(A)(2)$	0%
Regular discharge needs to maintain water chemistry See 40 CFR §423.13(k)(2)(i)(A)(3)	5.7%
Other infrequent maintenance events See 40 CFR §423.13(k)(2)(i)(A)(4)	8.6%
Total % of PWV of coincident maximum volume discharged per day	Up to 14.3%
Total % Discharge Volume Requested	10%

Operational strategies may be employed to reduce the total 30-day rolling average discharge lower than the sum of the individual contributors. The requested 10% total discharge volume reflects the implementation of these strategies.





INTRODUCTION 1.

The Cardinal Station is located near Brilliant, OH and has three (3) pulverized coal fired steam electric units with a combined net output of approximately 1,880 megawatts (MW). Units 1 and 2 are B&W opposed-firing boilers and have a gross capacity of 615 MW, each. Unit 3 is also a pulverized coal boiler and has a gross capacity of 650 MW. All units burn bituminous coal and are equipped with a common bottom ash handling system.

The Cardinal bottom ash system includes a CCR compliant retrofitted bottom ash pond (the "Bottom Ash Pond"). The bottom ash handling system at each of the station's three units sluices bottom ash transport water (BATW) via several pipes to the Bottom Ash Pond. The primary purpose of the Bottom Ash Pond is to settle out bottom ash particles for disposal. BATW is recycled to the station for reuse and for use in the plant's flue gas desulfurization (FGD) system. BATW from the Bottom Ash Pond may be discharged to the Low Volume Waste stream pond (LVW Pond), as needed, to obtain the target recirculation water quality and ultimately to the Ohio River. This discharge is regulated by the station's active National Pollutant Discharge Elimination System (NPDES) permit.

The U.S. Environmental Protection Agency (EPA) has promulgated Effluent Limitations Guidelines (ELG) and Standards for the Steam Electric Power Generating Point Source Category (40 CFR Part 423). The ELG standards have been revised and amended several times since they were first promulgated in 1974, including amendments published in 2015 and 2020. The 2015 amendments, published as a final rule in the Federal Register on November 3, 2015, imposed a zero-discharge limitation for all pollutants in BATW for any electric generating unit with a total nameplate capacity above 50 megawatts (MW), including the discharge of pollutants in BATW in a high recycle rate system (80 FR 67838, November 3, 2015). Technologies required to comply with the 2015 requirement generally required facilities to recycle most of their BATW or convert to dry ash handling systems.

On October 13, 2020, the EPA published a reconsidered ELG rule which revised the requirements for BATW and allowed the discharge of a limited amount of bottom ash purge water (85 FR 64650, October 13, 2020, the "2020 Reconsideration Rule"). Standards in the 2020 Reconsideration Rule, codified at 40 CFR 423.13(k)(2)(i)(A), allow the discharge of pollutants in bottom ash purge water from a properly installed, operated, and maintained bottom ash system under the following conditions:

(1) To maintain system water balance when precipitation-related inflows are generated from storm events exceeding a 10-year storm event of 24-hours or longer duration.



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- (2) To maintain system water balance when regular inflows from wastestreams other than bottom ash transport water exceed the ability of the bottom ash system to accept recycled water and segregating these other wastestreams is not feasible.
- (3) To maintain system water chemistry where installed equipment at the facility is unable to manage pH, corrosive substances, substances or conditions causing scaling, or fine particulates to below levels which impact system operation or maintenance.
- (4) To conduct maintenance not otherwise included above.

The total volume of the bottom ash purge water discharges listed above must be determined on a case-by-case basis but in no event shall the discharge exceed a 30-day rolling average of ten percent of the primary active wetted bottom ash system volume (primary wetted volume or "PWV").

This evaluation was prepared to assess the Cardinal BATW system operating conditions associated with the §423(k)(2)(i) discharge allowance, and to support the technical information needed to fulfill Cardinal's initial certification requirements at 40 CFR 423.19(c) for facilities that discharge BATW pursuant to §423.13(k)(2)(i).

SCOPE OF EVALUATION 2.

The scope of this evaluation includes discussion of the following pertinent elements of the plant design and operation based on the Cardinal Station drawings and documents provided by Cardinal Operating Company:

- The Primary Active Wetted Bottom Ash System Volume
- List of All Potential Discharges
- Narrative Description of the Wastewater Treatment Systems

3. THE PRIMARY ACTIVE WETTED BOTTOM ASH SYSTEM VOLUME

S&L developed a primary wetted volume calculation including all bottom ash and ash water handling equipment, piping, and trenches based on drawings provided by Cardinal Operating Company. Per 40 CFR 423.11(aa), the term "primary active wetted bottom ash system volume" is defined as the maximum volumetric capacity of bottom ash transport water in all non-redundant piping (including recirculation piping) and primary bottom ash collection and recirculation loop tanks (e.g., bins, troughs, clarifiers, and hoppers) of a wet bottom ash system, excluding the volumes of surface impoundments, secondary bottom ash system equipment (e.g., installed spares, redundancies, and maintenance tanks), and non-bottom ash transport systems that may direct process water to the bottom ash.

Based on the definition in 423.11(aa), the total calculated primary wetted volume at Cardinal was determined for each of the bottom ash systems. The primary wetted volume, and corresponding maximum allowable discharge is provided in Table 1. Please refer to Appendix A – Bottom Ash Volume Calculation for the calculation details, including material assumptions, information, and calculations used to determine the primary wetted bottom volume.

Table 1: Primary Wetted Volume

Bottom Ash System	Primary Wetted Volume (gallons)	Maximum Allowable Discharge (30-day rolling average gallons per day)
Combined Unit 1, 2, & 3	657,345	65,735

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LIST OF ALL POTENTIAL DISCHARGES 4.

Provided the Cardinal bottom ash systems are installed, operated, and maintained in accordance with industry standards, the following discharges are expected from the system:

- Discharges to Balance Precipitation-related Flows
 - 10-year / 24-hour storm or larger event collected in bottom ash system
- Discharges to Maintain System Water Chemistry
 - Water discharges to maintain bottom ash system pH
- Maintenance Related Discharges
 - Discharge to drain the system in a timely manner
 - Maintain bottom ash system water balance during ash sluice pipeline maintenance

Discharges to balance wastewater flow are not expected because other wastewater streams are not directed to the bottom ash system at Cardinal.

4.1 DISCHARGES TO BALANCE PRECIPITATION-RELATED INFLOWS

As part of this evaluation, S&L evaluated storms exceeding the 10-year 24-hour storm event, including longer durations to determine how such rainfall events affect the need to discharge purge water from the bottom ash system. Please refer to Appendix B – Bottom Ash System Rainfall Estimate for the calculation details, including material assumptions, information, and calculations used to determine the 10-year 24-hour rainfall event.

Equipment included in the surge capacity calculation is summarized in Table 2.



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Table 2 - Systems and Volume Included in Surge Capacity

Bottom Ash System	Available Surge Volume (Gallons)
Units 1, 2, and 3 Bottom Ash System	
Units 1 & 2 Boiler Room Sump Surge Volume	2,796
Units 3 Ash Hopper Pit Sump Surge Volume	1,492
Units 1 & 2 Ash Hopper Surge Volume	3,733
Unit 3 Ash Hopper Surge Volume	2,747
Surge Volume of Bottom Ash Pond	11,057,384
Total Units 1, 2, and 3 Surge Capacity	11,068,153

During sluicing operations, bottom ash is sluiced to the Bottom Ash Pond. Ash is stored in the settling pond and, on occasion, dredged into trucks for final storage in a landfill. The maximum quantity of ash is approximately equal to the volume available in the settling pond following several years of continuous operation. For this evaluation, it is assumed that the rainfall event occurs during the sluicing operation; thus, the volume of ash collected within the bottom ash system is subtracted from the available volume in the surge tank.

Stormwater flows for the 10-year events and the 50-year events are summarized in Figure 1 and Figure 2, respectively and compared to the calculated surge capacity summarized above.

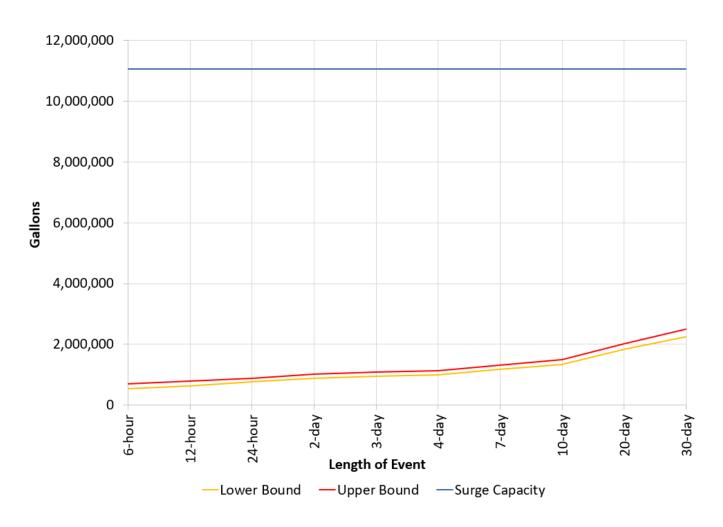


Figure 1 – 10-year Storm Events Rain Runoff Evaluation

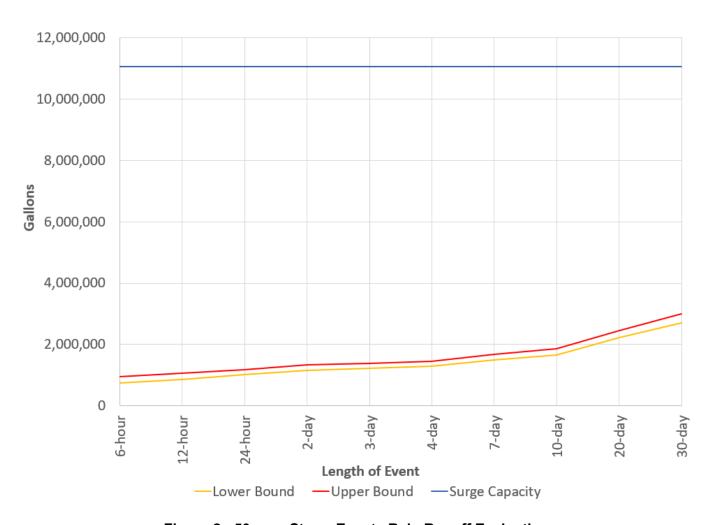
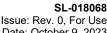


Figure 2 - 50-year Storm Events Rain Runoff Evaluation

As shown in Figure 1 and Figure 2 above, the Bottom Ash Pond is adequately sized to contain 100% of the stormwater runoff volume generated during either the 10-year or 50-year storm events, which would allow Cardinal to not discharge from the Bottom Ash Pond during each of the stormwater events evaluated up to the 50-year, 30-day event.

Free board was also added to the pond depth to ensure that the pond will not overtop its berms.





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4.2 DISCHARGES TO BALANCE WASTEWATER INFLOWS

Water in the bottom ash systems at Cardinal is recirculated to the extent feasible. Services such as hopper wall cooling, seal trough water, and ash fluidization in the hoppers are supplied from recirculated water. Therefore, no discharge is required to maintain system balance from wastewater inputs other than BATW.

4.3 DISCHARGES TO MAINTAIN SYSTEM WATER CHEMISTRY

The EPA studied the behavior of coal ash particles in water in its study titled "Behavior of Coal Ash Particles in Water: Trace Metal Leaching and Ash Settling" (EPA-600/7-80-067, March 1980). The study was conducted at Tennessee Valley Authority (TVA) coal-fired power plants. The report addressed six major areas of concern in wet ash disposal, namely, the (1) characteristics of ashes and ash pond effluents, (2) effects of ash and raw water characteristics on the pH of ash pond water, (3) methods for pH adjustment of ash pond effluents, (4) settling characteristics of both fly ash and bottom ash, (5) leaching of minerals from ashes, and (6) relationship of trace metals to pH and concentration of suspended solids in ash pond effluents. Of specific interest are the evaluations of ash pond water quality characteristics in relation to the chemical quality of the fuel burned at twelve TVA coal-fired power stations.

The primary system chemistry concern is the buildup of bottom ash fines in the recirculating transport water. Fines enter the bottom ash system with other, larger, particles of ash falling into the hopper and occasionally from fracturing of the larger particles of ash due to the thermal shock of entering the hopper water. Some fines exit the bottom ash system through entrainment in bottom ash purge water and ash in trucks being taken to landfill. The fines will concentrate in the bottom ash water until the mass flow rate of fines into the system is equal to the mass flow rate of fines exiting. According to Cardinal operating data, the plant maintains a total suspended solids (TSS) concentration in the BATW of less than 19.7 mg/L at 99% confidence to protect bottom ash system pumps from excessive abrasion damage. Table 3 provides an estimate of the bottom ash purge water discharge needed at Cardinal to maintain a TSS concentration of 19.7 mg/L. Please refer to Appendix C – Bottom Ash Purge Water Suspended Solids Estimate for the calculation details, including material assumptions, information, and calculations used by the certifying professional engineer to determine the primary wetted bottom volume.



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Table 3 - Estimated Bottom Ash Purge Water Discharge to Maintain TSS

Bottom Ash System	Bottom Ash Purge
Unit 1, 2, and 3	5.3% of PWV

Another system chemistry concern is the scaling or corrosivity of the BATW in high-recycle bottom ash handling systems. S&L used Cardinal fuel ash quality and the chart on page 17 of the coal ash study referenced above (EPA-600/7-80-067, pg. 17) to estimate the pH of the high-recycle bottom ash handling system at Cardinal. The chart relates the ratio of ash calcium oxide and magnesium oxide concentrations to the ash sulfur trioxide concentration [(CaO + MgO)/SO₃ (mole ratio)]. All of the units at Cardinal burn the same fuel, the results of applying the EPA analysis are shown in Table 4.

Table 4 – Estimate of Bottom Ash System Equilibrium pH

Fuel	Fuel Ash Calcium Oxide (%)	Fuel Ash Magnesium Oxide (%)	Fuel Ash Sulfur Tri- Oxide (%)	Ratio of (CaO+MgO) to SO ₃	Estimated pH
Marshall County Coal Resources	3.20	0.72	2.69	1.46	<3 (acidic)
Ohio County Coal Resources	2.31	0.59	2.20	1.31	<3 (acidic)
Iron Senergy	3.59	0.78	3.85	1.14	<3 (acidic)
Tunnel Ridge	1.81	0.73	1.63	1.56	<3 (acidic)

The predicted acidic chemistry of the bottom ash system at Cardinal will occur at system chemical equilibrium, which takes time to achieve. In order to prevent the system from reaching chemical equilibrium, water in the system may be continuously discharged and made-up with fresh utility or service water. The maximum allowable discharge rate allowed by the 2020 Reconsideration Rule (i.e., 10% of PWV per day) would provide the greatest protection from constituents in the ash creating acidic water in the system.



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4.4 MAINTENANCE RELATED DISCHARGES

An allowance to discharge from the BATW system is needed to conduct maintenance activities. In order to drain the entire bottom ash system for maintenance and maintain the 30-day rolling average per day discharge requirement taking into account discharges addressed in Sections 4.1 through 4.3, an allowable discharge equal to or greater than the following is needed:

$$\frac{\%PWV}{day} = \frac{((TSV/PWV))}{30 \text{ days}}$$

Where:

TSV: Total System Volume PWV: Primary Wetted Volume

%PWV/day: Minimum Percentage of Primary Wetted Volume per Day

At Cardinal, the bottom ash handling system has a total system volume (without the Bottom Ash Pond) of 723,792 gallons and a PWV of 657,345 gallons. Thus, in order to drain the system completely for a maintenance event and maintain the 30-day rolling average per day discharge requirement, an allowable discharge for maintenance on a %PWV/day basis greater than the following is needed:

$$\frac{\%PWV}{day} = \frac{\left(\left((723,792)/657,345\right)\right)}{30 \ days} = \frac{3.7\%PWV}{day}$$

According to e-mail correspondence with Cardinal Operations Personnel, on each unit, during normal operation, certain sumps (boiler room sump on Unit 1 and 2, ash pit sump on Unit 3) collect bottom ash transport water. The water from the sumps is pumped through the non-operating bottom ash transport pipeline on each unit. This normally keeps that bottom ash transport water contained within the "closed loop" system.

However, on occasion, the bottom ash lines need maintenance work. When one of the two bottom ash lines on a unit requires maintenance (while the generating unit is still in service), the one remaining sluice pipeline is employed to transport ash to the bottom ash pond. The pipeline on which maintenance is being performed is unavailable for use to convey the sump water. During these maintenance events, water from the applicable sump is routed to the LVW Pond.

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Based on historical operations, the average time needed to perform maintenance on one of these transport lines is approximately 8 hours. The estimated volume of water discharged as a percentage of PWV per day during one of these maintenance events may be calculated using the following formulae:

$$MWV = SPC \times EOD$$

Where:

MWV: Maintenance Water Volume (gallons)

SPC: Sump Pump Capacity (gpm)

EOD: Estimated Operation Duration (min)

$$\frac{\%PWV}{day} = \frac{\left((MWV/PWV) \right)}{30 \ days}$$

Where:

MWV: Total System Volume PWV: Primary Wetted Volume

%PWV/day: Minimum Percentage of Primary Wetted Volume per Day

For example, during a Unit 1 sluice pipeline outage, the Unit 1 boiler room sump (rated at 2000 gpm) may operate for the entirety of the 8-hour (480-minute) maintenance period.

$$MWV = 2000 \times 480 = 960,000 \ gallons$$

$$\frac{\%PWV}{day} = \frac{((960,000/657,345))}{30 \ days} = \frac{4.9\%PWV}{day}$$

The total discharge requested for these maintenance activities is the total of the two events, or 8.6% of PWV per day.

4.5 TOTAL DISCHARGES

The minimum 30-day rolling average discharge rate on a %PWV per day basis is calculated as the sum of the discharges necessary for each bottom ash purge water category. The minimum discharge for the combined units at Cardinal is summarized in the Table 5.



Table 5 - The 30-Day Rolling Average Discharge Volume as a Percent of Primary Active Wetted **Bottom Ash System Volume**

Type of Discharge Event	Units 1, 2 and 3
Exceeding 10-year, 24-hour (or longer duration) storm event See 40 CFR $\S423.13(k)(2)(i)(A)(1)$	0%
Regular discharge needs to maintain water balance due to wastewater inflows See 40 CFR $\S423.13(k)(2)(i)(A)(2)$	0%
Regular discharge needs to maintain water chemistry See 40 CFR §423.13(k)(2)(i)(A)(3)	5.7%
Other infrequent maintenance events See 40 CFR §423.13(k)(2)(i)(A)(4)	8.6%
Total % of PWV of coincident maximum volume discharged per day	Up to 14.3%
Total % Discharge Volume Requested	10%

Operational strategies may be employed to reduce the total 30-day rolling average discharge lower than the sum of the individual contributors. The requested 10% total discharge volume reflects the implementation of these strategies.

NARRATIVE DESCRIPTION OF THE WASTEWATER TREATMENT 5. **SYSTEMS**

Cardinal is equipped with the following wastewater treatment systems which do not treat bottom ash transport water:

- Unit 1 & 2 Sewage Treatment Plant for Domestic Wastewater (Outfall 006)
- Unit 3 Sewage Treatment Plant for Domestic Wastewater (Outfall 008)
- Common FGD Wastewater Treatment System (Outfall 601)

Cardinal is equipped with the following wastewater treatment systems which do treat bottom ash transport water:

Bottom Ash Pond Discharge (To FGD)





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Prior to December 31, 2025, Cardinal will install, commission, and startup the following wastewater treatment system:

Flue gas desulfurization wastewater treatment system compliant with discharge limitations in 40 CFR 423.

5.1 NON-BOTTOM ASH TREATMENT DISCHARGES

The Unit 1&2 Sewage Treatment System for Domestic Wastewater discharges to Outfall 006. The system receives a blend of domestic sewage and air conditioning condensate. The system consists of aeration, activated sludge, sedimentation, flocculation, sand filtration, and UV disinfection, which removes activated sludge and disinfects the domestic sewage. The Unit 1&2 Sewage Treatment System discharges a daily average of 0.02 MGD into the Riddles Run. This flow is not expected to significantly change in the future.

The Unit 3 Sewage Treatment System for Domestic Wastewater discharges to Outfall 008. The system receives a blend of domestic sewage and laboratory wastewater. The system consists of aeration, activated sludge, sedimentation, flocculation, sand filtration, and UV disinfection, which removes activated sludge and disinfects the domestic sewage. The Unit 3 Sewage Treatment System discharges a daily average of 0.02 MGD into the Ohio River. This flow is not expected to change significantly in the future.

The FGD Wastewater Treatment System discharges to Internal Outfall 601. The system receives a blend of Unit 1, 2, and 3 FGD wastewater. The system consists of equalization, neutralization, primary clarification, and secondary clarification, which removes suspended solids and neutralizes the stream. The FGD Wastewater Treatment System discharges a daily average of 0.78 MGD into the Outfall 001, which discharges to the Ohio River. This flow may be reduced due to future changes to the operation of Cardinal Station.

5.2 BOTTOM ASH TREATMENT DISCHARGES

The Bottom Ash Pond discharge is located at the southern end of the plant site. The system consists of a sedimentation basin which removes suspended solids from bottom ash transport water. This system recirculates the majority of the water it receives to the suction of the bottom ash system recirculation pumps located on the north bank of the Bottom Ash Pond. In order to control pH, suspended solid fines, and other constituents, a certain amount of water is discharged to the FGD. This flow is not expected to change in the future.





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5.3 FUTURE WASTEWATER TREATMENT SYSTEMS

Prior to December 31,2025, Cardinal will install a polishing bioreactor to treat the effluent of the existing FGD wastewater treatment system. The bioreactor system, which uses microorganisms to reduce soluble pollutants, will be designed meet the ELG limits. The capacity of the system is 440 gpm based on Cardinal Station operating data.





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APPENDIX A.

BOTTOM ASH VOLUME CALCULATION

Cardinal Station

DOCUMENT NO. 2020-03682 BOTTOM ASH SYSTEM WETTED VOLUME CALCULATION

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PROJECT NO. 13770-006 Date: 15 August 2023

ISSUE SUMMARY Form SOP-0402-07, Revision 12

		DESIGN CONTROL SUMMARY	
CLIENT:	Buckeye Power	UNIT & NO.: 1, 2, 3	Page No.:
PROJECT NAME:	Cardinal Generating Station		<u></u>
PROJECT NO.:	13770-006	☐ NUCLEAR SAF ☑ NOT NUCLEAF	ETY RELATED R SAFETY RELATED
CALC. NO.:	2020-03682		
TITLE:	Bottom Ash Volume Wetted Calculation		
EQUIPMENT NO.:			
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PREPARER N. Clough	Nathaniel Clouds	DATE:	15-Aug-23
REVIEWER D. Wu		DATE:	15-Aug-23
APPROVER D. Wu	David Wu Dall: 2023.06.15 11.04.35.0500'	DATE:	15-Aug-23
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PROJECT NO. 13770-006 Date: 15 August 2023

BOTTOM ASH SYSTEM WETTED VOLUME CALCULATION

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BOTTOM ASH SYSTEM WETTED VOLUME CALCULATION

1.0	PURPOSE AND SCOPE:								
1.01	The Cardinal power station consists of three (3) units. Project 13770.006 includes the lining and closure of the existing bottom ash ponds for each units.								
		primary active wetted volume of the revised bottom ash			e (10% of				
1.02	the primary active wetted bottom ash volume).	primary detire wetter votable of the revised conton as	. system in accordance with 220 regu	and on the control of purge	(10/001				
	, and a second s								
Item	Description	Reference	Unit of Measure	Data Value	Input (V/UV/				
Ittin	Description	Reference	ome of Measure	Data value					
2.0	DESIGN INPUTS:		<u> </u>		EJ)				
		ed Definitions, is provided below for basis of included e	equipment:						
		m volume" means the maximum volumetric capacity of		redundant nining (including recirculation					
2.01		circulation loop tanks (e.g., bins, troughs, clarifiers, an			v				
2.01		ipment (e.g., installed spares, redundancies, and mainte							
	the bottom ash.	pmen (e.g., minuted spares, redundancies, and manne	mance tames, and non-conton assure	maport systems that may all cer process react to					
2.02	The specific gravity of the water is 1.00 and the de	encity is 62.4 lb/ft3			EJ				
2.02		s are determined per drawings in Attachment 8.02.			V				
2.03	Units 1 & 2 Boiler Room Sump volume is determ				v				
2.05		the Boiler Room Sump is determined per Attachment 8	2.06		v				
2.06	Unit 3 Ash Hopper and Seal Trough volumes are		3.00.		v				
2.07	Unit 3 Ash Hopper Pit Sump volume is determine				v				
2.08		oths were determined using drawings and Google Earth i	images shown in Attachment 8 07		EJ				
2.09		s determined per the Bill of Materials in Attachment 8.04			V				
2.10		m Ash Pumps to Jet Pumps is determined using Attachn			v				
2.11		h Pumps to Jet Pumps is determined using Attachment 8			v				
Item	Description	Reference	Unit of Measure	Data Value	_ v				
3.0	ASSUMPTIONS:	Reference	Unit of Measure	Data value					
		in is assumed the same length as the Units 1 & 2 overflo	ay nining to the Boiler Poom Sumn		EJ				
	Unit 3 overflow piping to the Ash Hopper Pit Sump is assumed the same length as the Units 1 & 2 overflow piping to the Boiler Room Sump.								
3.01					EI				
3.02	For all three (3) Units, bottom ash hopper surge ve	olume was taken at high water level, 6" above normal op			EJ				
	For all three (3) Units, bottom ash hopper surge volume Seal Trough is assumed to be 6" deep and extends	plume was taken at high water level, 6" above normal op 6" around the ash hoppers.	perating level.	5 fact freehoard so an assumed dowth of 5 ft is	EJ EJ				
3.02	For all three (3) Units, bottom ash hopper surge volume Seal Trough is assumed to be 6" deep and extends. The South Pond was not considered part of the price.	olume was taken at high water level, 6" above normal op	perating level. the surge volume. The South Pond has	5 feet freeboard so an assumed depth of 5 ft is					
3.02 3.03	For all three (3) Units, bottom ash hopper surge verseal Trough is assumed to be 6" deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33.	olume was taken at high water level, 6" above normal or 6" around the ash hoppers. imary wetted volume, however, it is considered part of the	perating level. the surge volume. The South Pond has s).	•	EJ				
3.02 3.03 3.04	For all three (3) Units, bottom ash hopper surge verseal Trough is assumed to be 6" deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33.	olume was taken at high water level, 6" above normal op 6" around the ash hoppers. imary wetted volume, however, it is considered part of the 9 acre-feet (based on an average pond area of 6.78 acres	perating level. the surge volume. The South Pond has s).	•	EJ EJ				
3.02 3.03 3.04 3.05	For all three (3) Units, bottom ash hopper surge versions assumed to be 6° deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A'	olume was taken at high water level, 6" above normal op 6" around the ash hoppers. imary wetted volume, however, it is considered part of ti 9 acre-feet (based on an average pond area of 6.78 acres WRP discharge lines for each Unit is the lower diameter	perating level. the surge volume. The South Pond has s).	"nominal for Units 1 and 2).	EJ EJ				
3.02 3.03 3.04 3.05 Item	For all three (3) Units, bottom ash hopper surge versions as the same of the s	olume was taken at high water level, 6" above normal op 6" around the ash hoppers. mary wetted volume, however, it is considered part of ti 9 acre-feet (based on an average pond area of 6.78 acres WRP discharge lines for each Unit is the lower diameter Variables RIA:	perating level. the surge volume. The South Pond has s).	"nominal for Units 1 and 2).	EJ EJ				
3.02 3.03 3.04 3.05 Item	For all three (3) Units, bottom ash hopper surge we Seal Trough is assumed to be 6° deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A Description METHODOLOGY & ACCEPTANCE CRITE The methodology for performing the calculations involved.	olume was taken at high water level, 6" above normal op 6" around the ash hoppers. mary wetted volume, however, it is considered part of ti 9 acre-feet (based on an average pond area of 6.78 acres WRP discharge lines for each Unit is the lower diameter Variables RIA:	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2).	EJ EJ				
3.02 3.03 3.04 3.05 Item 4.0	For all three (3) Units, bottom ash hopper surge we Seal Trough is assumed to be 6° deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A Description METHODOLOGY & ACCEPTANCE CRITE The methodology for performing the calculations involved.	olume was taken at high water level, 6" above normal op. 6" around the ash hoppers. mary wetted volume, however, it is considered part of the grace-feet (based on an average pond area of 6.78 acres WRP discharge lines for each Unit is the lower diameter Variables RIA: ess the following principal steps: ash water during normal plant operation and ash handling pro	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2).	EJ EJ				
3.02 3.03 3.04 3.05 Item 4.0	For all three (3) Units, bottom ash hopper surge versions as sumed to be 6" deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A Description METHODOLOGY & ACCEPTANCE CRITE The methodology for performing the calculations involved identify all equipment and piping expected to contain	olume was taken at high water level, 6" above normal op. 6" around the ash hoppers. mary wetted volume, however, it is considered part of the grace-feet (based on an average pond area of 6.78 acres WRP discharge lines for each Unit is the lower diameter Variables RIA: ess the following principal steps: ash water during normal plant operation and ash handling pro	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2).	EJ EJ				
3.02 3.03 3.04 3.05 Item 4.0	For all three (3) Units, bottom ash hopper surge versions assumed to be 6° deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A Description METHODOLOGY & ACCEPTANCE CRITE The methodology for performing the calculations involved identify all equipment and piping expected to contain bettermine the volume of all identified equipment and	olume was taken at high water level, 6" above normal of 6" around the ash hoppers. """ """ """ """ """ """ """ """ """	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2). Data Value	EJ EJ				
3.02 3.03 3.04 3.05 Item 4.0	For all three (3) Units, bottom ash hopper surge versions assumed to be 6° deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A Description METHODOLOGY & ACCEPTANCE CRITE The methodology for performing the calculations involved identify all equipment and piping expected to contain bettermine the volume of all identified equipment and	olume was taken at high water level, 6" above normal op 6" around the ash hoppers. """""""""""""""""""""""""""""""""""	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2).	EJ EJ				
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3.02 3.03 3.04 3.05 Item 4.0 4.01	For all three (3) Units, bottom ash hopper surge we Seal Trough is assumed to be 6° deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A Description METHODOLOGY & ACCEPTANCE CRITE The methodology for performing the calculations involved the state of the state	olume was taken at high water level, 6" above normal op. 6" around the ash hoppers. 6" around the ash hoppers. 6" around the wash hoppers. WRP discharge lines for each Unit is the lower diameter Wariables RIA: "ese the following principal steps: ash water during normal plant operation and ash handling propiping that is applicable V = Volume [fi3] 1 = Length (ft) w = Width (ft) V = Volume [fi3] 1 = Length (ft) w = Width (ft) w = Width (ft)	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2). Data Value	EJ EJ				
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3.02 3.03 3.04 3.05 Item 4.0 4.01	For all three (3) Units, bottom ash hopper surge vseal Trough is assumed to be 6° deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A Description METHODOLOGY & ACCEPTANCE CRITE The methodology for performing the calculations involved identify all equipment and piping expected to contain between the performing the calculations involved in the performance of the performance of the calculations of the contains and Volume of Rectangular Prism Volume of Triangular Prism	olume was taken at high water level, 6" above normal of 6" around the ash hoppers. """ """ """ """ """ """ """ """ """	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2).	EJ EJ				
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3.02 3.03 3.04 3.05 Item 4.0 4.01	For all three (3) Units, bottom ash hopper surge versure and the sassumed to be 6° deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A Description METHODOLOGY & ACCEPTANCE CRITE The methodology for performing the calculations involved identify all equipment and piping expected to contain • Determine the volume of all identified equipment and Volume of Rectangular Prism Volume of Triangular Prism	olume was taken at high water level, 6" above normal of 6" around the ash hoppers. """ """ """ """ """ """ """ """ """	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2).	EJ EJ				
3.02 3.03 3.04 3.05 Item 4.0 4.01	For all three (3) Units, bottom ash hopper surge vseal Trough is assumed to be 6° deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A Description METHODOLOGY & ACCEPTANCE CRITE The methodology for performing the calculations involved identify all equipment and piping expected to contain between the performing the calculations involved in the performance of the performance of the calculations of the contains and Volume of Rectangular Prism Volume of Triangular Prism	olume was taken at high water level, 6" above normal op 6" around the ash hoppers. """ """ """ """ """ """ """ """ """	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2). Data Value $V = lwh$ $V = lwh\left(\frac{1}{2}\right)$ $V = \left(\frac{B_1 + B_2}{2}\right)hd$	EJ EJ				
3.02 3.03 3.04 3.05 Item 4.01 4.02 4.03	For all three (3) Units, bottom ash hopper surge versure and the sassumed to be 6° deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A Description METHODOLOGY & ACCEPTANCE CRITE The methodology for performing the calculations involved identify all equipment and piping expected to contain • Determine the volume of all identified equipment and Volume of Rectangular Prism Volume of Triangular Prism	olume was taken at high water level, 6" above normal of 6" around the ash hoppers. """ """ """ """ """ """ """ """ """	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2). Data Value $V = lwh$ $V = lwh\left(\frac{1}{2}\right)$ $V = \left(\frac{B_1 + B_2}{2}\right)hd$	EJ EJ				
3.02 3.03 3.04 3.05 Item 4.0 4.01 4.02	For all three (3) Units, bottom ash hopper surge versure and the sassumed to be 6° deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A Description METHODOLOGY & ACCEPTANCE CRITE The methodology for performing the calculations involved identify all equipment and piping expected to contain • Determine the volume of all identified equipment and Volume of Rectangular Prism Volume of Triangular Prism	olume was taken at high water level, 6" above normal op 6" around the ash hoppers. """ """ """ """ """ """ """ """ """	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2).	EJ EJ				
3.02 3.03 3.04 3.05 Item 4.01 4.02 4.03	For all three (3) Units, bottom ash hopper surge versure and the sassumed to be 6° deep and extends. The South Pond was not considered part of the prused based on total pond volume for a total of 33. It is assumed that the last 50 ft of piping for the A Description METHODOLOGY & ACCEPTANCE CRITE The methodology for performing the calculations involved identify all equipment and piping expected to contain • Determine the volume of all identified equipment and Volume of Rectangular Prism Volume of Triangular Prism	olume was taken at high water level, 6" above normal of 6" around the ash hoppers. """ """ """ """ """ """ """ """ """	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2). Data Value $V = lwh$ $V = lwh\left(\frac{1}{2}\right)$ $V = \left(\frac{B_1 + B_2}{2}\right)hd$	EJ EJ				
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3.02 3.03 3.04 3.05 Item 4.01 4.02 4.03	For all three (3) Units, bottom ash hopper surge versure and the search of the same of the process of the search of the search of the search of the process of the search	olume was taken at high water level, 6" above normal of 6" around the ash hoppers. """ """ """ """ """ """ """ """ """	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2). Data Value $V = lwh$ $V = lwh\left(\frac{1}{2}\right)$ $V = \left(\frac{B_1 + B_2}{2}\right)hd$ $V = \left(\frac{lwh}{3}\right)$	EJ EJ				
3.02 3.03 3.04 3.05 Item 4.01 4.02 4.03	For all three (3) Units, bottom ash hopper surge versure and the search of the same of the process of the search of the search of the search of the process of the search	olume was taken at high water level, 6" above normal of 6" around the ash hoppers. """ """ """ """ """ """ """ """ """	he surge volume. The South Pond has s). piping (14" nominal for Unit 3 and 12	"nominal for Units 1 and 2). Data Value $V = lwh$ $V = lwh\left(\frac{1}{2}\right)$ $V = \left(\frac{B_1 + B_2}{2}\right)hd$	EJ EJ				



BOTTOM ASH SYSTEM WETTED VOLUME CALCULATION

		M ASH STSTEM WETTED							
Item	Description	Reference	Unit of Measure	Equation					
5.0	CALCULATIONS:			-					
5.01	See Attachment 8.01 for wetted volume summar	y breakdown							
Item	Description	Reference	Unit of Measure	Value	Accept (Y/N)				
6.0	RESULTS:								
6.01	Wetted volume of equipment and piping								
6.02	Units 1 & 2 Ash Hoppers	Attachment 8.02	gal	123,740	Y				
6.03	Units 1 & 2 Seal Trough	Assumption 3.05	gal	550	Y				
6.04	Units 1 & 2 Overflow Piping	Attachment 8.06	gal	318	Y				
6.05	Units 1 & 2 Boiler Room Sump	Attachment 8.03	gal	28,754	Y				
6.06	Unit 3 Ash Hoppers	Attachment 8.05	gal	72,187	Y				
6.07	Unit 3 Seal Trough	Assumption 3.05	gal	274	Y				
6.08	Unit 3 Overflow Piping	Assumption 3.01	gal	159	Y				
6.09	Unit 3 Ash Hopper Pit Sump	Attachment 8.09	gal	2,238	Y				
6.10	AWRP Piping	Attachment 8.07	gal	185,037	Y				
6.11	Piping from Bottom Ash Pump to Jet Pump	Assumption 3.04	gal	4,420	Y				
6.12	Piping from Jet Pumps to South Pond	Attachment 8.08	gal	119,591	Y				
6.13	Boiler Room Sump and Bottom Ash Hopper Pit Sump Discharge lines to Crossover	Attachments 8.03 and 8.13	gal	7,481	Y				
6.14	Units 1 and 2 Boiler Room Sump Crossover Piping to South Pond	Attachment 8.12	gal	92,465	Y				
6.15	Unit 3 Ash Hopper Pit Sump Crossover Piping to South Pond	Attachment 8.12	gal	20,131	Y				
	TOTAL WETTED VOLUME UNITS 1, 2 & 3		gal	657,345	Y				
	Estimated Max Daily Blowdown based on 10% wetted volume over a 30-day rolling average		gpm	46	Y				
6.16	TOTAL VOLUME UNITS 1, 2 & 3		gal	723,792	Y				
6.17	Units 1 & 2 Boiler Room Sump Surge Volume	Attachment 8.03	gal	2,796	Y				
6.18	Units 3 Ash Hopper Pit Sump Surge Volume	Attachment 8.09	gal	1,492	Y				
6.19	Units 1 & 2 Ash Hopper Surge Volume	Attachment 8.02	gal	3,733	Y				
6.20	Unit 3 Ash Hopper Surge Volume	Attachment 8.05	gal	2,747	Y				
6.21	Surge Volume of South Pond	Assumption 3.04	gal	11,057,384	Y				
	C	1		7					
7.0	REFERENCES:								
7.01	N/A								
8.0	ATTACHMENTS:								
8.01	Wetted Ash Volume Calculation Summary								
8.02	U1 & U2 Bottom Ash Hopper Volume								
8.03	U1 & U2 Boiler Room Sump								
8.04	U1, U2 & U3 Bottom Ash Piping Isometrics								
8.05	U3 Bottom Ash Hopper Volume								
8.06	U1 & U2 Bottom Ash Hopper Overflow Pipe								
8.07	AWRP Piping drawings and images								
8.08	A WKP riping drawings and images Excel Formulas								
8.09									
	U1 and U2 Bottom Ash Pumps to Jet Pumps								
8.10									
8.11	U3 Bottom Ash Pumps to Jet Pumps U1 and U2 Bottom Ash Sump Pump Piping and U3 A	a-l. H Die G Die in - franc G	C4h D4						
8.12			South Folid						
8.13	U3 Ash Hopper Pit Sump Discharge pipe to Crossover								



PROJECT NO. 13770-006 Date: 15 August 2023

8.01 Wetted Ash Volume Calculation Summary



PROJECT NO. 13770-006 Date: 15 August 2023

WETTED ASH VOLUME CALCULATION - EQUIPMENT

Piping	Pipe schedule	Pipe nominal dia (in)	Pipe Inner dia (in)	Pipe length (ft)	Pipe Cross Sectional area (ft²)	Volume (ft³)	Volume (gal)	Notes
1. Unit 1 Bottom Ash Hopper								
1-01 - Hopper Volume	N/A		N/A	N/A	N/A	N/A	61,870	
1-02 - Seal Trough (if applicable)	N/A	N/A	N/A	N/A	N/A	36.75	275	
1-03 - Surge Capacity (assume water level to be at emergency overflow level for hopper)	N/A		N/A	N/A	N/A	249.28	1,867	
1-04 - Overflow piping to Boiler Room Sump	STD		12	27	0.79	21.21	159	
1-05 - Boiler Room Sump	N/A	N/A	N/A	N/A	N/A	1,920.00	14,377	First Pump Start level at 666' is used
1-06 - Boiler Room Sump Surge Volume	N/A	N/A	N/A	N/A	N/A	186.72	1,398	Extreme High level alarm at 667'-2" is used
2. Unit 2 Bottom Ash Hopper								
2-01 - Hopper Volume	N/A	N/A	N/A	N/A	N/A	N/A	61,870	
2-02 - Seal Trough (if applicable)	N/A	N/A	N/A	N/A	N/A	36.75	275	
2-03 - Surge Capacity (assume water level to be at emergency overflow level for hopper)	N/A	N/A	N/A	N/A	N/A	249.28	1,867	
2-04 - Overflow piping to Boiler Room Sump	STD		12	27	0.79	21.21	159	
2-05 - Boiler Room Sump	N/A	N/A	N/A	N/A	N/A	1,920.00	14,377	First Pump Start level at 666'" is used
2-06 - Boiler Room Sump Surge Volume	N/A	N/A	N/A	N/A	N/A	186.72	1,398	Extreme High level alarm at 667'-2" is used
3. Unit 3 Bottom Ash Hopper								
3-01 - Hopper Volume	N/A	N/A	N/A	N/A	N/A	9,640.42	72,187	
3-02 - Seal Trough (if applicable)	N/A	N/A	N/A	N/A	N/A	36.63	274	
3-03 - Surge Capacity (assume water level to be at emergency overflow level for hopper)	N/A	N/A	N/A	N/A	N/A	366.81	2,747	
3-04 - Overflow piping to Ash Hopper Pit Sump	STD	12	12	27	0.79	21.21	159	
3-05 - Ash Hopper Pit Sump	N/A	N/A	N/A	N/A	N/A	298.94	2,238	First Pump Start level at 80' is used
3-06 - Ash Hopper Pit Sump Surge Volume	N/A	N/A	N/A	N/A	N/A	199.29	1,492	Third Pump Start level at 82' is used
4. Surge Volume of South Pond	N/A	N/A	N/A	N/A	N/A	1,476,680.61	11,057,384	
F. Total Valuma of Equipment							238.989	The sum of all volumes above except the Surge
5. Total Volume of Equipment							230,989	Volume of the South Pond



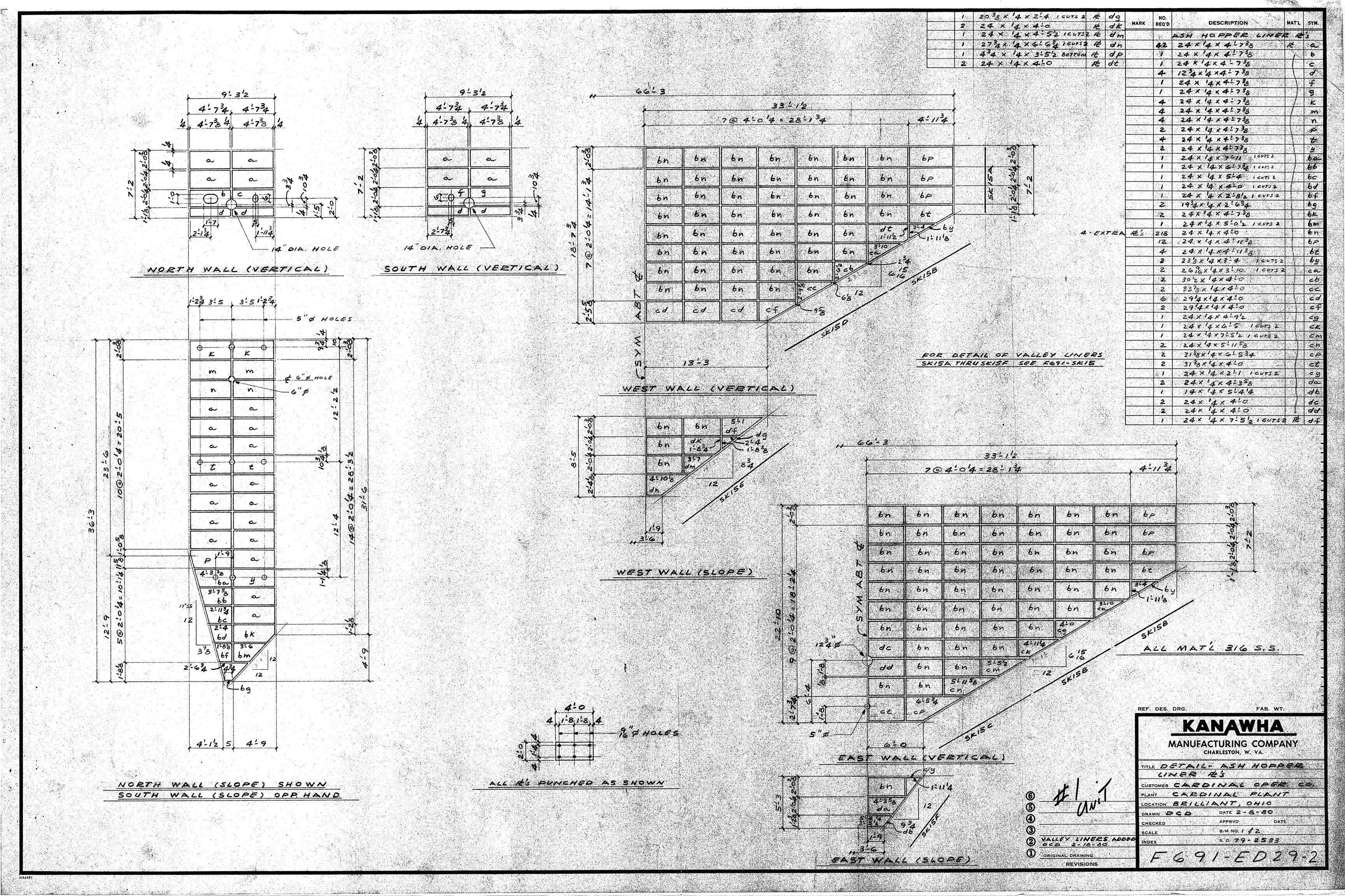
WETTED ASH VOLUME CALCULATION - PIPING

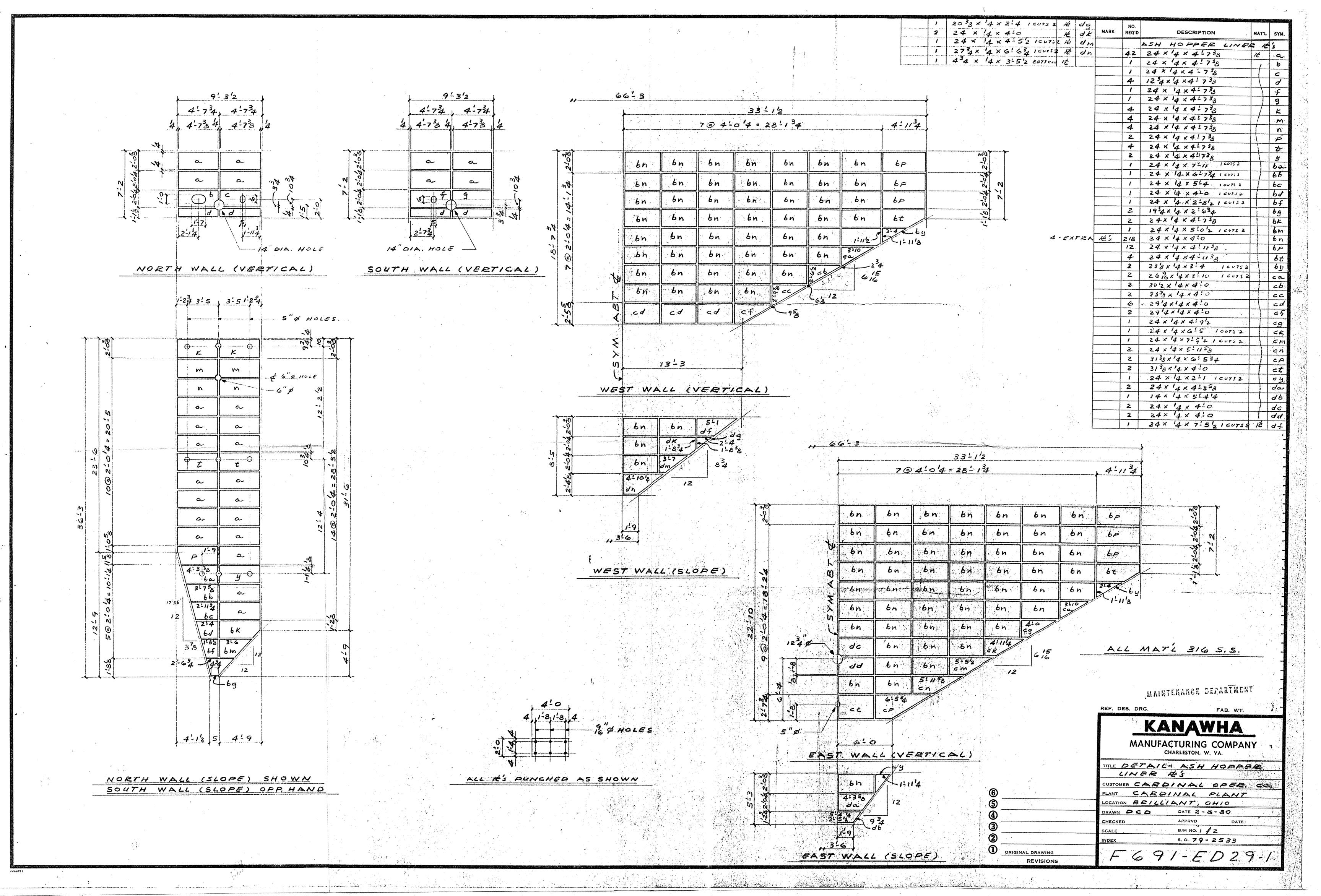
Piping	Pipe schedule	Pipe nominal dia (in)	Pipe Inner dia (in)	Pipe length (ft)	Pipe Cross Sectional area (ft²)	Volume (ft ³)	Volume (gal)	Notes
1. Piping from Ash Water Recirculation Pump (AWRP) Loop to Units 1, 2, and 3			•		•		•	•
1-01a - AWRP Discharge Common Header up to Unit 3	STD		29.25	98	4.67	457.30	3,424	
1-01b - AWRP Discharge Common Header up to Unit 3	STD (20)	24	23.25	2522	2.95	7,435.64	55,678	
1-01c - Redundant AWRP Discharge Pipe	STD (20)	24	23.25	2522	2.95	7,435.64	55,678	Redundant AWRP pipe for the discharge common header up to Unit 3
1-02a - AWRP Discharge Dedicated line to Unit 3 Bottom Ash Pump	STD	18	17.25	672	1.62	1,090.62	8,167	
1-02b - AWRP Discharge Dedicated line to Unit 3 Bottom Ash Pump	STD (30)	14	13.25	50	0.96	47.88	359	Assumed 14" nominal piping extend 50 ft to Bottom Ash Pump
1-03 - AWRP Discharge Common Header up to Unit 2	STD (20)	24	23.25	4740	2.95	13,974.99	104,645	
1-04a - AWRP Discharge Dedicated line to Unit 2 Bottom Ash Pump	STD (30)	16	15.25	456	1.27	578.40	4,331	
1-04b - AWRP Discharge Dedicated line to Unit 2 Bottom Ash Pump	STD	12	12	50	0.79	39.27	294	Assumed 12" nominal piping extend 50 ft to Bottom Ash Pump
1-05a - AWRP Discharge Dedicated line to Unit 1 Bottom Ash Pump	STD (30)	16	15.25	826	1.27	1,047.72	7.845	
1-05b - AWRP Discharge Dedicated line to Unit 1 Bottom Ash Pump	STD	12	12	50	0.79	39.27	294	Assumed 12" nominal piping extend 50 ft to Bottom Ash Pump
2. Piping from Bottom Ash Pump to Jet Pump		l						, and
2-01 - Unit 1 and Unit 2 Common Bottom Ash Pump to Jet Pump	STD	12	12	550.58	0.79	432.43	3,238	Conservatively used just the lengths of pipe from Att. 8.10 and assumed all pipe was 12"
2-02 - Unit 3 Bottom Ash Pump to Jet Pump	STD	12	12	200.9	0.79	157.79	1,182	Conservatively used just the lengths of pipe from Att. 8.11 and assumed all pipe was 12"
3. Piping from Jet Pump to South Pond								
3-01 - Unit 1 Jet Pump to South Pond	HDPE / Basalt Lined	12	11.8	8448	0.76	6,415.72	48,041	ID from CBP doc, A portion of the pipe is 14" (SDR 13.5) HDPE (ID 11.8") and another portion is 12" Basalt lined CS (ID 11.93") so 11.8" is used for conservatism
3-02 - Unit 2 Jet Pump to South Pond	HDPE / Basalt Lined	12	11.8	8342	0.76	6,335.52	47,440	ID from CBP doc, A portion of the pipe is 14" (SDR 13.5) HDPE (ID 11.8") and another portion is 12" Basalt lined CS (ID 11.93") so 11.8" is used for conservatism
3-03 - Unit 3 Jet Pump to South Pond	HDPE / Basalt Lined	12	11.8	4240	0.76	3,219.81	24,110	ID from CBP doc, A portion of the pipe is 14" (SDR 13.5) HDPE (ID 11.8") and another portion is 12" Basalt lined CS (ID 11.93") so 11.8" is used for conservatism
4. Boiler Room Sump Discharge to the Crossover								
4-01 - Unit 1 Boiler Room Sump Discharge to Crossover	CS Polyurethane-lined pipe (assumed STD)		12	756	0.79	593.37	4,443	Assumed the same ID as Carbon Steel STD pipe
4-02 - Unit 2 Boiler Room Sump Discharge to Crossover	CS Polyurethane-lined pipe (assumed STD)	1 12	12	480	0.79	376.99	2,823	Assumed the same ID as Carbon Steel STD pipe
4-03 - Unit 3 Ash Hopper Pit Sump Discharge to Crossover	Sch. 40	10	10.02	53	0.55	28.75	215	
4-04 - Units 1 and 2 Boiler Room Sump Crossover Piping to South Pond	HDPE / Basalt Lined	12	11.8	8130	0.76	12,348.44	92,465	ID from CBP doc, A portion of the pipe is 14" (SDR 13.5) HDPE (ID 11.8") and another portion is 12" Basalt lined CS (ID 11.93") so 11.8" is used for conservatism
4-05 - Unit 3 Ash Hopper Pit Sump Crossover Piping to South Pond	HDPE / Basalt Lined	12	11.8	3540	0.76	2,688.40	20,131	ID from CBP doc, A portion of the pipe is 14" (SDR 13.5) HDPE (ID 11.8") and another portion is 12" Basalt lined CS (ID 11.93") so 11.8" is used for conservatism
5. Total Volume of Piping		1	<u> </u>	l	1		484,803	The sum of all volumes above

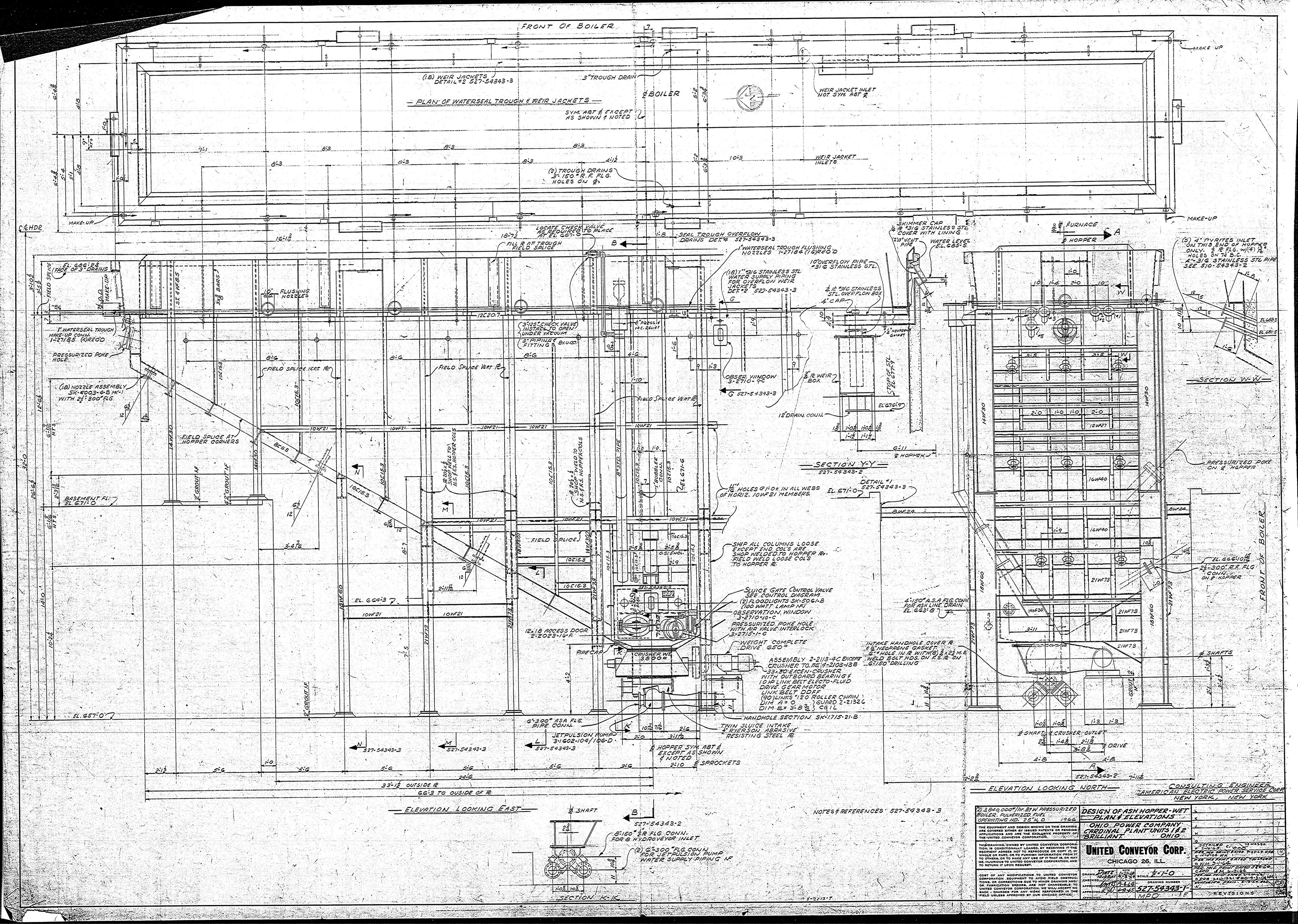


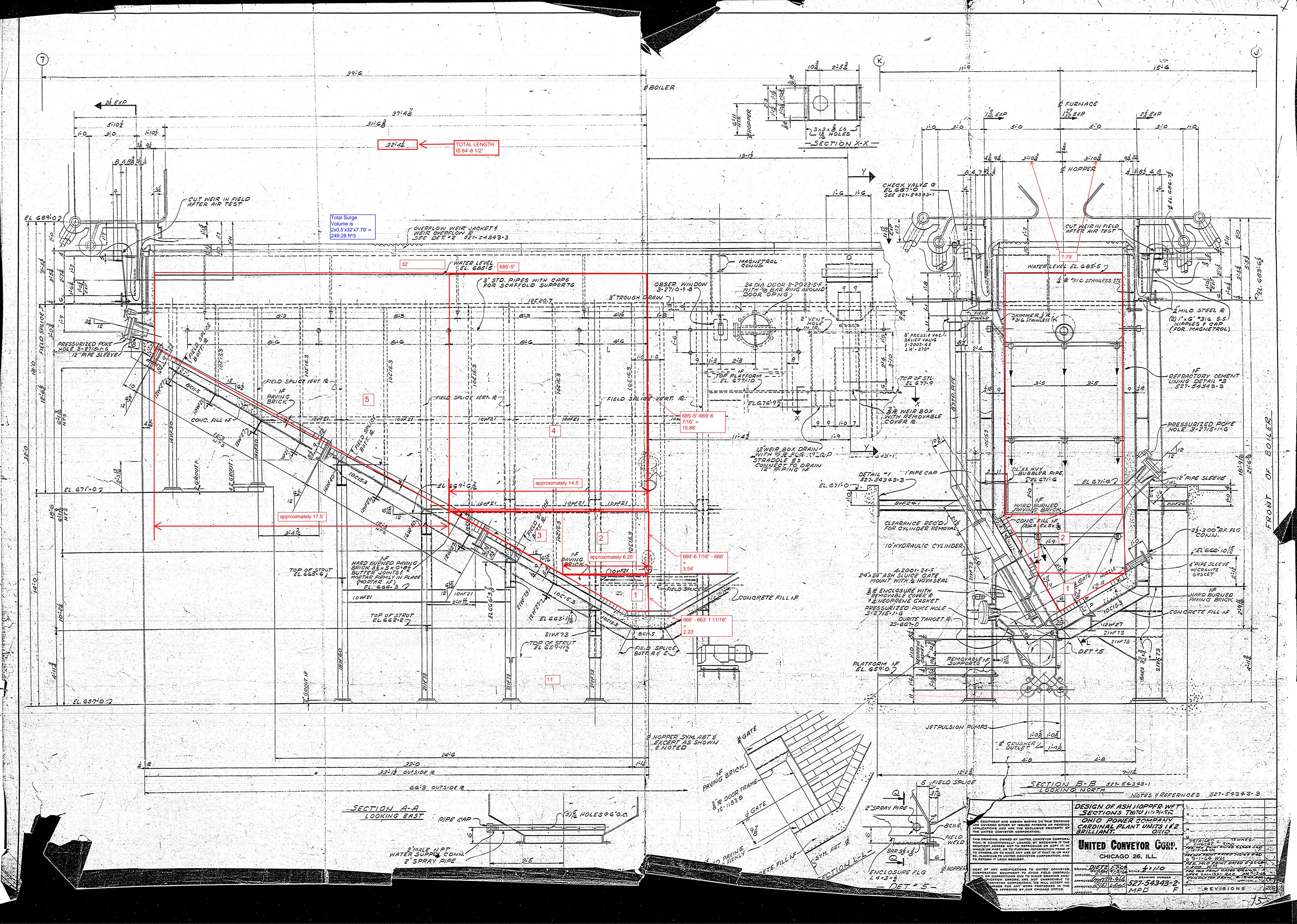
PROJECT NO. 13770-006 Date: 15 August 2023

8.02 U1 & U2 Bottom Ash Hopper Volume



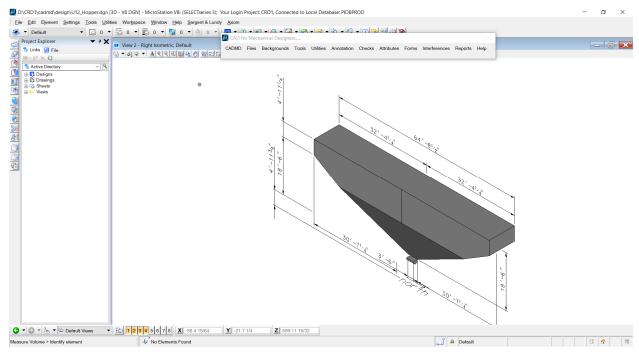


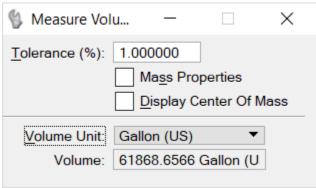




Unit 1/2 Bottom Ash Hopper Wetted Volume = 61,870 gallon

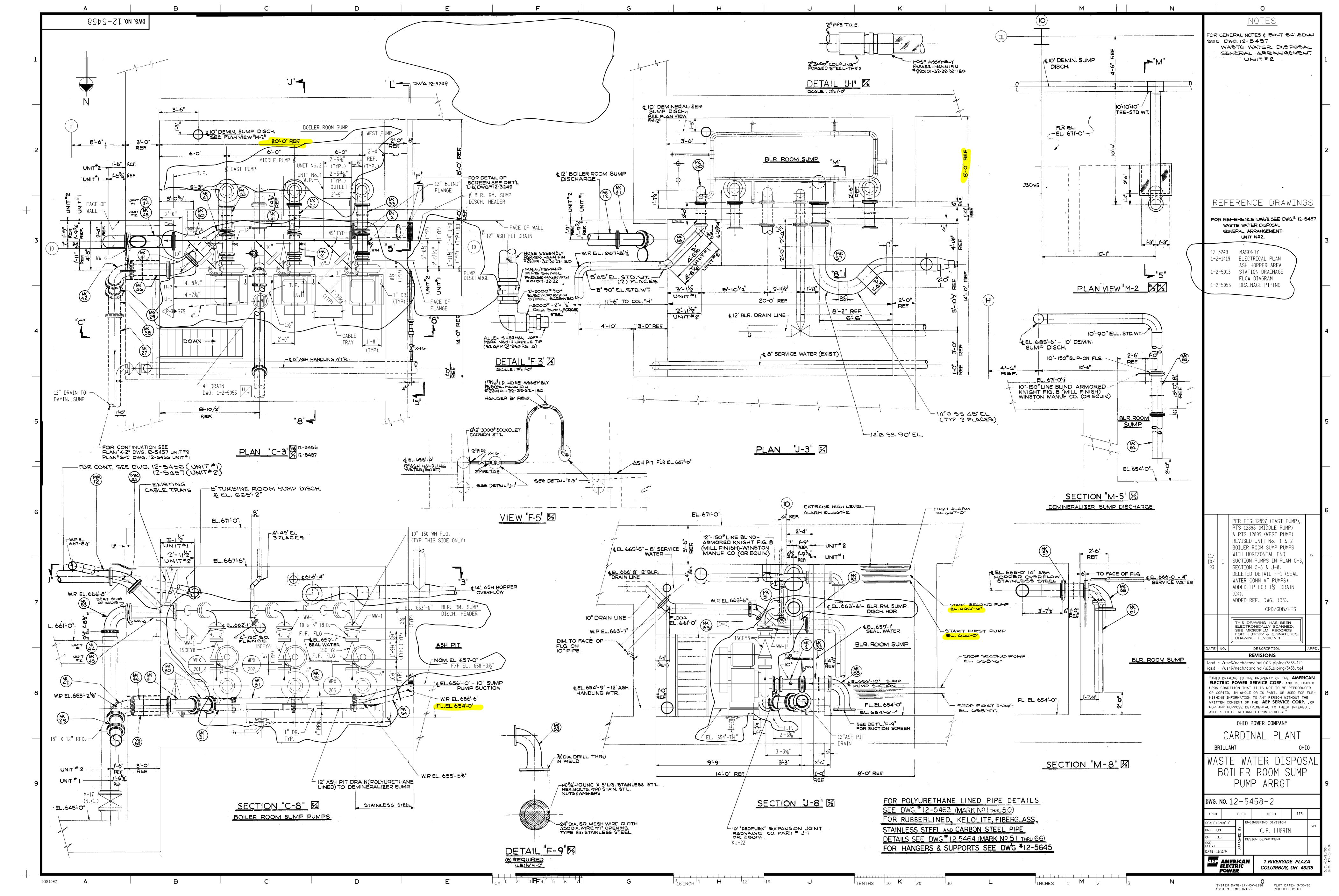
Filename: U12_Hopper.dgn

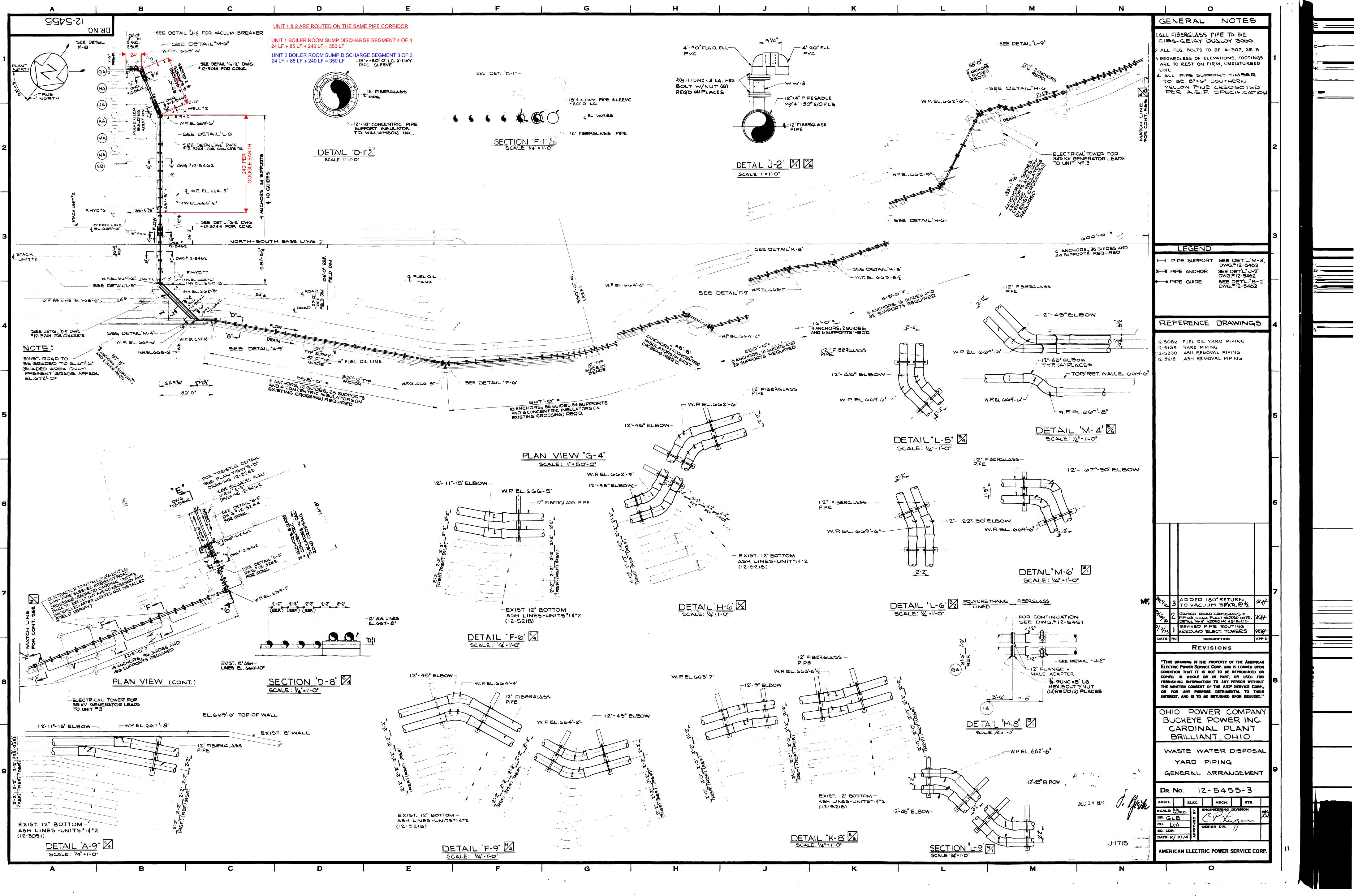


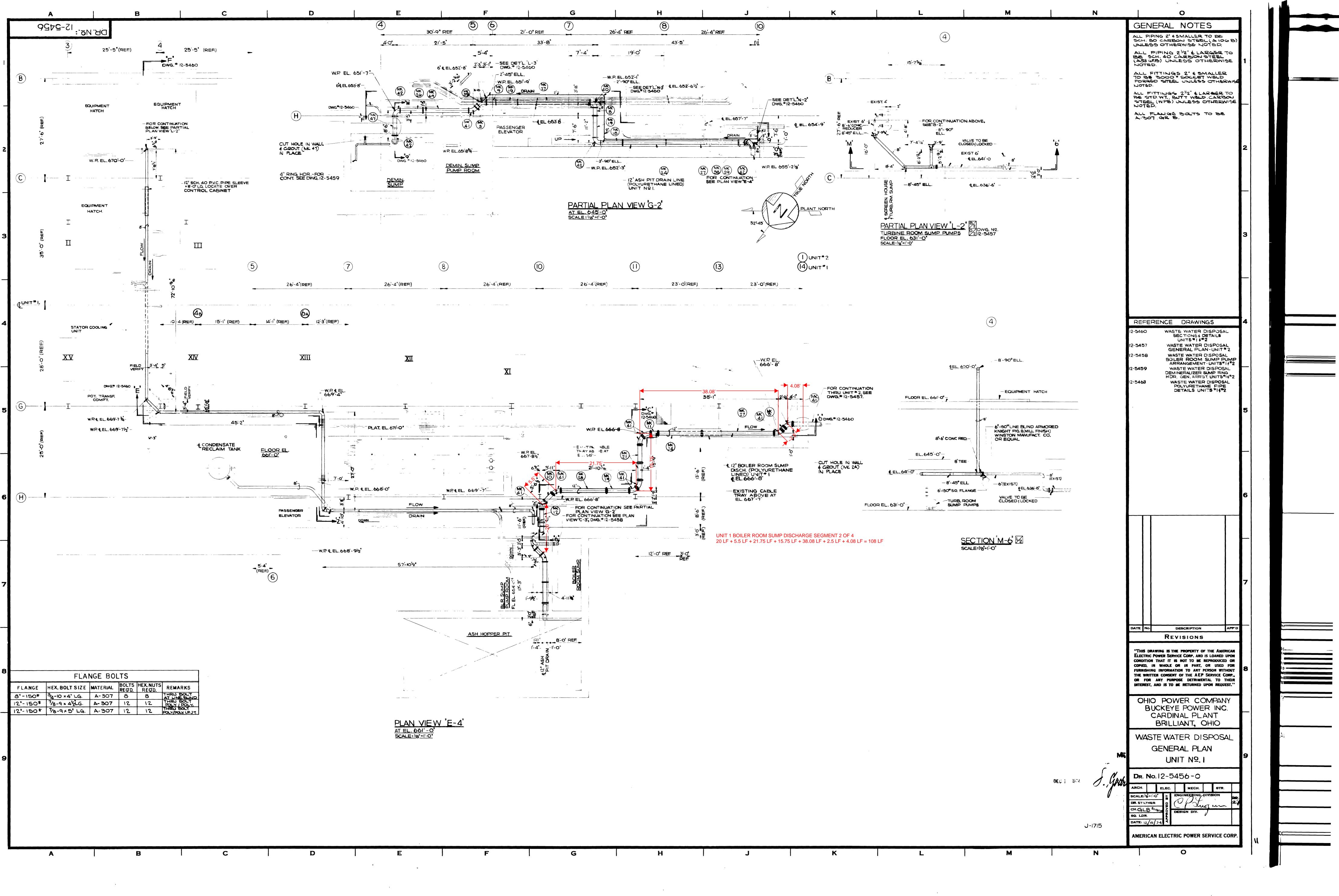


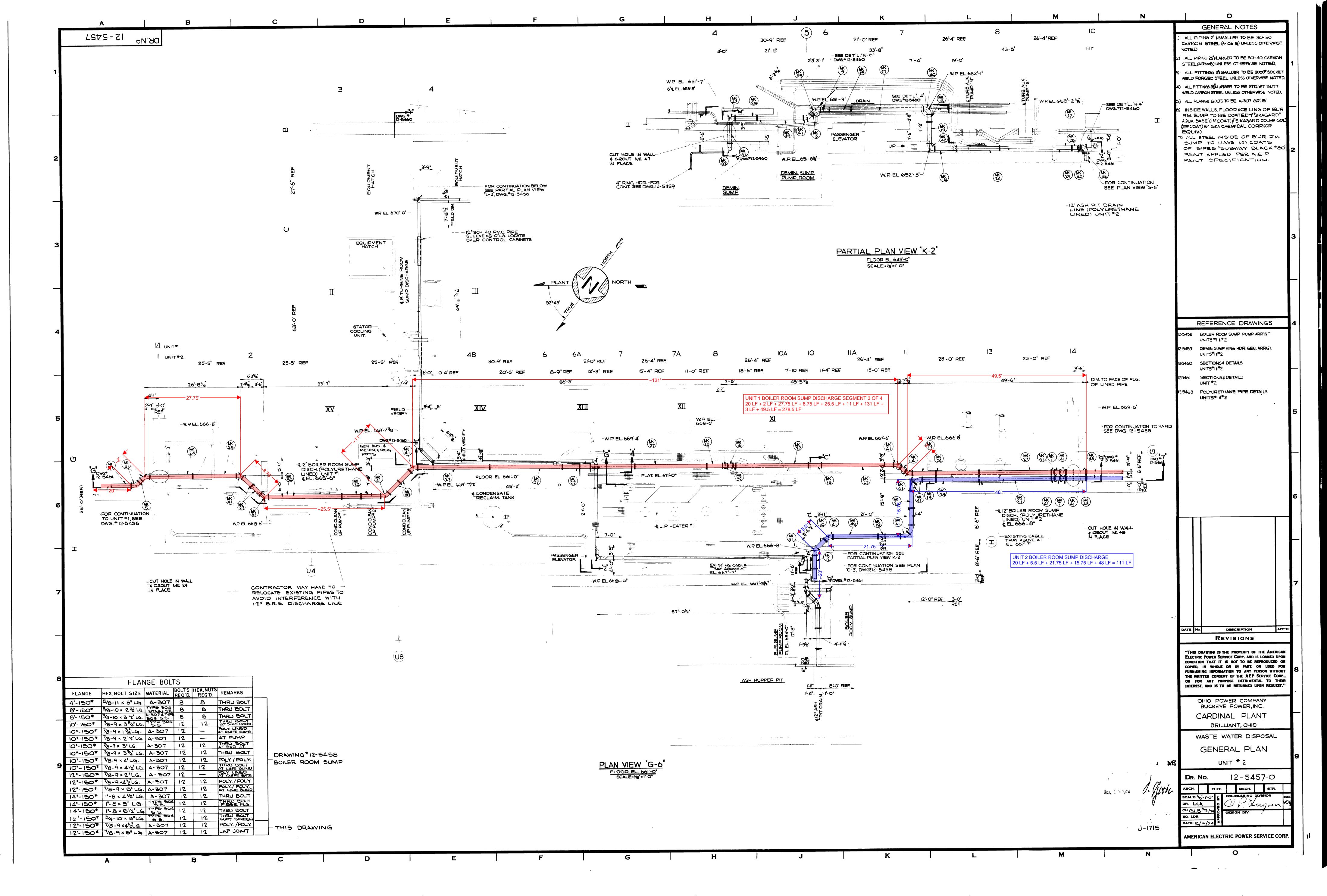


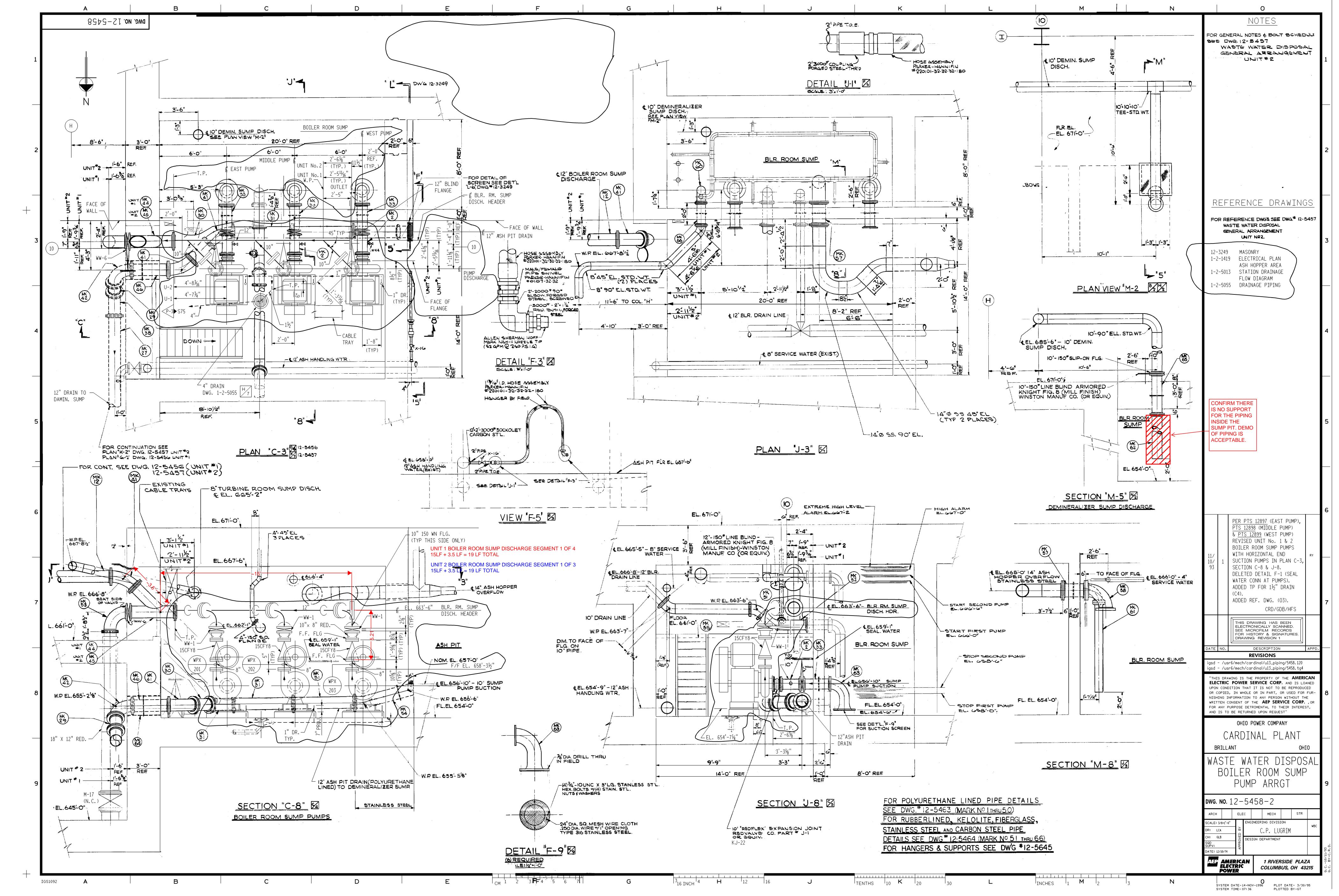
8.03 U1 & U2 Boiler Room Sump





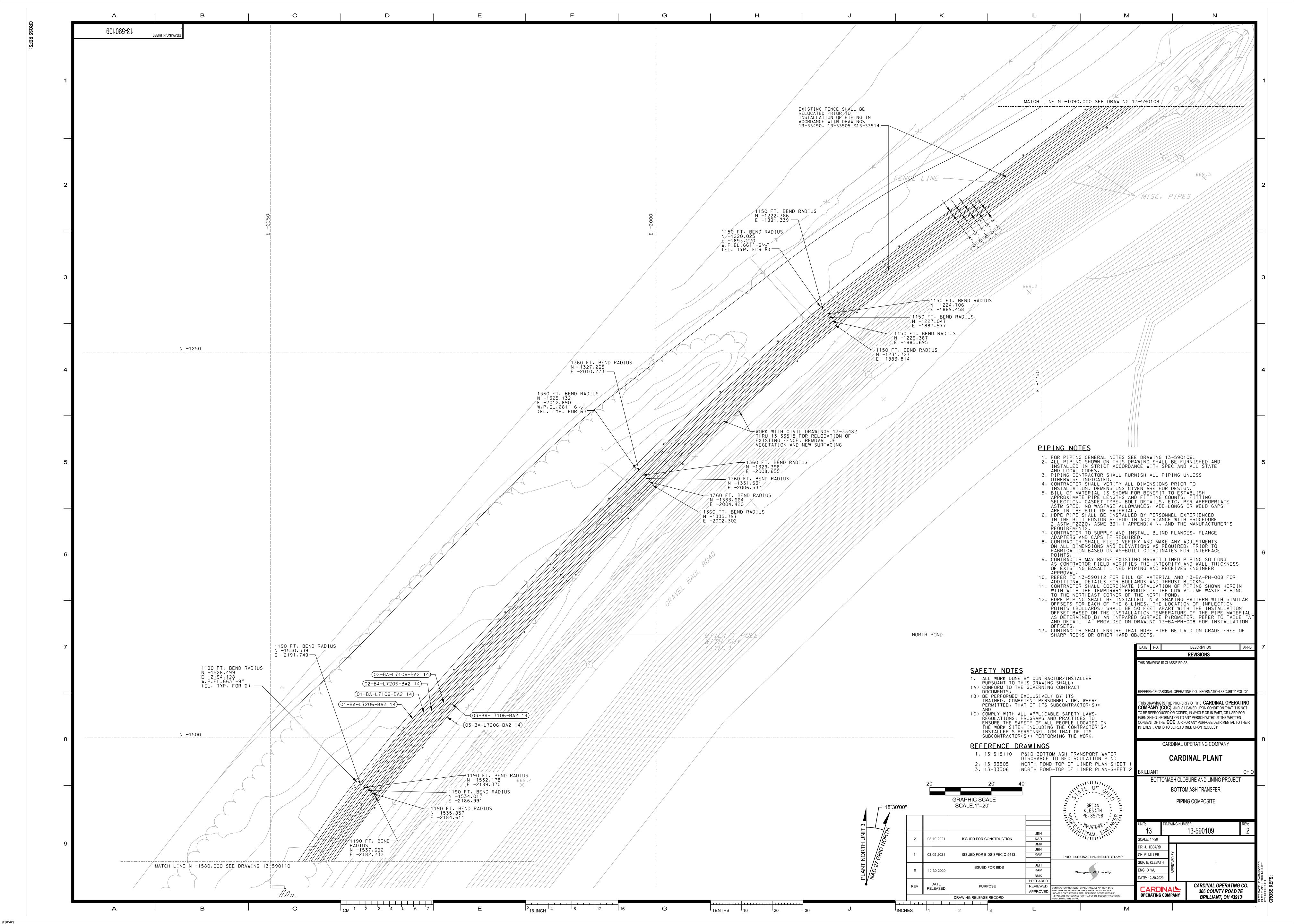


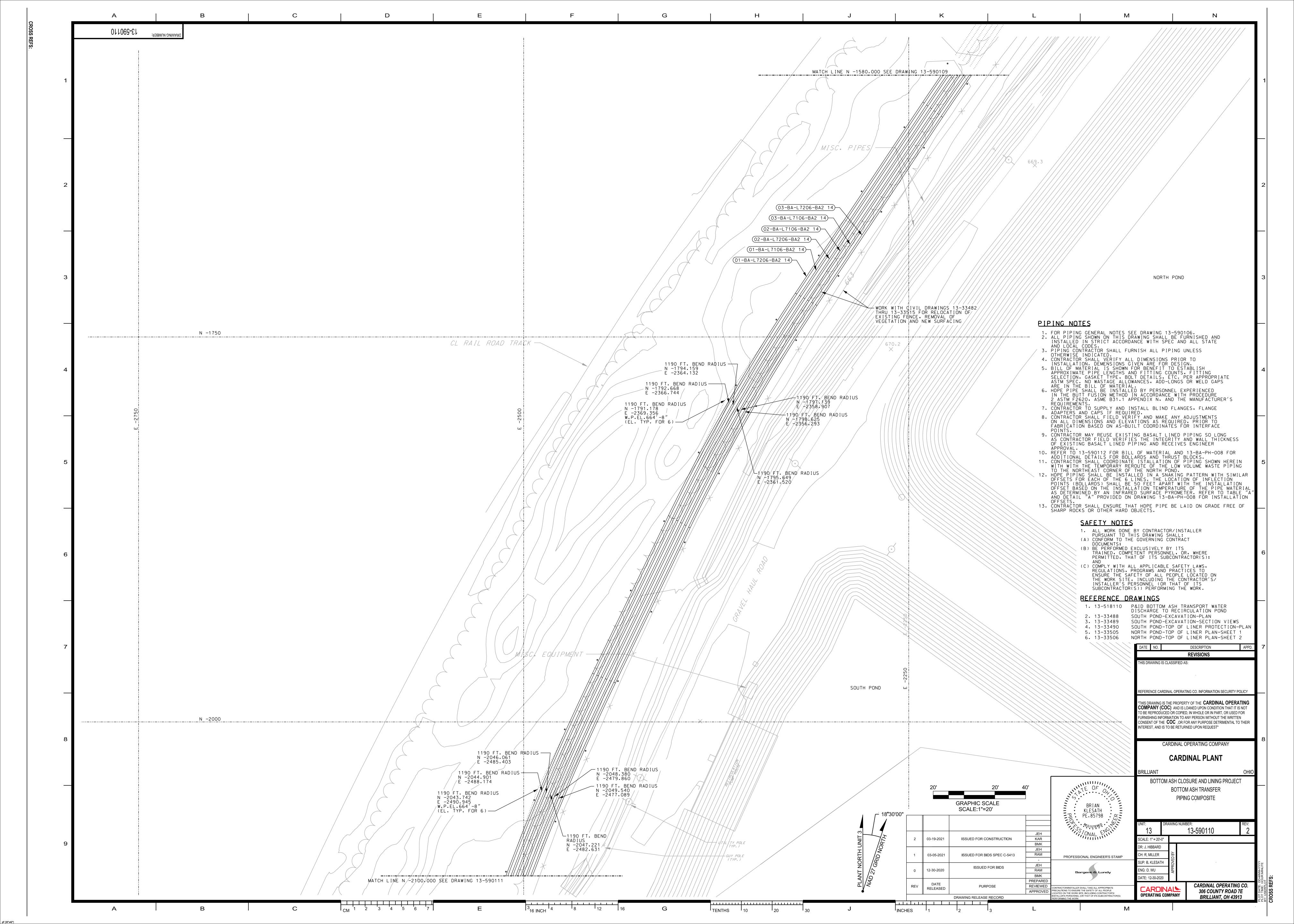


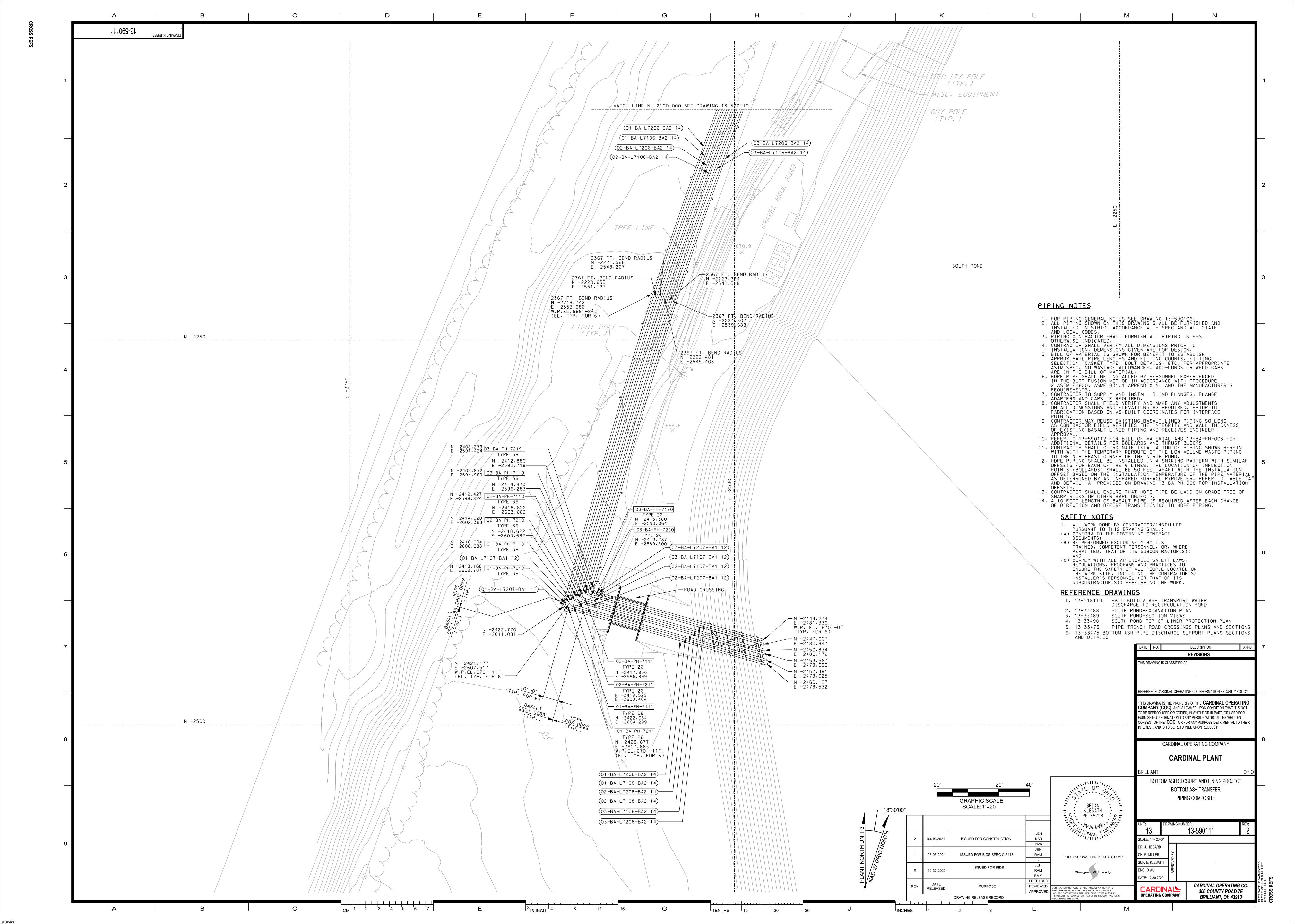


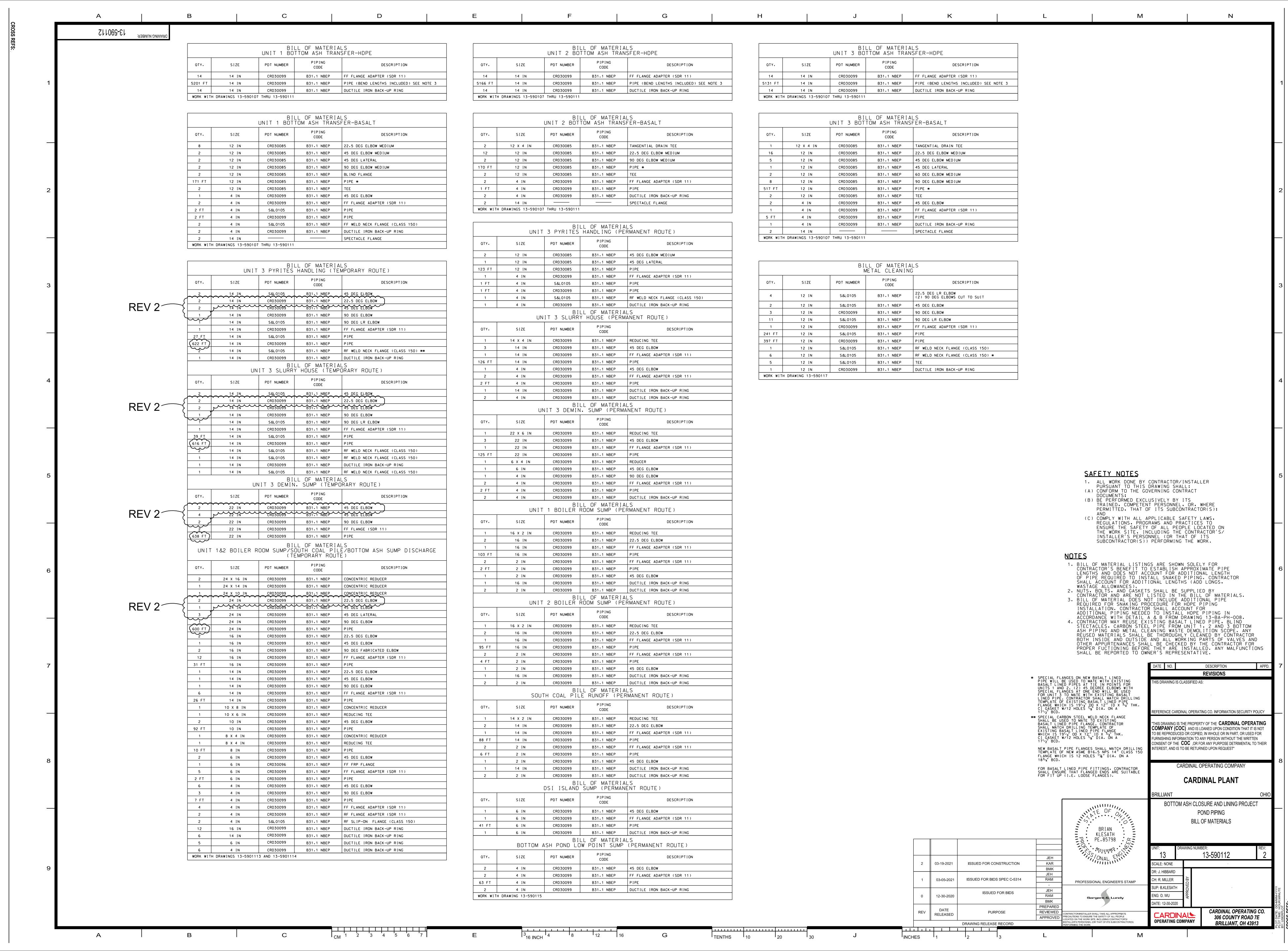


8.04 U1, U2 & U3 Bottom Ash Piping Isometrics











8.05 U3 Bottom Ash Hopper Volume

Article Number = CD-3-01-16 Article Status = Series = 600 Plant = Cardinal Unit = 3 Volume = 1 Section = a TabTitle = Steam Generating Equipment

Title = Bottom Ash Removal System

March 5, 1992 Descriptive Article C-3-1-16

Cardinal Plant Unit 3

BOTTOM ASH REMOVAL SYSTEM

Reference Illustrations: Figs. C-3-1-16-1 and C-3-1-16-2

The bottom ash removal system consists of an ash hopper with two hydraulically operated ash gates, two 10 hp motor driven ash crushers, 32 slope jetting nozzles, two door jetting nozzles, two emergency jetting nozzles and two jet pulsion pumps. Each jet pump transports the ash through its own discharge line to the ash disposal area located on the plant property. The system is designed for the removal of ashes once per shift.

Ash Hoppers

Each of the ash hoppers is a refractory lined, steel plate structure supported from the floor of the building. The hopper extends across the full width of the boiler and is located directly under the throat formed by the sloping furnace walls.

Since the steam generator hangs from the structural steel at the top of the building and expands downward, while the ash hopper is supported from below, it is necessary to allow for vertical expansion of approximately 13" and still maintain a gas tight joint between the steam generator and the ash hopper. This is provided for by a water seal consisting of a water filled box or trough attached to the top periphery of the hopper.

A vertical plate or skirt hangs from the lower furnace wall inlet header into the seal trough and expands downward forming a water seal. The seal trough and skirt extend around the entire periphery of the ash hopper. The skirt is made of stainless steel to provide protection against heat and corrosion.

A header around the ash hopper supplies makeup water to the seal trough from twenty nozzles located in each corner and the sides and ends. These nozzles are positioned to circulate water around the seal trough in a counterclockwise direction when viewed from above. See Figure C-3-1-16-2.

The makeup water provided to the seal trough is low head ash service water which is normally supplied by the ash water recirculating pumps. A backup source of low head ash service water is from the river water makeup pumps.

In addition the seal trough makeup nozzles can be flushing nozzles by opening a 6" air operated valve (3WA-032) from the high head ash service water supply. This should be operated once daily for approximately 5 minutes to flush the

bottom of the seal trough clear of silt and sediment.

Except when dewatering the ash hopper for inspection, the hopper should be maintained full of water to protect the refractory lining. The water also breaks the fall of large pieces of hot slag which shatter upon contact with the relatively cool water. Refractory cooling water is distributed continuously from a perforated stainless steel spray pipe installed on top of the refractory wall and extending around the complete periphery of the hopper. This is done to keep the refractory which is exposed above the normal water level wet and cool. This water also replaces losses from evaporation and ash gate leakage.

The perforated spray pipe is divided into 14 independent sections, each supplied by a separate line from the low head ash service water system (see above). Each line has an orifice installed to limit the flow of water and to prevent shutting off all flow. A pressure regulating valve (3WA-036) can be bypassed if additional cooling or flushing water flow is desired. See Figure C-3-1-16-2. Dividing this cooling water spray pipe into separate sections guards against damage to all refractory should the water supply be lost to a pipe due to a plugged orifice or line.

Excess water in the ash hopper flows through two normal and one emergency overflow "skimmer caps" each with an 8" stainless steel pipe to a weir box then on to the ash hopper sump. Normally, the refractory cooling water flow to the hopper is in excess of gate and evaporation leakage losses. This results in a continuous flow of water from the overflow weir box to the ash hopper sump.

When ashes are being removed from the hopper, the water level will drop a few feet; the hopper may be left in this condition allowing water level to be restored by the normal flow of refractory cooling water. When the hopper has been dewatered for inspection or some other reason, it should be promptly refilled at least until the sloping floors are covered using the jetting nozzles. Then if desired, the remaining portion can be allowed to fill from the normal flow of refractory cooling water.

Slope jetting nozzles are provided to help move the ashes down the sloping floors of the hopper to the gate openings. There are slope nozzles on each of the outboard slopes. Each nozzle is sized to deliver 80 gpm at 125 psi. Two regulating valves, one for each slope, control water flow to the nozzles. These valves are operated from switches mounted locally on a subpanel in the ash pit.

There is one door jetting nozzle on each wall of the hopper. These nozzles are directed to flush ashes through the gate on the opposite wall. Flow to the door jetting nozzles is regulated by two valves. The door jetting nozzles are operated from switches on the ash handling subpanel.

One emergency jetting nozzle is provided for each ash gate and is located inside the grinder encloser opposite the ash gate. These are to be used when the gates fail to close due to an obstruction. Flow to the emergency jetting nozzle is regulated by local air operated control valves located near the clinker grinder enclosure.

The ash water mixture is discharged from either side of the ash hopper through one of two air and hydraulically operated gates. Filtered water and 100 psi air for operating the ash gates is supplied from the filtered water head tank and the plant air system. Each gate is controlled by a manually operated 4-way valve mounted on the ash gate enclosure. The position of each gate can be determined by observing the position of an indicator device mounted on top of the gate enclosure. An observation door and a flood light mounted on the enclosure of each gate permit viewing the gate and crusher.

Large pieces of ash which will not fit through the gate opening can be rodded either through (1) the aspirated lance doors mounted on each gate enclosure or (2) through the lance doors mounted near the top and at each end of the ash hopper or (3) through the lance door mounted above each gate enclosure on the wall of the hopper.

From each ash gate, the ash water mixture flows into the corresponding crusher where the ash is crushed to a size suitable for pumping. The crusher consists of a heavy crushing roll with removable teeth which is rotated against a stationary set of teeth. The shaft of the crusher roll is supported in bearings mounted in a structural frame which is bolted to the outlet flange of the ash gate enclosure. A packing gland around each shaft opening prevents furnace gasses

from leaking out of the furnace housing. Sealing water for the gland is supplied by the seal water pumps from the filtered water head tank.

Each crusher is chain driven through a reduction gear by separate 10 hp, 1780 rpm, 575-volt induction motors. A hydraulic coupling is provided between the motor and reduction gear to prevent overloading the motor or damaging the crusher should scrap iron become lodged between the moving and stationary teeth. The crushers are controlled from the ash handling subpanel. The subpanel contains a control switch marked Forward-Stop-Reverse and a forward-reversing selector switch. Motor current is indicated by an ammeter on the same subpanel. Whenever the crusher motor current rises above normal, indicating that the crusher is stalled, the motor should be reversed to clear the crusher. This is done by turning both switches to the Reverse position. Upon indication of normal current, both switches should be returned to the Forward position to continue discharging ash.

From the crusher, the ash water mixture flows to a jet pump bolted to a transition piece underneath the crusher housing. The jet pump discharges to an ash disposal line running out to the ash disposal area located on the plant property. Only one crusher, the corresponding jet pump and its line are required to remove ashes. A drain valve, located at the outlet of the jet pump, is provided to drain the line during cold weather. This valve should be opened after removing ashes during cold weather. It should be kept closed at all other times, particularly when removing ashes, to prevent the drain line from plugging.

Each jet pump is supplied with water from the bottom ash water pump discharge header, through an air operated valve. The controls for the bottom ash water pumps are located on Panel SV in the control room.

Operating Procedure

The following procedure should be used for operating the bottom ash removal system.

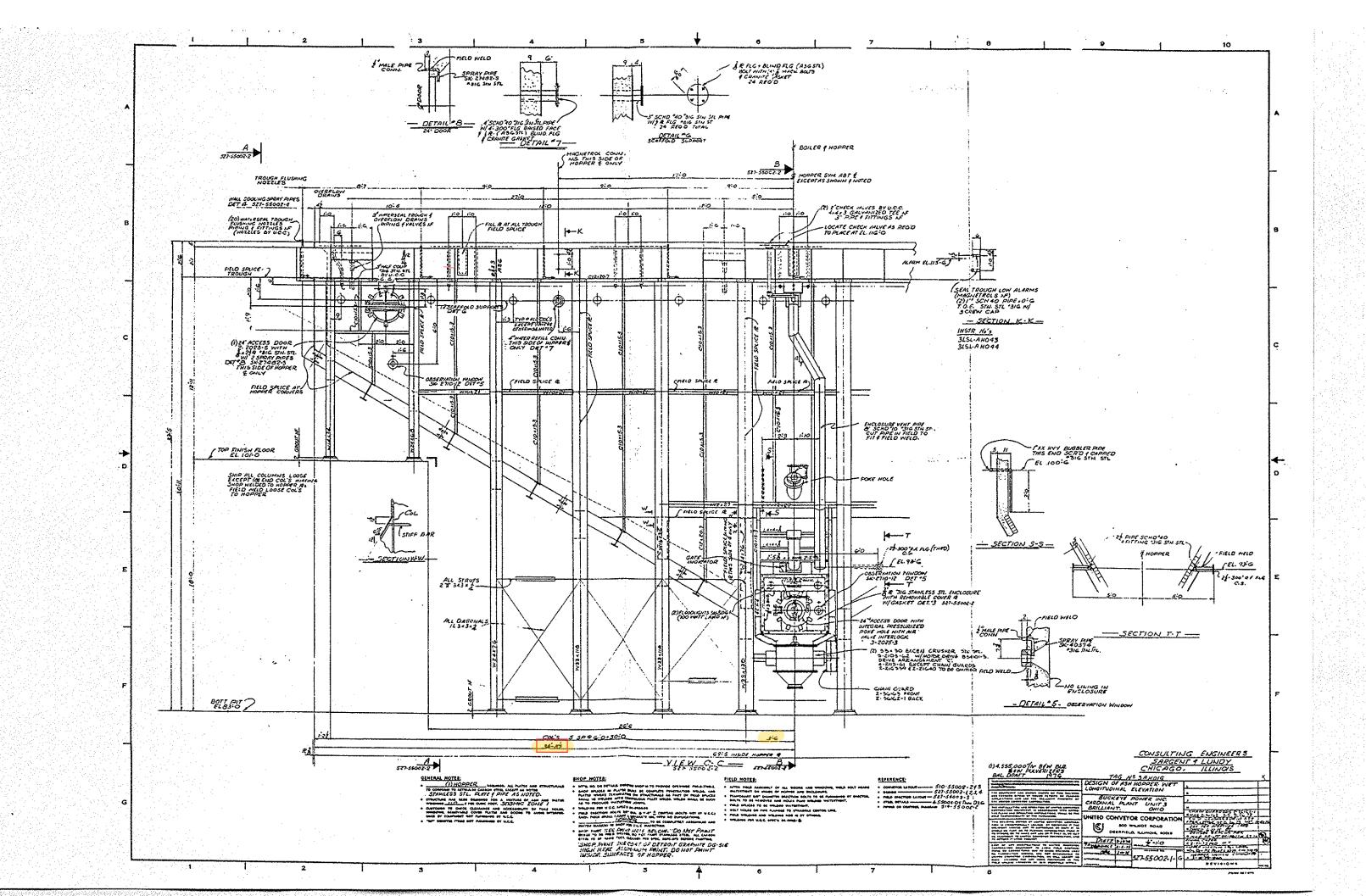
- 1.Start a bottom ash water pump.
- 2. Close the ash line drain valve at the jet pump outlet for one jet pump on each hopper.
- 3. Open the air operated water supply valve to the one jet pump in each hopper that is to be used.
- 4. Observe pressure gages and confirm:
 - a. Adequate water supply pressure to the jet pump (main control room).
- b. Jet pump discharge pressure is less than supply pressure. If pressures are equal, the ash line is plugged (ash pit).
 - 5. Start the ash crusher for the in-service jet pump.
- 6.Open the hydraulic gate wide open with the 4-way valve located on the ash gate enclosure observing the jet pump discharge pressure. Increasing pressure indicates the pumping of ash.
- 7.Immediately open the water supply valve to the door jetting nozzles located on the hopper side opposite the open ash gate. Open the water supply valves to one set of slope jetting nozzles for one minute on each slope. Alternate the two sets of slope jetting nozzles on the hopper until the jet pump discharge pressure decreases indicating removal of all ash.
 - 8. When all ash has been removed, shut off the water to all jetting nozzles, close the ash gates and stop the crusher.
- 9. After a ten minute flush, close the air operated water supply valve to the jet pump and shut down the bottom ash water pump.

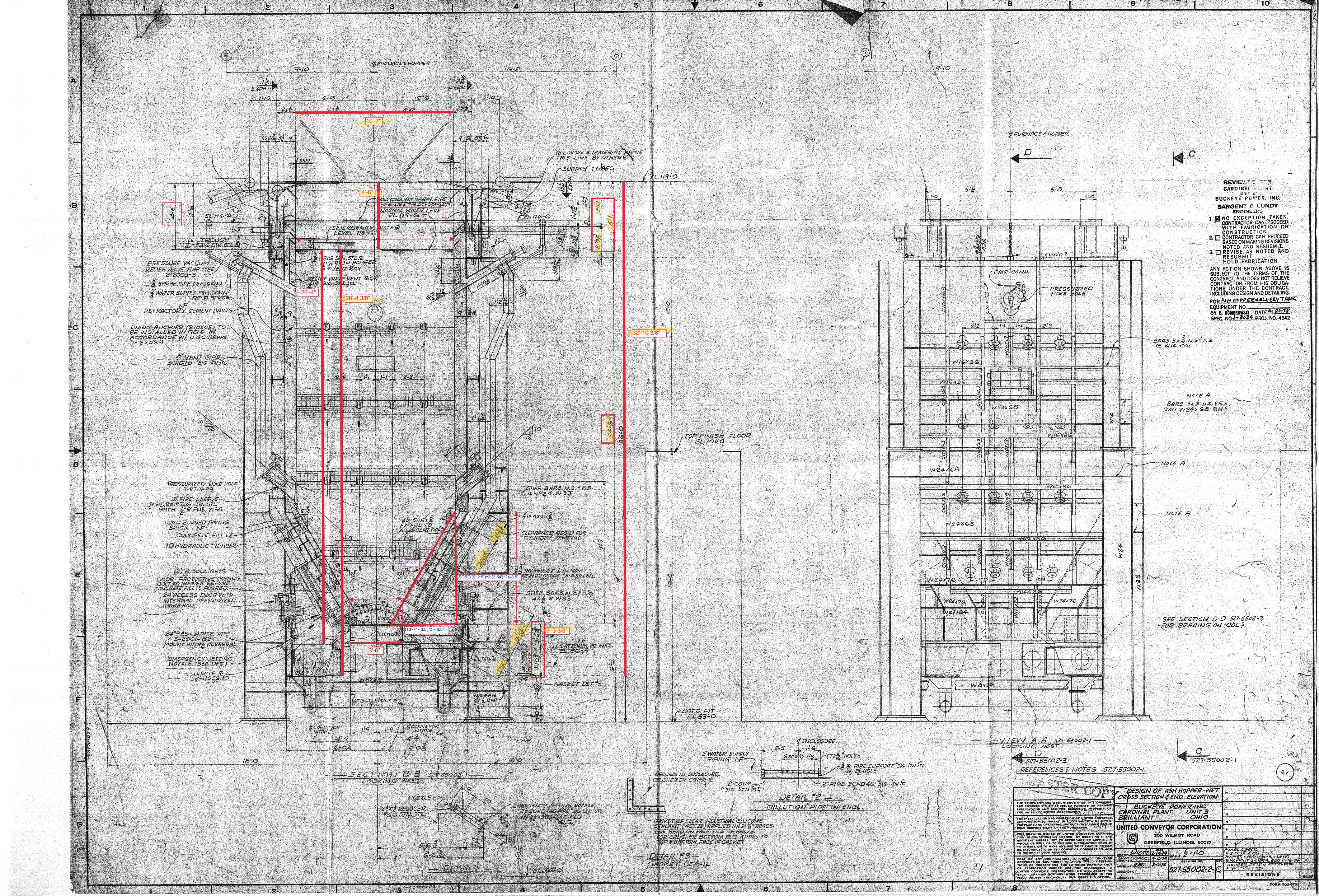
10.In cold weather, open the ash line drain valve located at the jet pump outlet.

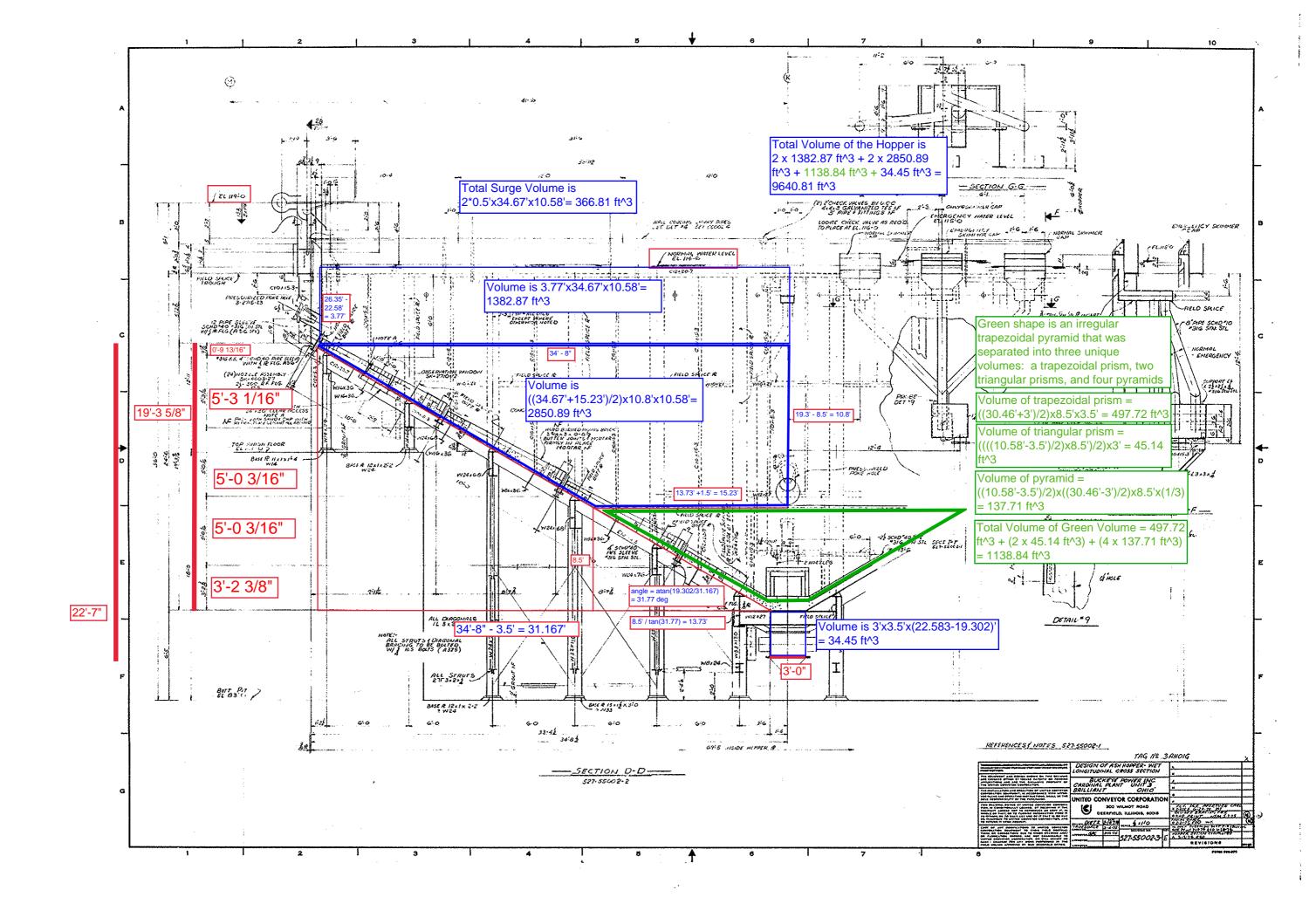
It is recommended that once daily the ash hopper be completely dewatered when using the ash crushers and jet pumps to run bottom ash. This is to be done so that the hopper can be inspected for any large pieces of slag remaining in the hopper. If there are any, the jetting nozzles can be used to dislodge the slag and if necessary, it can be broken up by rodding from the aspirated doors. The hopper should be quickly refilled using the jetting nozzles until the sloping floors of the hopper are covered. The remainder of the hopper can be filled with water from the refractory cooling weirs.

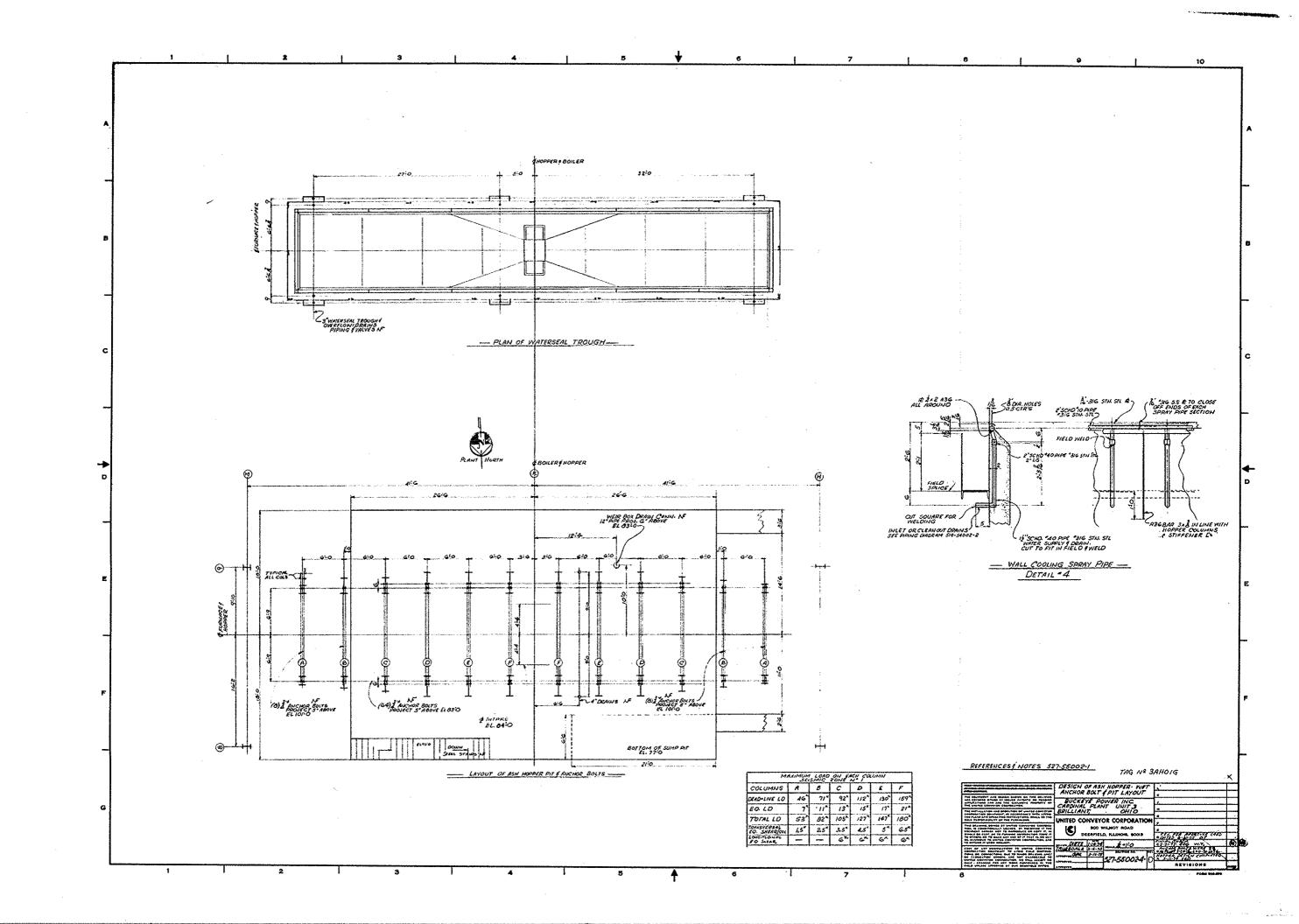
Do not operate any wall slag blowers or IK blowers when removing bottom ash from the boiler and particularly not when the hoppers are empty during inspection. This is necessary to guard against the possibility of dislodging a large piece of slag which could damage the hopper floor due to the low water level in the hopper during these periods.

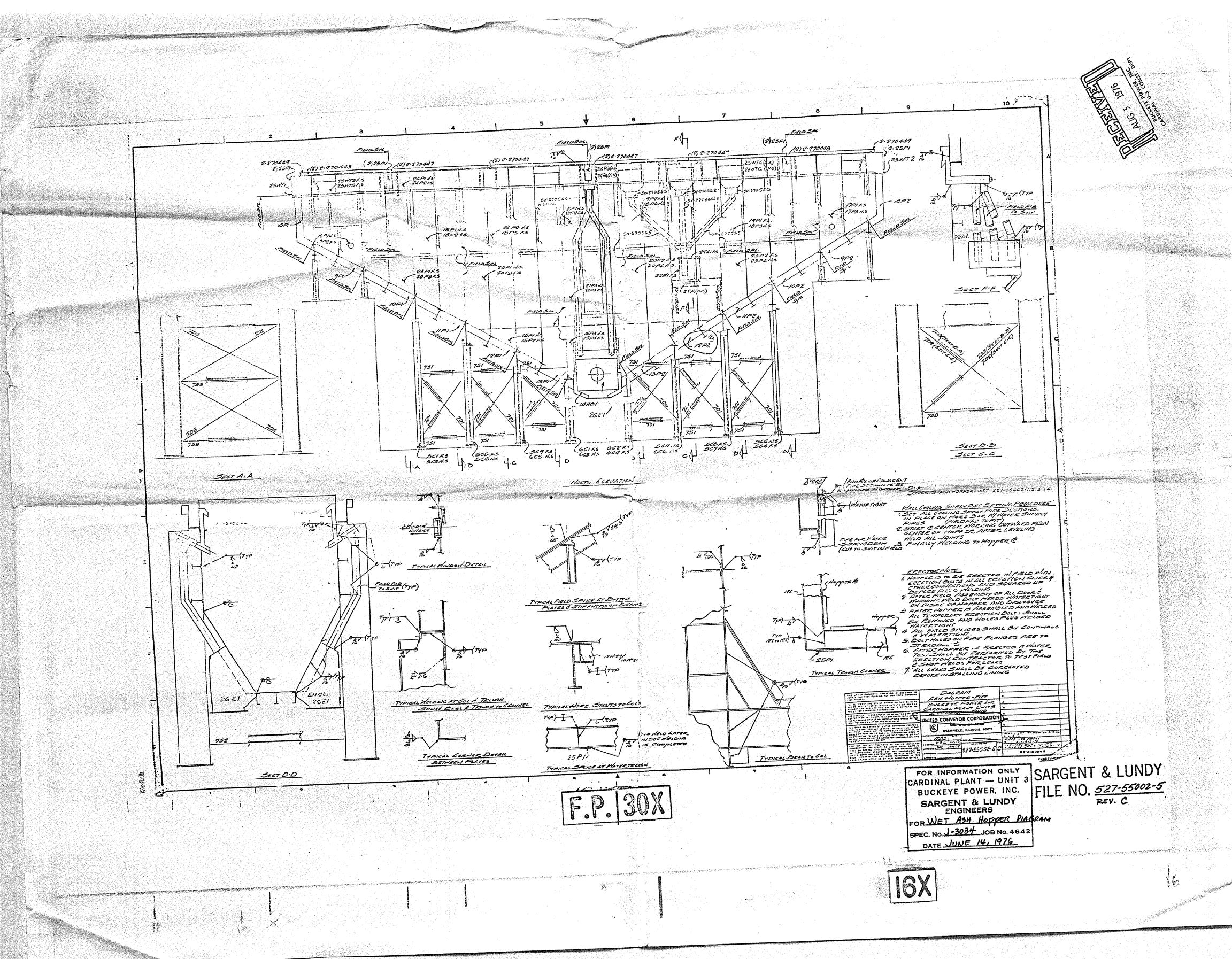
The time required to empty the hopper after eight hours full load operation using a jet pulsion pump is approximately 30 minutes. The storage capacity of the hopper, 9790 cubic feet and 386 tons is such that if no discharge of ash water mixture took place, due to machinery breakdown for example, it would take approximately 45 hours to fill the hopper with slag at full load operation.







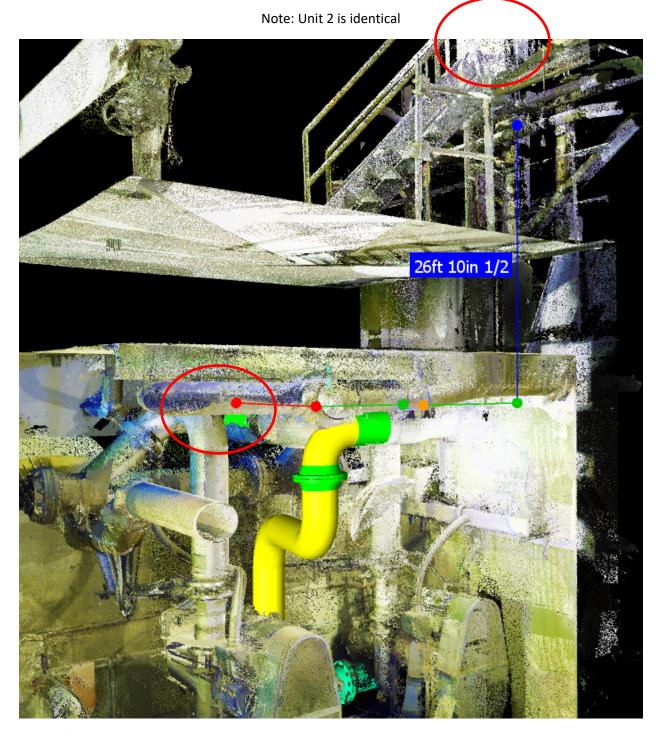






8.06 U1 & U2 Bottom Ash Hopper Overflow Pipe

Unit 1 Bottom Ash hopper Overflow Pipe (From Overflow Box to Boiler Room Sump)



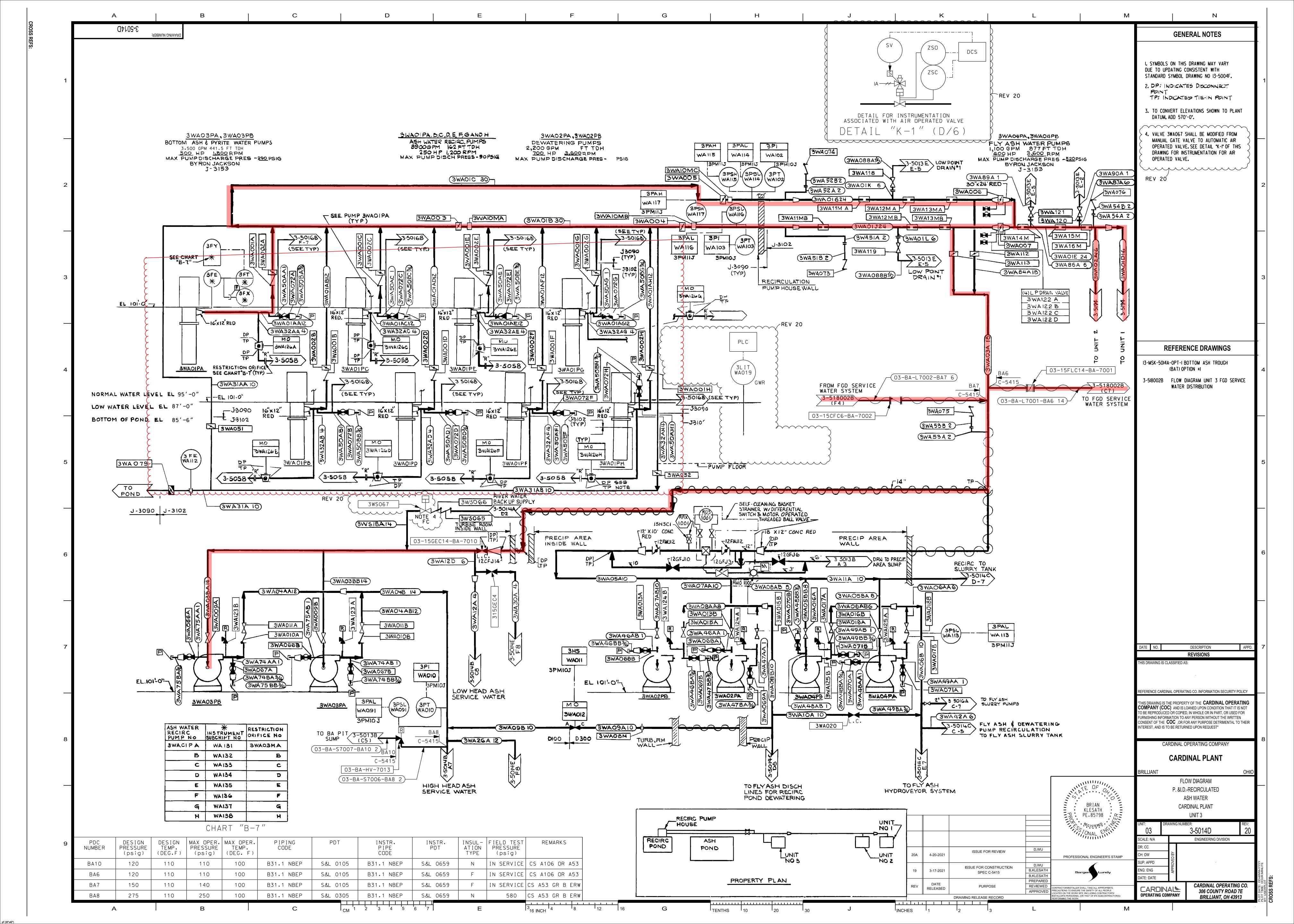
27 LF of pipe

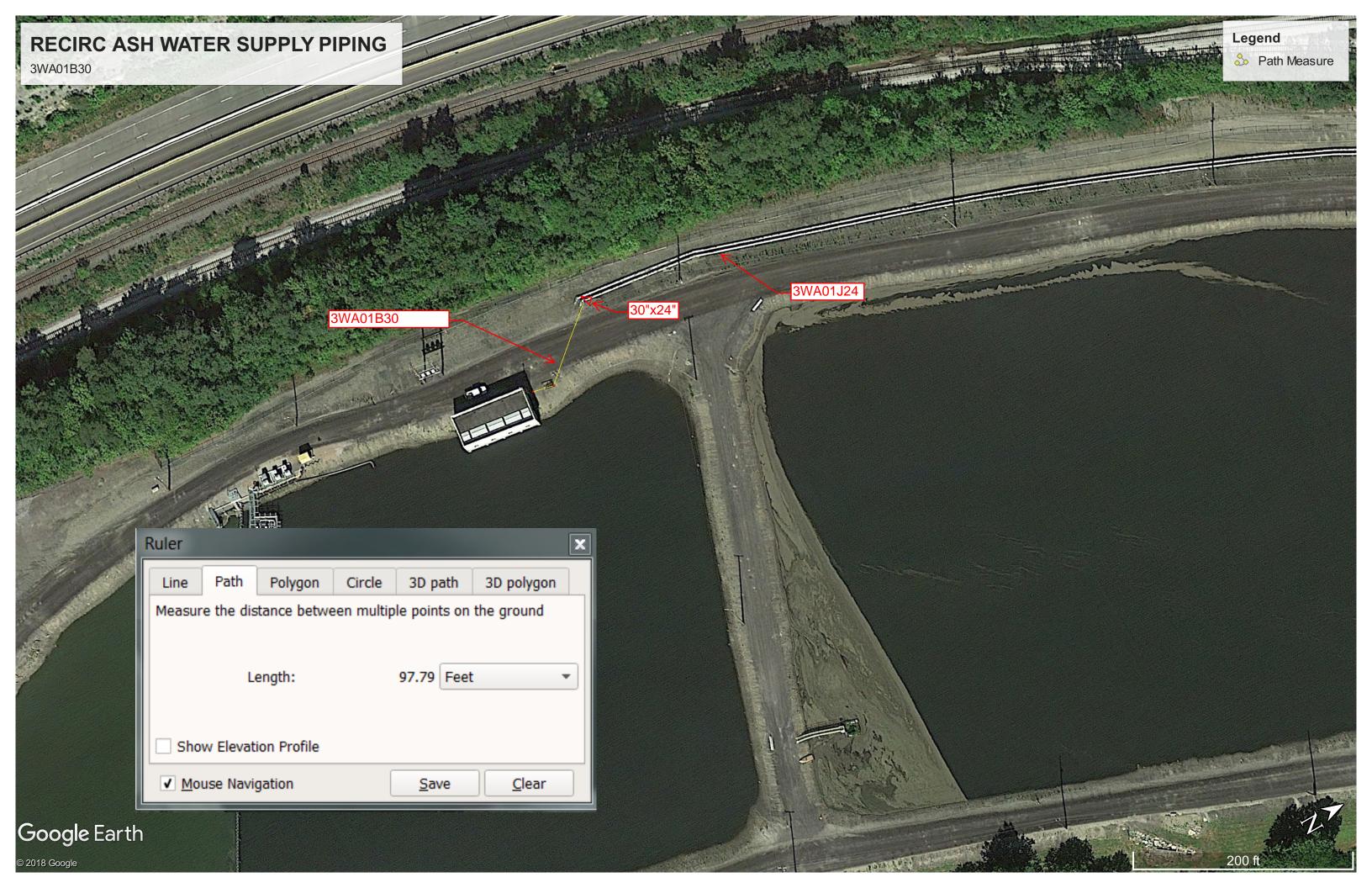
Top Right Circle = Overflow Box

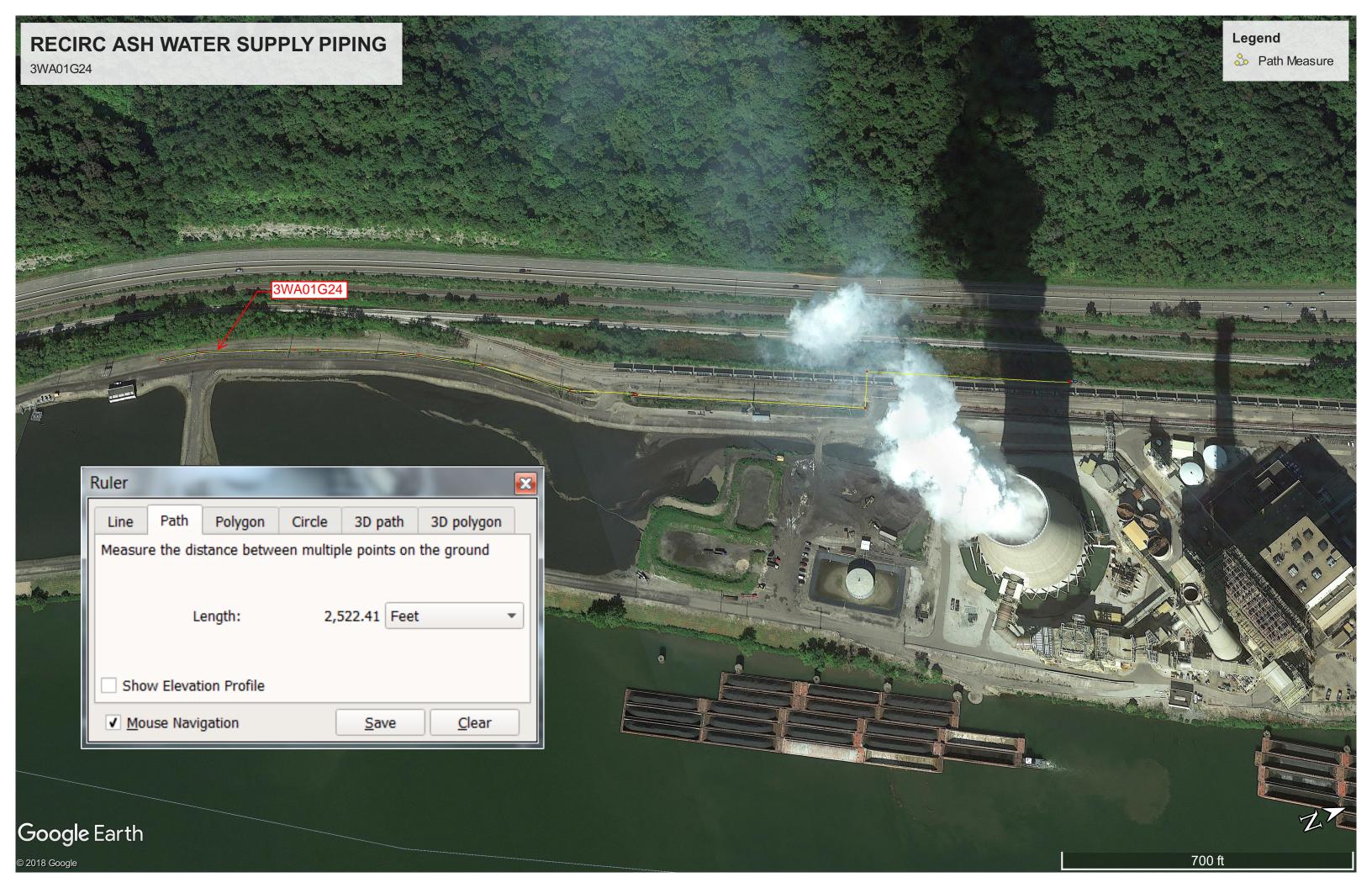
Bottom Left Circle = Connection to Boiler Room Sump



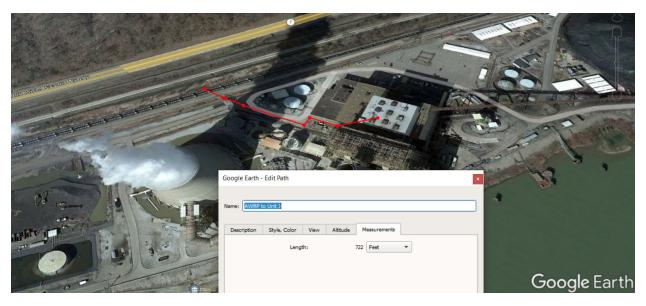
8.07 AWRP Piping drawings and images







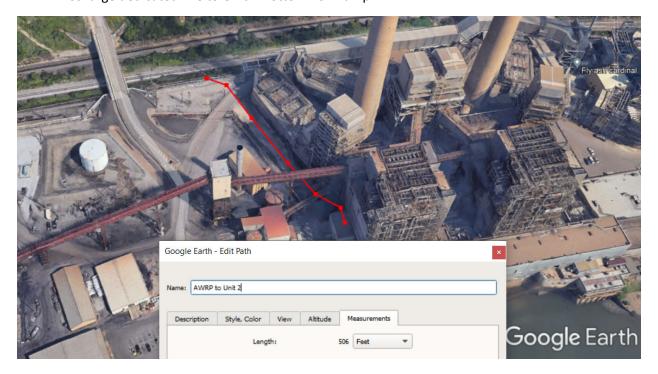
AWRP Discharge dedicated line to Unit 3 Bottom Ash Pump



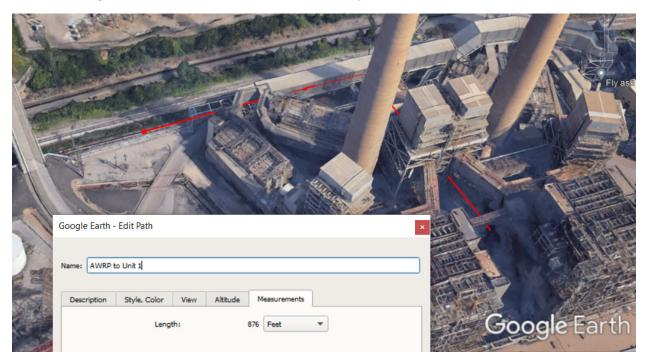
AWRP Common Header to Unit 2



AWRP Discharge dedicated line to Unit 2 Bottom Ash Pump



AWRP Discharge dedicated line to Unit 1 Bottom Ash Pump





8.08 Excel Formulas



=Cover!A21

=Cover!A21									
			•						
1	PURPOSE AND SCOPE:								
1.01	The Cardinal power station consists of three (3) units. Project 13770,006 includes the lining and closure of the existing bottom ash ponds for each units.								
	The purpose of this calculation is to determine the primary active wetted volume of the revised bottom sab system in accordance with ELG regulations in order to estimate the allowance of purge (10% of the primary active wetted bottom sab volume).								
1.02	The purpose of this calculation is to determine the primary active wetted volume of the revised bottom as	n system in accordance with ELCs regulations in order to estimate the allowance of purge (10% of the primary active	wetted bottom ash volume).						
Item	Description	Reference	Unit of Measure	Data Value	Input				
				****	(V/UV/EJ)				
2	DESIGN INPUTS:	-	1						
	ELO Proposed Rule Section 423.11(as), Specialized Definitions, is provided below for basis of included equipment: The term 'primary active weter about man abstraction of the activation of the								
	Impoundments, secondary bottom ash system equipment (e.g., installed spares, redundancies, and maintenance tanks), and non-bottom ash transport systems that may direct process water to the bottom ash.								
=B10+0.01	imponuments, secondary vortion as system equipment (e.g., instatted spares, redundances, and maintenance turns), and nonvortion as a turnsport systems mat may are express mater to the vortion as n.								
=B11+0.01	The specific gravity of the water is 1,00 and the density is 62.4 lb/ft3.								
=B12+0.01	Units 1 & 2 Ash Hopper and Seal Trough volumes are determined per drawings in Attachment 8.02.				EJ V				
=B13+0.01	Units 1 & 2 Asia riopper and sear riough volumes are determined per drawings in Attachment 8.02. Units 1 & 2 Boiler Room Sump volume is determined per drawings in Attachment 8.03.				v				
=B14+0.01	The pipe length for Units 1 & 2 overflow piping to the Boiler Room Sump is determined per Attachment	9.00			v				
=B14+0.01 =B15+0.01	Unit 3 Ash Hopper and Seal Trough volumes are determined per drawings in Attachment 8.05.	0.00.			v				
=B15+0.01 =B16+0.01	Unit 3 Ash Hopper and Sear Trough volumes are determined per drawings in Attachment 8.05. Unit 3 Ash Hopper Pit Sump volume is determined per drawings in Attachment 8.09.				v				
	Onit 3 Ash Hopper Pit Sump volume is determined per drawings in Attachment 8.09. Ash Water Recirculation Pump (AWRP) Pipe lengths were determined using drawings and Google Earth	:							
=B17+0.01					EJ				
=B18+0.01	Units 1, 2 & 3 Bottom Ash water piping volume is determined per the Bill of Materials in Attachment 8.0	14.			V				
=B19+0.01	Routing for the piping from the Units 1 & 2 Bottom Ash Pumps to Jet Pumps is determined using Attachn				V				
=B20+0.01	Routing for the piping from the Unit 3 Bottom Ash Pumps to Jet Pumps is determined using Attachment 8				V				
Item	Description	Reference	Unit of Measure	Data Value					
3	ASSUMPTIONS:								
=B23+0.01	Unit 3 overflow piping to the Ash Hopper Pit Sump is assumed the same length as the Units 1 & 2 overflo				EJ				
=B24+0.01	For all three (3) Units, bottom ash hopper surge volume was taken at high water level, 6" above normal op-	perating level.			EJ				
=B25+0.01	Seal Trough is assumed to be 6" deep and extends 6" around the ash hoppers.				EJ				
	The South Pond was not considered part of the primary wetted volume, however, it is considered part of the	he surge volume. The South Pond has 5 feet freeboard so an assumed depth of 5 ft is used based on total pond volume	e for a total of 33.9 sere-feet (based on an a	average nond area of 6.78 acres)	EJ				
=B26+0.01	The bount one was not consucred part of the primary wester volume, nowever, it is consucred part of the	the stage volume. The south Folke has 5 feet necessate to an assumed deput of 5 K is used based on total point volume	e for a total or 55.5 acre reet (oasea on all a	relage pola area of 0.70 acres).	Ed				
	It is assumed that the last 50 ft of piping for the AWRP discharge lines for each Unit is the lower diameter piping (14* nominal for Unit 3 and 12* nominal for Unit 3 and 12* nominal for Unit 3 and 12* nominal for Unit 1 and 21.								
=B27+0.01	(0.01 It is assumed that the last 30 it of piping for the AWKP discharge times for each Unit is the lower distinctor piping (14 nominal for Units 1 and 2).								
Item	Description	Variables		Data Value					
	•								
4	METHODOLOGY & ACCEPTANCE CRITERIA:								
*	The methodology for performing the calculations involves the following principal steps:								
	The methodology for performing the calculations: involves the following principal steps: - Identify all quignents and princip percept doe routine as what extreme drainer ported part operation and ash handling processes.								
=B30+0.01	- Mentity all equipment and priping expected to contain any water during normal plant operation and sish handling processes Determine the Volume of all destribute designment and priping the single designment and priping the designmen								
	Volume of Rectangular Prism	V = Volume [ft3]							
	Totalic of rectangular From	I = Length (ft)							
		w = Width (ft)		V = lwh					
=B31+0.01		h = Height (ft)							
	Volume of Triangular Prism	V = Volume [ft3]							
	*	I = Length (ft)		, , , , , /1\					
		w = Width (ft)		$V = lwh\left(\frac{1}{2}\right)$					
=B32+0.01		h = Height(ff)		(2)					
	Volume of Trapezoidal Prism	V = Volume [ft3]							
		B1 = Base 1 (ft)		4					
		B1 = Base 1 (ft) B2 = Base 2 (ft)		$V = \left(\frac{B_1 + B_2}{2}\right)hd$					
		h = Height (ft)		v - (2) mu					
D22 - 0 01		d = Depth (ft)							
=B33+0.01	11								
1	Volume of Pyramid	V = Volume [ft ²]		/huk\					
		h = Height (ft)		$V = \left(\frac{lwh}{3}\right)$					
		l = Length (ft) w = Width (ft)		. (3)					
=B34+0.01		3.7							
	Volume of a pipe	V = Volume [ft3]							
		π = Constant (3.14)		$V = \pi r^2 L$					
		r = Internal Pipe Radius (ft)		r - A: L					
=B35+0.01		L = Length (ft)							

Wetted Volume Calc_Rev0.xism 1 of 2



=Cover!A21

=Cover!A21								
Item	Description	Reference	Unit of Measure	Equation				
	CALCULATIONS:	Militare	Unit of Measure					
5.01	See Attachment 8.01 for wetted volume summary breakdown							
Item	Description	Reference	Unit of Measure	Value	Accept (Y/N)			
6	RESULTS:	+						
6.01	Wetted volume of equipment and piping							
=B43+0.01	Units 1 & 2 Ash Hoppers	Attachment 8.02	gal	=Equipment!19*2	Y			
=B44+0.01	Units 1 & 2 Seal Trough	Assumption 3.05	gal	=Equipment!I10*2	Ý			
=B45+0.01	Units 1 & 2 Overflow Piping	Attachment 8.06	gal	=Equipment!I12*2	Ý			
=B46+0.01	Units 1 & 2 Boiler Room Sump	Attachment 8.03	gal	=2*Equipment!I13	Ý			
=B47+0.01	Unit 3 Ash Hoppers	Attachment 8.05	gal	=Equipment!123	Y			
=B48+0.01	Unit 3 Seal Trough	Assumption 3.05	gal	=Equipment!124	v			
=B49+0.01	Unit 3 Overflow Piping	Assumption 3.03	gal	=Equipment!126	v v			
=B50+0.01	Unit 3 Ash Hopper Pit Sump	Attachment 8.09	gal	=Fanisment107	v			
=B51+0.01	AWRP Piping	Attachment 8.07	gal	=SUM(Piping!19:118)-Piping!111	Ŷ			
=B52+0.01	Piping from Bottom Ash Pump to Jet Pump	Assumption 3.04	gal	=SUM(Piping!19:118)-Piping!111 =SUM(Piping!20:121)	Y			
=B53+0.01	Piping from Jet Pumps to South Pond	Attachment 8.08	gal	=SUM(Piping!123:125)	Y			
=B54+0.01	Boiler Room Sump and Bottom Ash Hopper Pit Sump Discharge lines to Crossover	Attachments 8.03 and 8.13	gal	=SUM(Piping!127:129)	Y			
=B55+0.01	Units 1 and 2 Boiler Room Sump Crossover Piping to South Pond	Attachment 8.12	gal	=Piping!I30	Y			
=B56+0.01	Unit 3 Ash Hopper Pit Sump Crossover Piping to South Pond	Attachment 8.12	gal	=Piping!I31	Y			
	TOTAL WETTED VOLUME UNITS 1, 2 & 3		gal	=SUM(F44:F57)	Y			
	Estimated Max Daily Blowdown based on 10% wetted volume over a 30-day rolling average		gpm	=F58°0.1/(60°24)	Y			
=B57+0.01	TOTAL VOLUME UNITS 1.2 & 3		gal	=Equipment!I30+Piping!I32	Y			
=B60+0.01	Units 1 & 2 Boiler Room Sump Surge Volume	Attachment 8.03	gal	=2*Equipment!I14	Ý			
=B61+0.01	Units 3 Ash Hopper Pit Sump Surge Volume	Attachment 8.09	gal	=Equipment!I28	Ý			
=B62+0.01	Units 1 & 2 Ash Hopper Surge Volume	Attachment 8.02	gal	=Equipment!II1*2	Y			
=B63+0.01	Unit 3 Ash Hopper Surge Volume	Attachment 8.05	gal	=Equipment!125	Ŷ			
=B64+0.01	Surge Volume of South Pond	Assumption 3.04	gal	=Equipment!I29	v			
			The state of the s					
7	REFERENCES:							
=B67+0.01	NA NA							
8	ATTACHMENTS:							
8.01	Wetted Ash Volume Calculation Summary							
=B71+0.01	UL & UB Stoom Ash Hopper Volume							
=B72+0.01	U. & U. Beller Kom Sump							
=B73+0.01	UI, UZ & Description Ash Paping Isometries							
=B74+0.01	U. C. C. C. Dominion of ping sometims U. S. C. C. Dominion of ping sometimes U. S. C. C. C. C. Dominion of ping sometimes U. S. C.							
=B75+0.01	OF DOWN TOWN TO A FROM TO A FROM TOWN TO A FROM TOWN TO A FROM TOWN TO A FROM TOWN TOWN TO A FROM TOWN TOWN TO A FROM TOWN TO A FROM TOWN TOWN TOWN TOWN TOWN TOWN TOWN TOWN							
=B76+0.01	OF RC 2 BROBERT STEEL BY SEED AND STEEL ST							
=B77+0.01	ANTA TIME DESCRIPTION OF THE PROPERTY OF THE P							
=B78+0.01	LENCE TORINGS All Roper Pit Sump							
=B79+0.01	Ut and UB bottom Ash Pumps to Jet Pumps							
=B80+0.01	U3 Bottom Ash Pumps to Jef Pumps							
=B81+0.01	UI and U2 Bottom Ash Sump Pump Piping and U3 Ash Hopper Pit Sump Piping from Crossover to South Pond							
=B82+0.01	U3 Ash Hopper Pit Sump Discharge pipe to Crossover							
	and the state of t							

Wetted Volume Calc_Rev0.xlsm 2 of 2

WETTED ASH VOLUME CALCULATION - EQUIPMENT

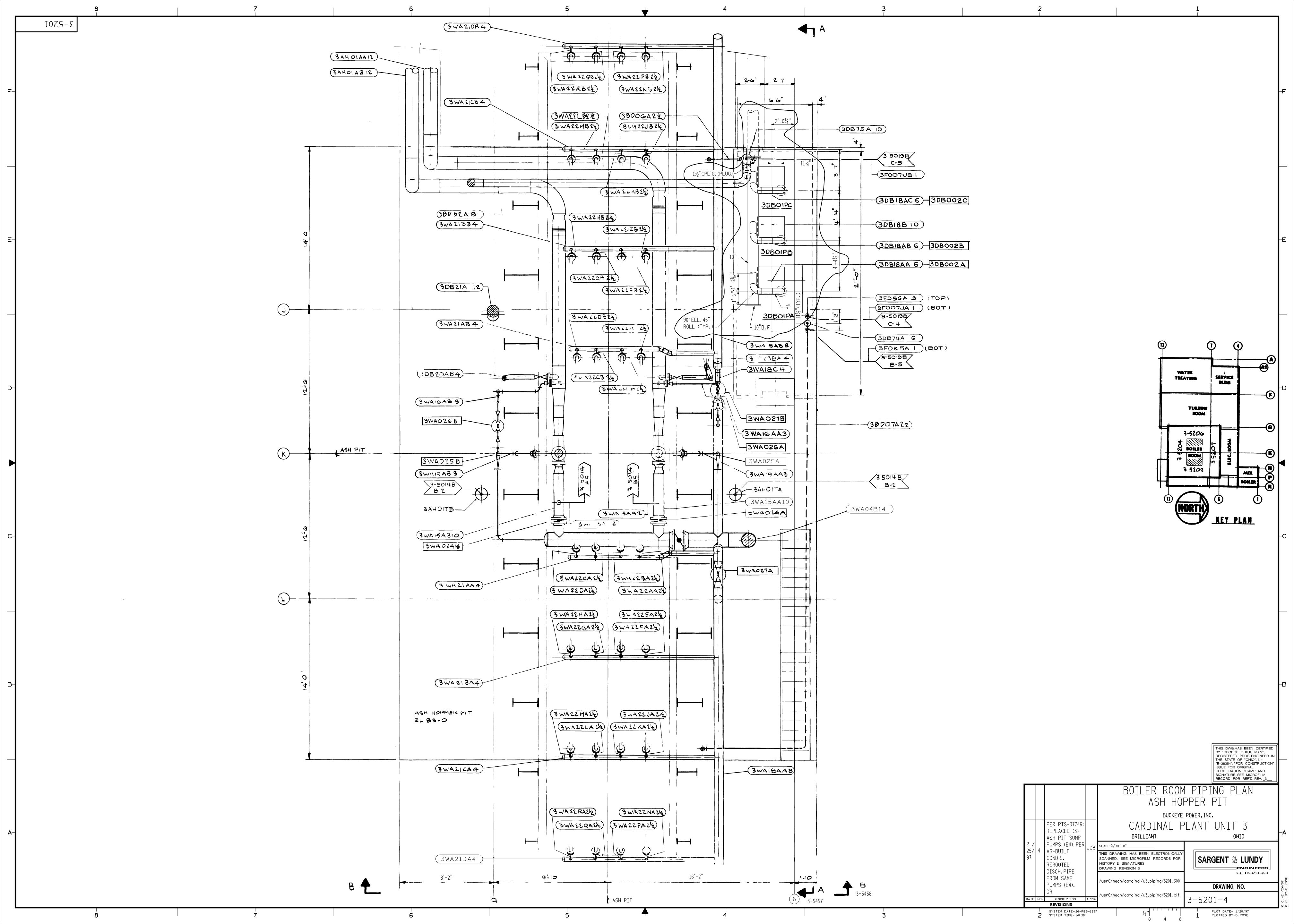
Piping	Pipe schedule	Pipe nor	ninal dia n) Pipe Inne	er dia (in)	Pipe length (ft)	Pipe Cross Sectional area (ft²)	Volume (ft³)	Volume (gal)	Notes
1. Unit 1 Bottom Ash Hopper									
1-01 - Hopper Volume		N/A N/A	N/A N/A	N/A	N/A	N/A		61870	
1-02 - Seal Trough (if applicable)				N/A	N/A		=((64.71+1)*(7.79+1)-(7.79*64.71))*0.5		
1-03 - Surge Capacity (assume water level to be at emergency overflow level for hopper)		N/A	N/A	N/A	N/A			=H11*62.4*0.12	
1-04 - Overflow piping to Boiler Room Sump		STD 12	12	27				=H12*62.4*0.12	
1-05 - Boiler Room Sump		N/A	N/A N/A	N/A	N/A	N/A		=H13*62.4*0.12	First Pump Start level at 666' is used
1-06 - Boiler Room Sump Surge Volume		N/A	N/A	N/A	N/A	N/A	=(667.167-666)*20*8	=H14*62.4*0.12	Extreme High level alarm at 667'-2" is used
2. Unit 2 Bottom Ash Hopper									
2-01 - Hopper Volume		N/A	N/A N/A	N/A	N/A	N/A		61870	
2-02 - Seal Trough (if applicable)		N/A	N/A	N/A	N/A	N/A	=((64.71+1)*(7.79+1)-(7.79*64.71))*0.5	=H17*62.4*0.12	
2-03 - Surge Capacity (assume water level to be at emergency overflow level for hopper)		N/A STD 12	N/A	N/A	N/A			=H18*62.4*0.12	
2-04 - Overflow piping to Boiler Room Sump			12	27		=(PI()*E19^2)/(4*144)		=H19*62.4*0.12	
2-05 - Boiler Room Sump		N/A N/A	N/A N/A	N/A	N/A	N/A	=(666-654)*20*8	=H20*62.4*0.12	First Pump Start level at 666" is used
2-06 - Boiler Room Sump Surge Volume		N/A	N/A	N/A	N/A	N/A	=(667.167-666)*20*8	=H21*62.4*0.12	Extreme High level alarm at 667'-2" is used
3. Unit 3 Bottom Ash Hopper									
3-01 - Hopper Volume		N/A	N/A	N/A	N/A			=H23*62.4*0.12	
3-02 - Seal Trough (if applicable)		N/A	N/A	N/A	N/A		=((61.75+1)*(10.5+1)-(10.5*61.75))*0.5	=H24*62.4*0.12	
3-03 - Surge Capacity (assume water level to be at emergency overflow level for hopper)		N/A STD 12	N/A	N/A	N/A			=H25*62.4*0.12	
3-04 - Overflow piping to Ash Hopper Pit Sump		STD 12	12	27		=(PI()*E26^2)/(4*144)	=F26*G26	=H26*62.4*0.12	
3-05 - Ash Hopper Pit Sump		N/A N/A	N/A N/A	N/A	N/A		=(80-77)*15.33*6.5	=H27*62.4*0.12	First Pump Start level at 80' is used
3-06 - Ash Hopper Pit Sump Surge Volume		N/A	N/A	N/A	N/A	N/A	=(82-80)*15.33*6.5	=H28*62.4*0.12	Third Pump Start level at 82' is used
4. Surge Volume of South Pond		N/A	N/A	N/A	N/A	N/A	=33.9*43559.9	=H29*62.4*0.12	
5. Total Volume of Equipment								=SUM(19:128)	The sum of all volumes above except the Surge Volume of the South P

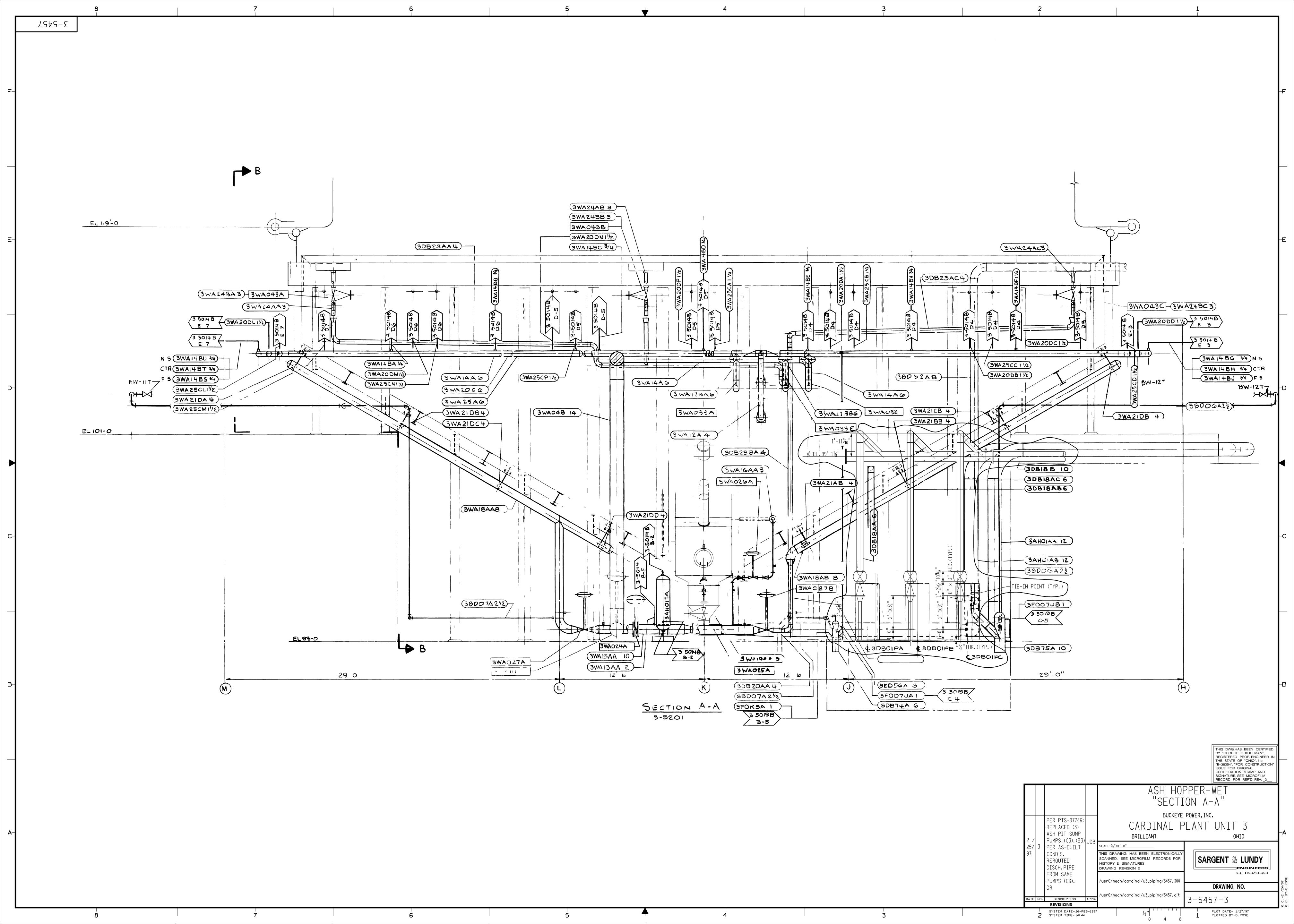
WETTED ASH VOLUME CALCULATION - PIPING

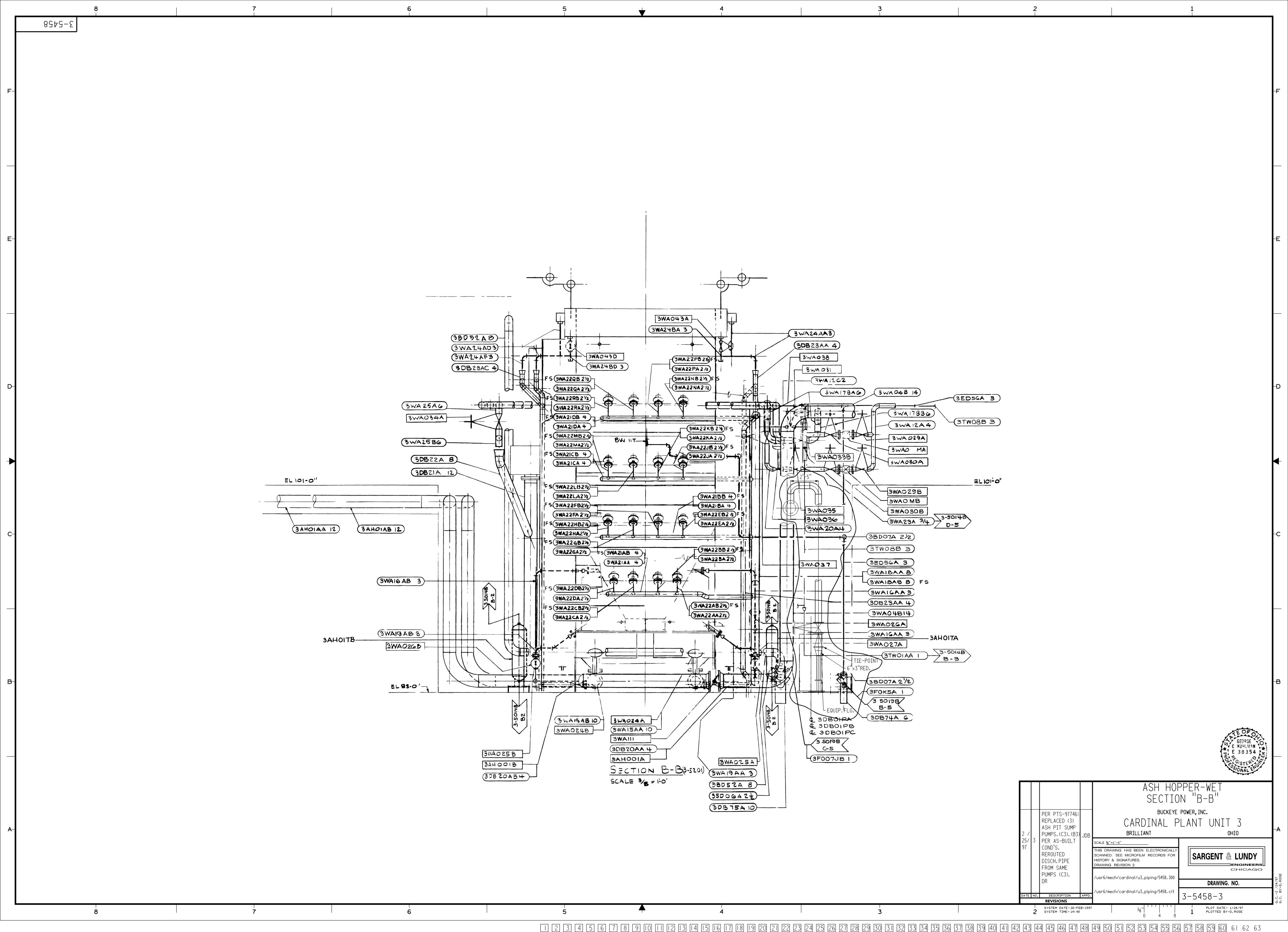
Piping	Pipe schedule Pipe nominal o	Pipe Inner dia (in)	Pipe length (ft)	Pipe Cross Sectional area (ft²)	Volume (ft³)	Volume (gal)	Notes
1. Piping from Ash Water Recirculation Pump (AWRP) Loop to Units 1, 2, and 3							
1-01a - AWRP Discharge Common Header up to Unit 3	STD 30	29.25	98	=(PI()*E9^2)/(4*144)	=F9*G9	=H9*62.4*0.12	
1-01b - AWRP Discharge Common Header up to Unit 3	STD (20) 24	23.25	2522	=(PI()*E10^2)/(4*144)	=F10*G10	=H10*62.4*0.12	
1-01c - Redundant AWRP Discharge Pipe	STD (20)	23.25	2522	=(PI()*E11^2)/(4*144)	=F11*G11	=H11*62.4*0.12	Redundant AWRP pipe for the discharge common header up to Unit 3
1-02a - AWRP Discharge Dedicated line to Unit 3 Bottom Ash Pump	STD 18	17.25	672	=(PI()*E12^2)/(4*144)	=F12*G12	=H12*62.4*0.12	
1-02b - AWRP Discharge Dedicated line to Unit 3 Bottom Ash Pump	STD (30)	13.25	50	=(PI()*E13^2)/(4*144)	=F13*G13	=H13*62.4*0.12	Assumed 14" nominal piping extend 50 ft to Bottom Ash Pump
1-03 - AWRP Discharge Common Header up to Unit 2	STD (20) 24	23.25 15.25	4740 456	=(PI()*E14^2)/(4*144)	=F14*G14 =F15*G15	=H14*62.4*0.12 =H15*62.4*0.12	
1-04a - AWRP Discharge Dedicated line to Unit 2 Bottom Ash Pump	STD (30) 16	15.25	456	=(PI()*E15^2)/(4*144)	=F15*G15	=H15*62.4*0.12	
1-04b - AWRP Discharge Dedicated line to Unit 2 Bottom Ash Pump	STD 12	12	50	=(PI()*E16^2)/(4*144)	=F16*G16	=H16*62.4*0.12	Assumed 12" nominal piping extend 50 ft to Bottom Ash Pump
1-05a - AWRP Discharge Dedicated line to Unit 1 Bottom Ash Pump	STD (30) 16	15.25	826	=(PI()*E17^2)/(4*144)	=F17*G17	=H17*62.4*0.12	
1-05b - AWRP Discharge Dedicated line to Unit 1 Bottom Ash Pump	STD 12	12	50	=(PI()*E18^2)/(4*144)	=F18*G18	=H18*62.4*0.12	Assumed 12" nominal piping extend 50 ft to Bottom Ash Pump
2. Piping from Bottom Ash Pump to Jet Pump							
2-01 - Unit 1 and Unit 2 Common Bottom Ash Pump to Jet Pump	STD 12	12	=204.4167+2*48.4167+249	3=(PI()*E20^2)/(4*144)	=F20*G20	=H20*62.4*0.12	Conservatively used just the lengths of pipe from Att. 8.10 and assumed all pi
2-02 - Unit 3 Bottom Ash Pump to Jet Pump	STD 12	12	200.9	=(PI()*E21^2)/(4*144)	=F21*G21	=H21*62.4*0.12	Conservatively used just the lengths of pipe from Att. 8.11 and assumed all pi
3. Piping from Jet Pump to South Pond	·		,				
3-01 - Unit 1 Jet Pump to South Pond	HDPE / Basalt Lined	11.8	=1.6*5280	=(PI()*E23^2)/(4*144)	=F23*G23	=H23*62.4*0.12	ID from CBP doc, A portion of the pipe is 14" (SDR 13.5) HDPE (ID 11.8") and a lined CS (ID 11.93") so 11.8" is used for conservatism
3-02 - Unit 2 Jet Pump to South Pond	HDPE / Basalt Lined	11.8	=1.58*5280	=(PI()*E24^2)/(4*144)	=F24*G24	=H24*62.4*0.12	ID from CBP doc, A portion of the pipe is 14" (SDR 13.5) HDPE (ID 11.8") and a lined CS (ID 11.93") so 11.8" is used for conservatism
3-03 - Unit 3 let Pump to South Pond	HDPE / Basalt Lined	11.8	4239.73	=(PI()*E25^2)/(4*144)	=F25*G25	=H25*62.4*0.12	ID from CBP doc, A portion of the pipe is 14" (SDR 13.5) HDPE (ID 11.8") and a lined CS (ID 11.93") so 11.8" is used for conservatism
4. Boiler Room Sump Discharge to the Crossover							
4-01 - Unit 1 Boiler Room Sump Discharge to Crossover	CS Polyurethane-lined pipe (assumed STD)	12	=108+350+278.5+19	={PI()*E27^2)/(4*144)	=F27*G27	=H27*62.4*0.12	Assumed the same ID as Carbon Steel STD pipe
4-02 - Unit 2 Boiler Room Sump Discharge to Crossover	CS Polyurethane-lined pipe (assumed STD)	12	=350+111+19	=(PI()*E28^2)/(4*144)	=F28*G28	=H28*62.4*0.12	Assumed the same ID as Carbon Steel STD pipe
4-03 - Unit 3 Ash Hopper Pit Sump Discharge to Crossover	Sch. 40 10	10.02	52.5	=(PI()*E29^2)/(4*144)	=F29*G29	=H29*62.4*0.12	
4-04 - Units 1 and 2 Boiler Room Sump Crossover Piping to South Pond	HDPE / Basalt Lined	11.8	=4995+389+2746	=(PI()*E30^2)/(4*144)	=2*F30*G30	=H30*62.4*0.12	ID from CBP doc, A portion of the pipe is 14" (SDR 13.5) HDPE (ID 11.8") and a lined CS (ID 11.93") so 11.8" is used for conservatism
4-05 - Unit 3 Ash Hopper Pit Sump Crossover Piping to South Pond	HDPE / Basalt Lined	11.8	=794+2746	=(PI()*E31^2)/(4*144)	=F31*G31	=H31*62.4*0.12	ID from CBP doc, A portion of the pipe is 14" (SDR 13.5) HDPE (ID 11.8") and a lined CS (ID 11.93") so 11.8" is used for conservatism
5. Total Volume of Piping						=SUM(I9:I31)	The sum of all volumes above

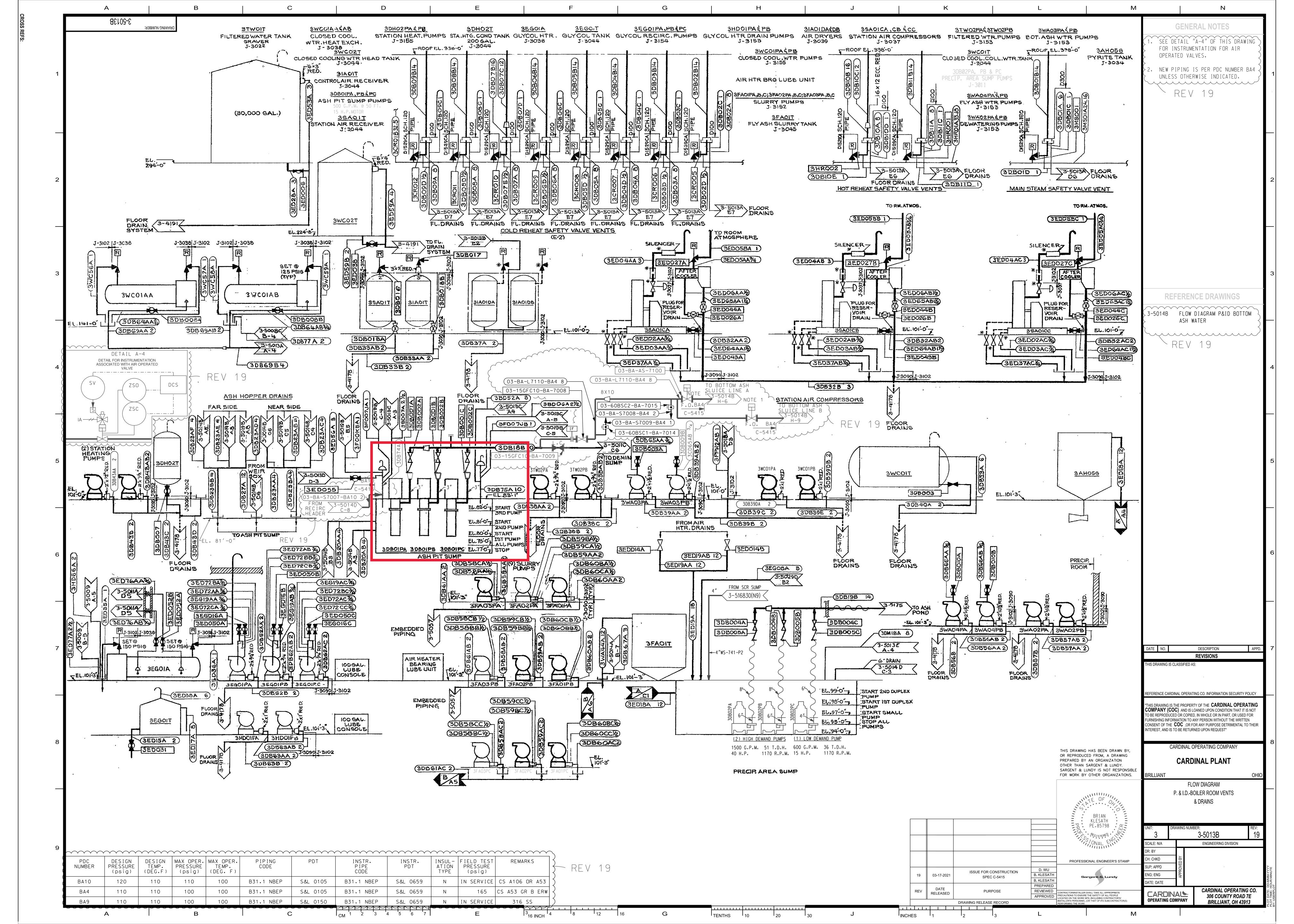


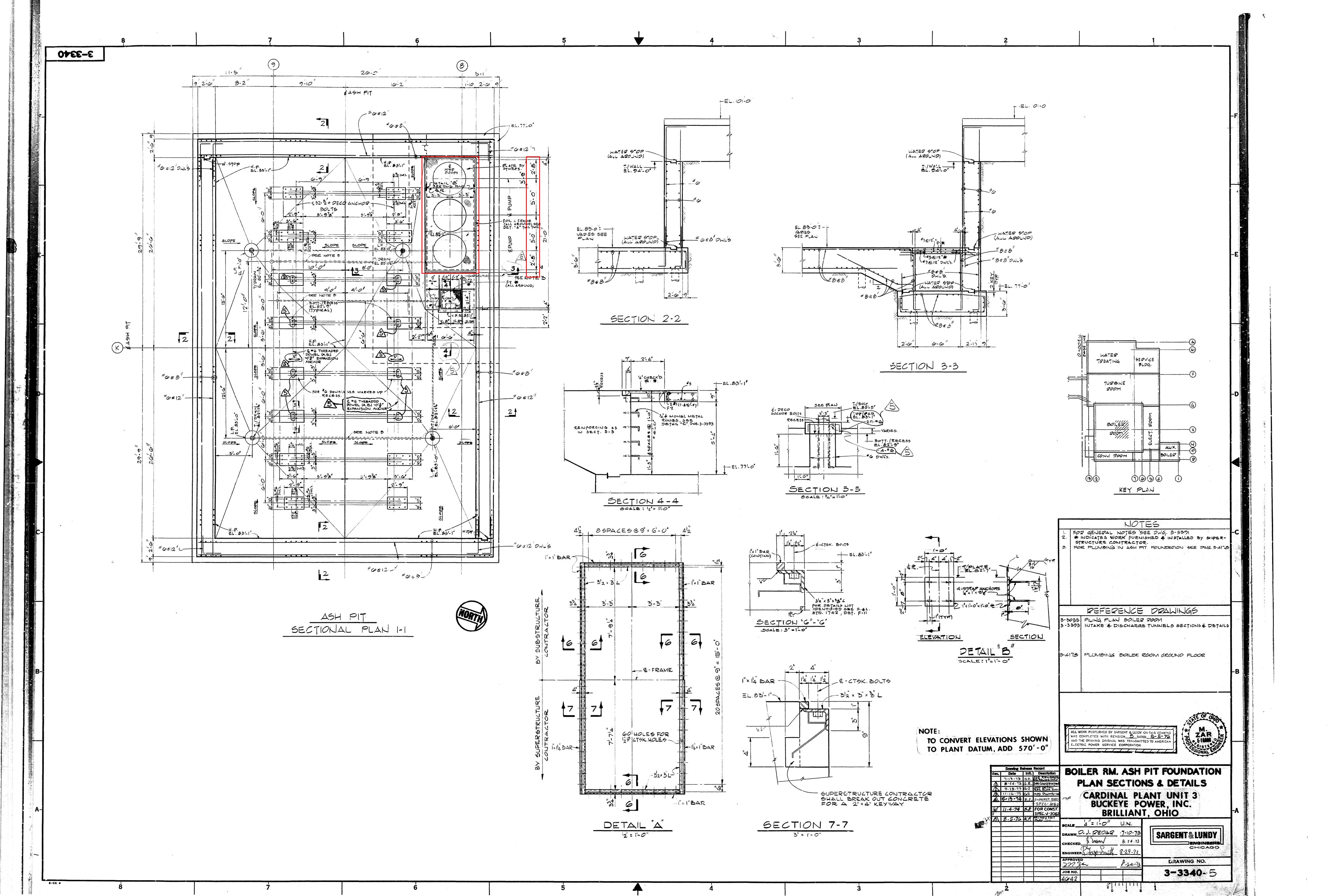
8.09 U3 Ash Hopper Pit Sump





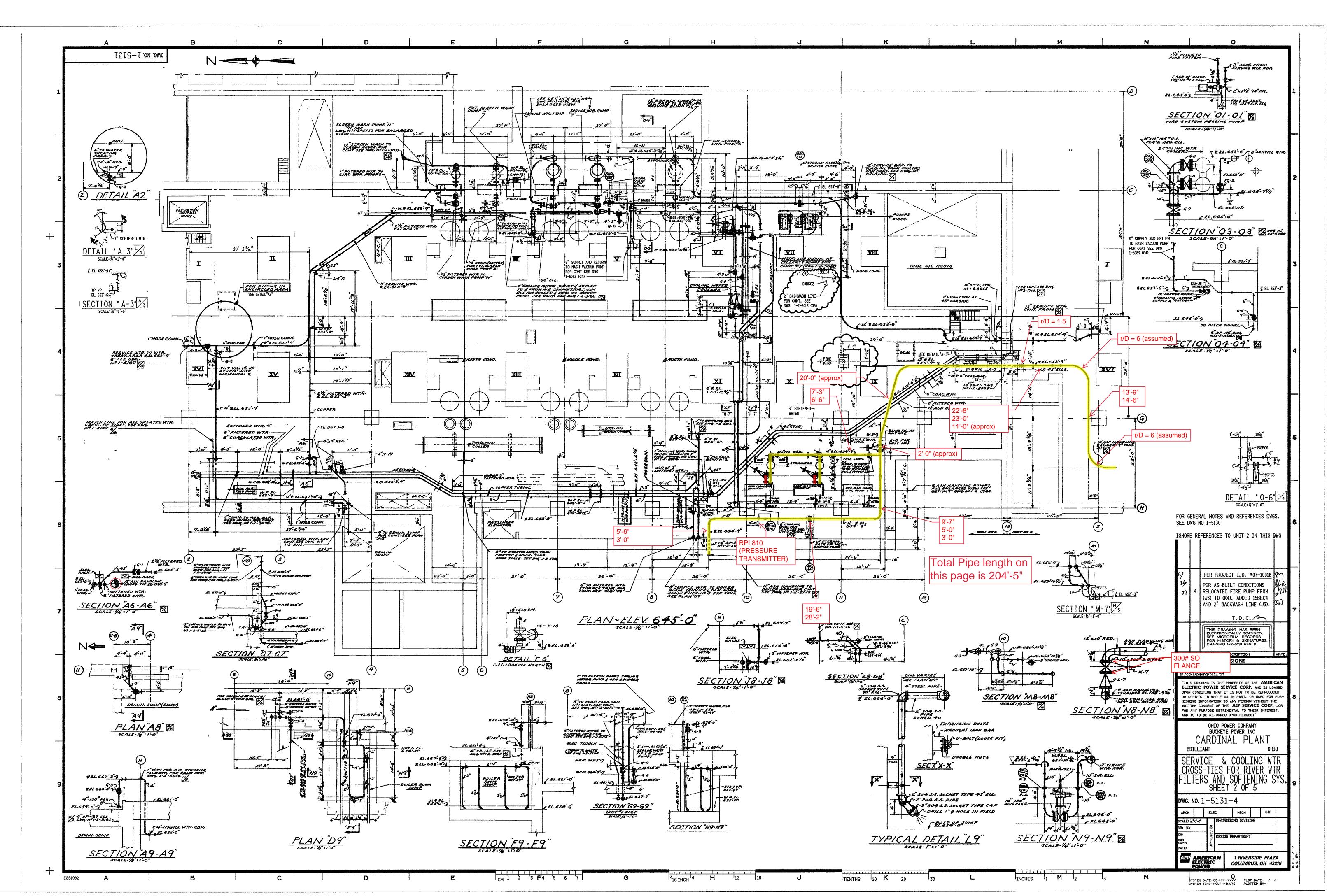


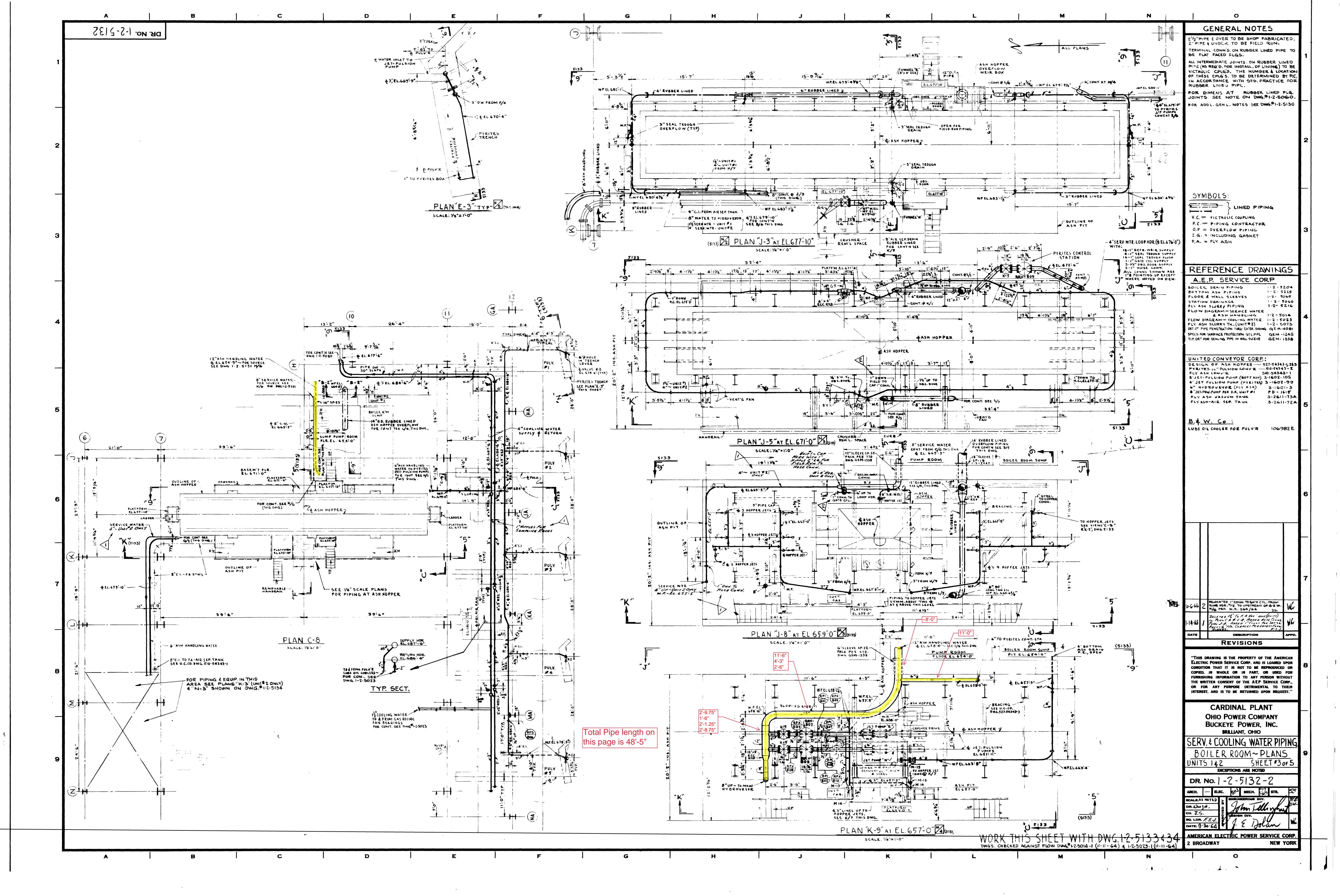


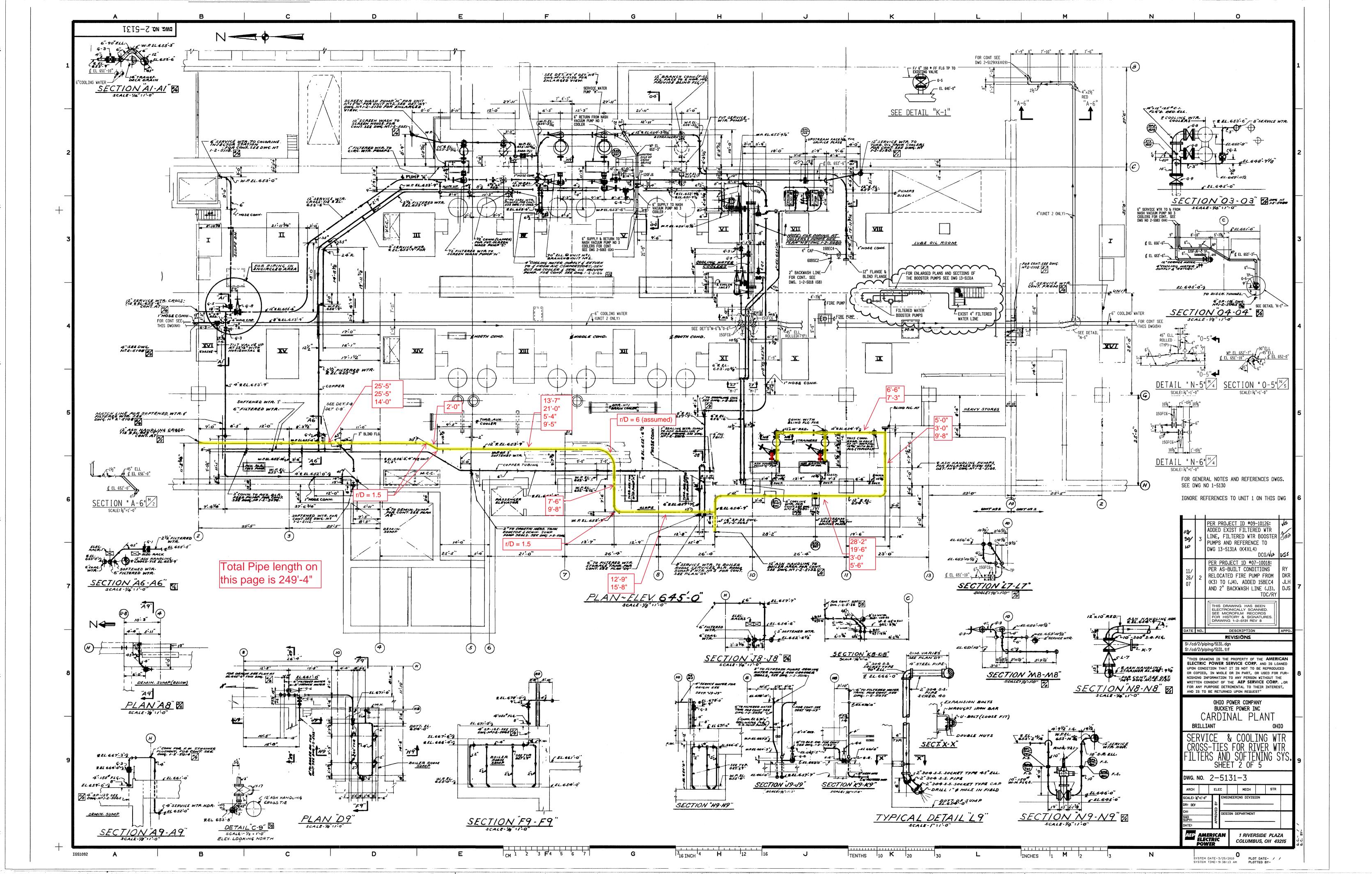




8.10 U1 and U2 Bottom Ash Pumps to Jet Pumps

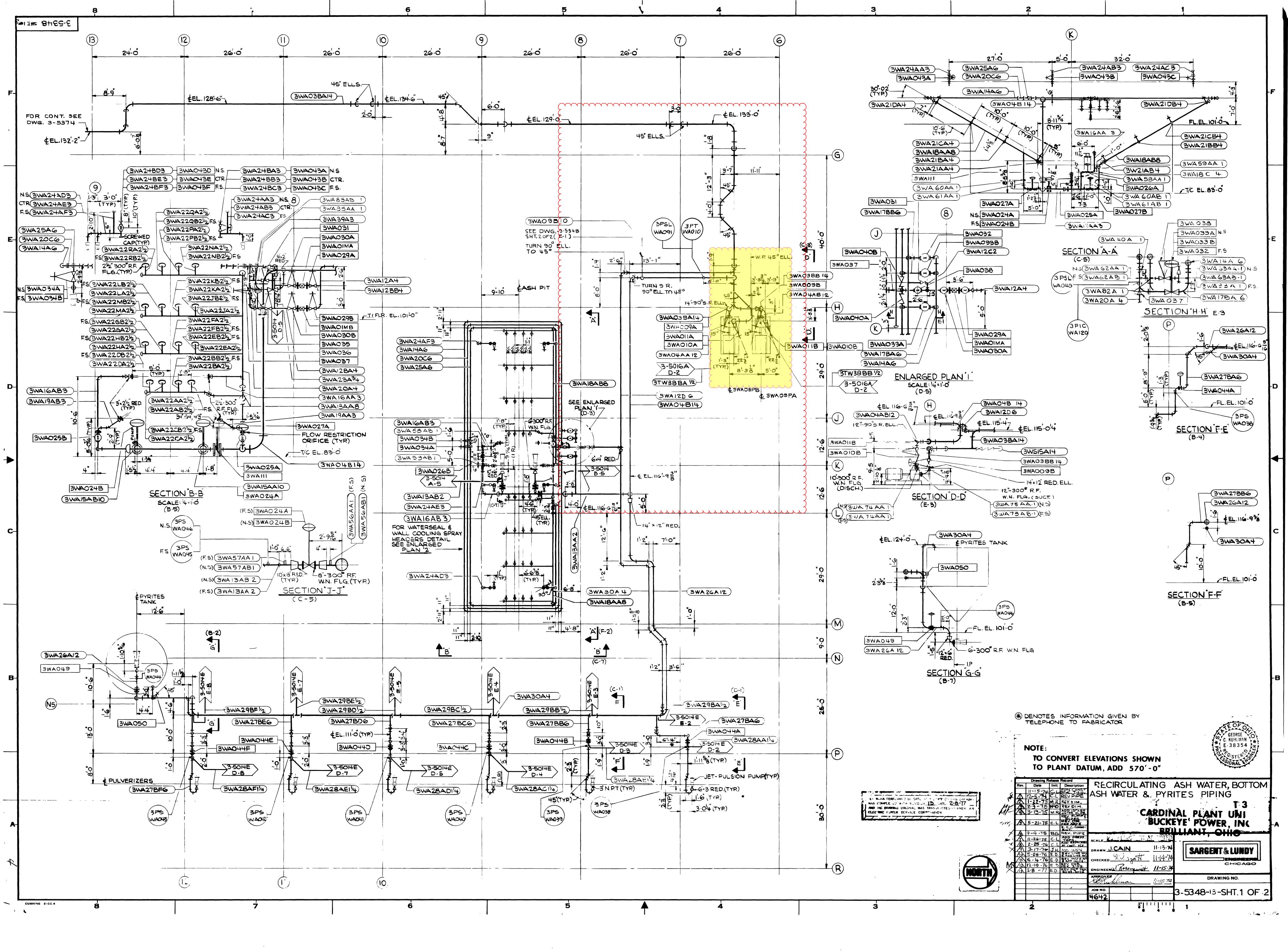


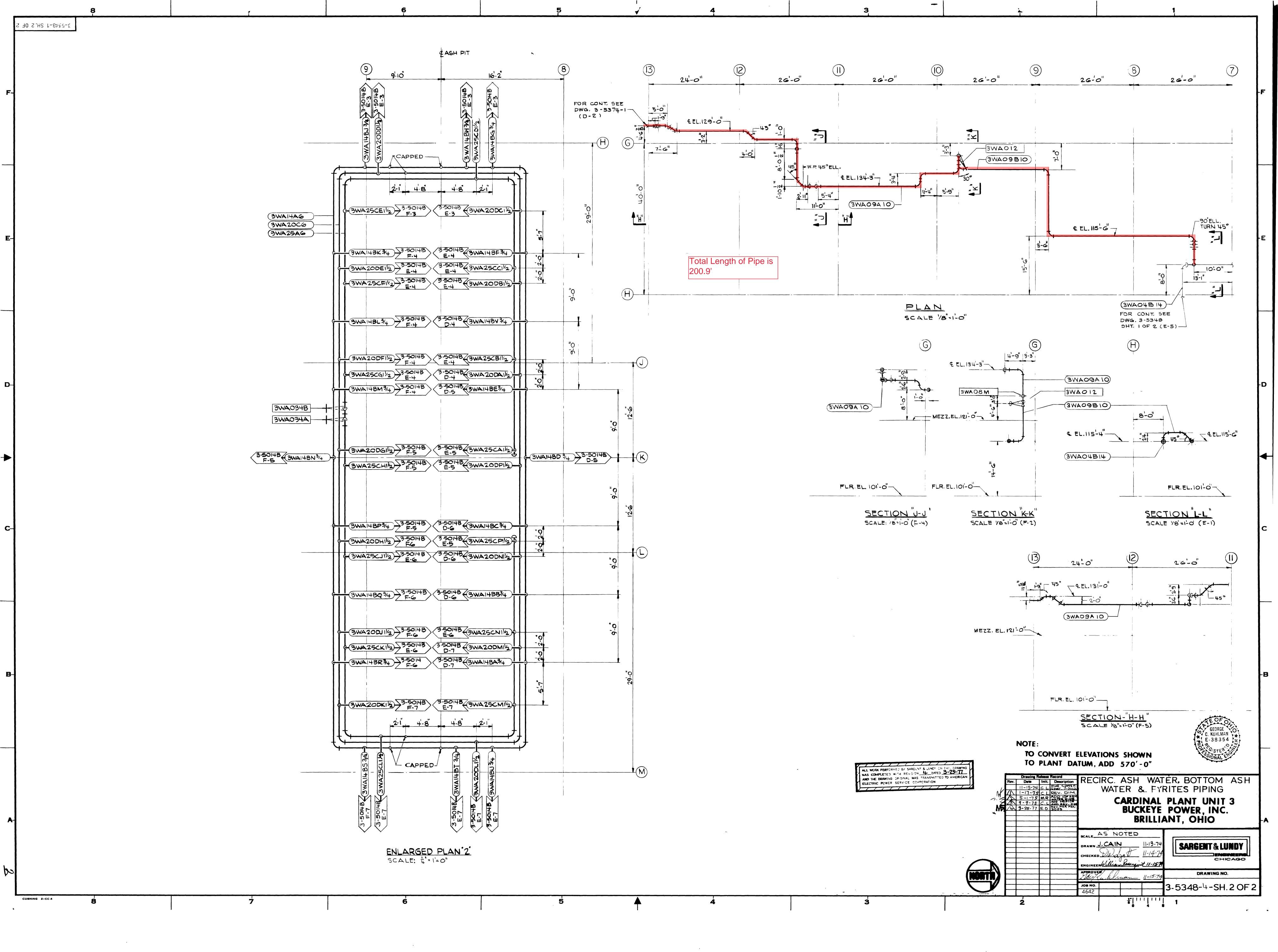






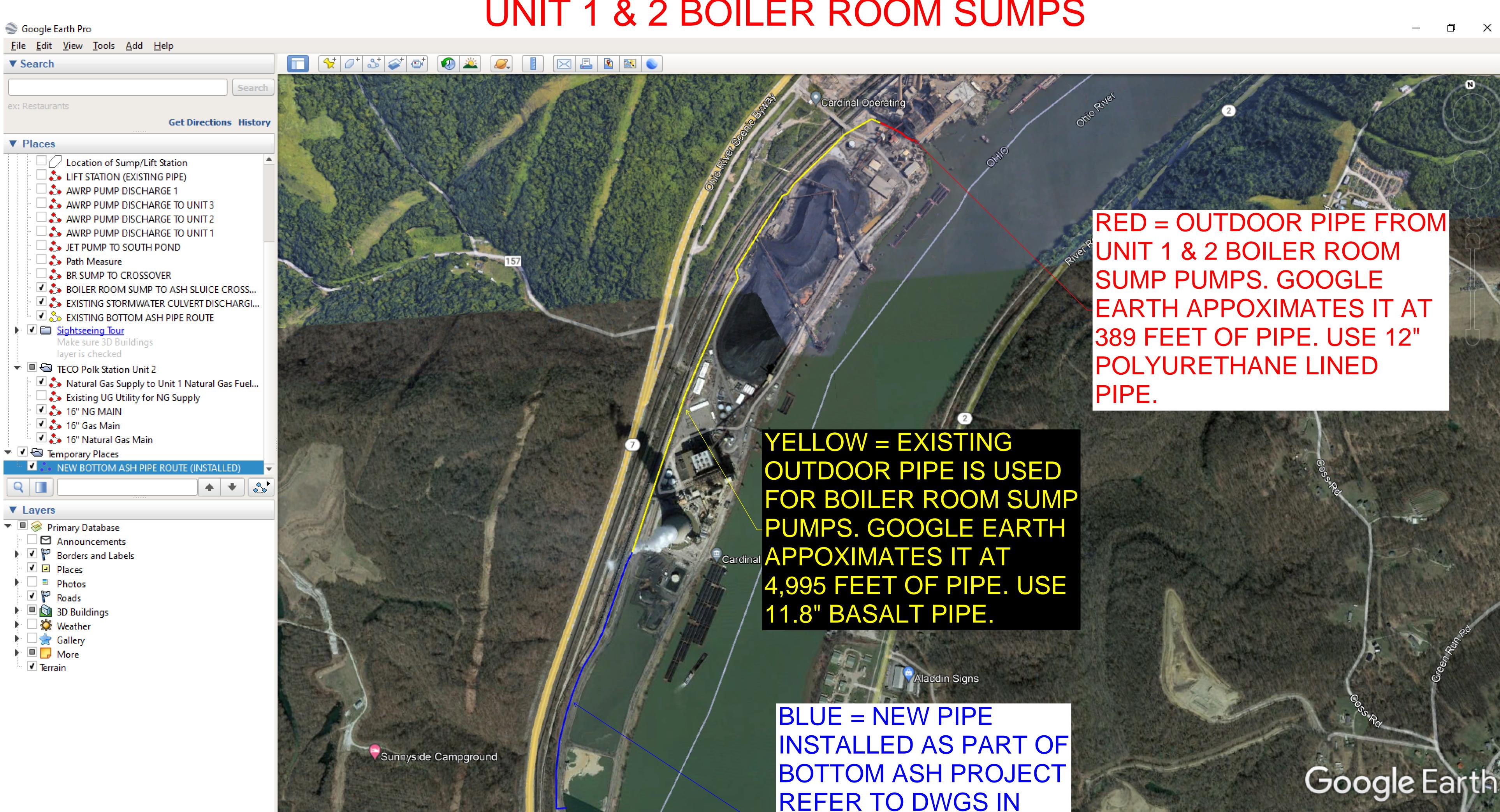
8.11 U3 Bottom Ash Pumps to Jet Pumps







8.12 U1 and U2 Bottom Ash Sump Pump Piping and U3 Ash Hopper Pit Sump Piping



EMAIL. GOOGLE EARTH

APPROXIMATES IT AT

2,746 FEET OF PIPE.

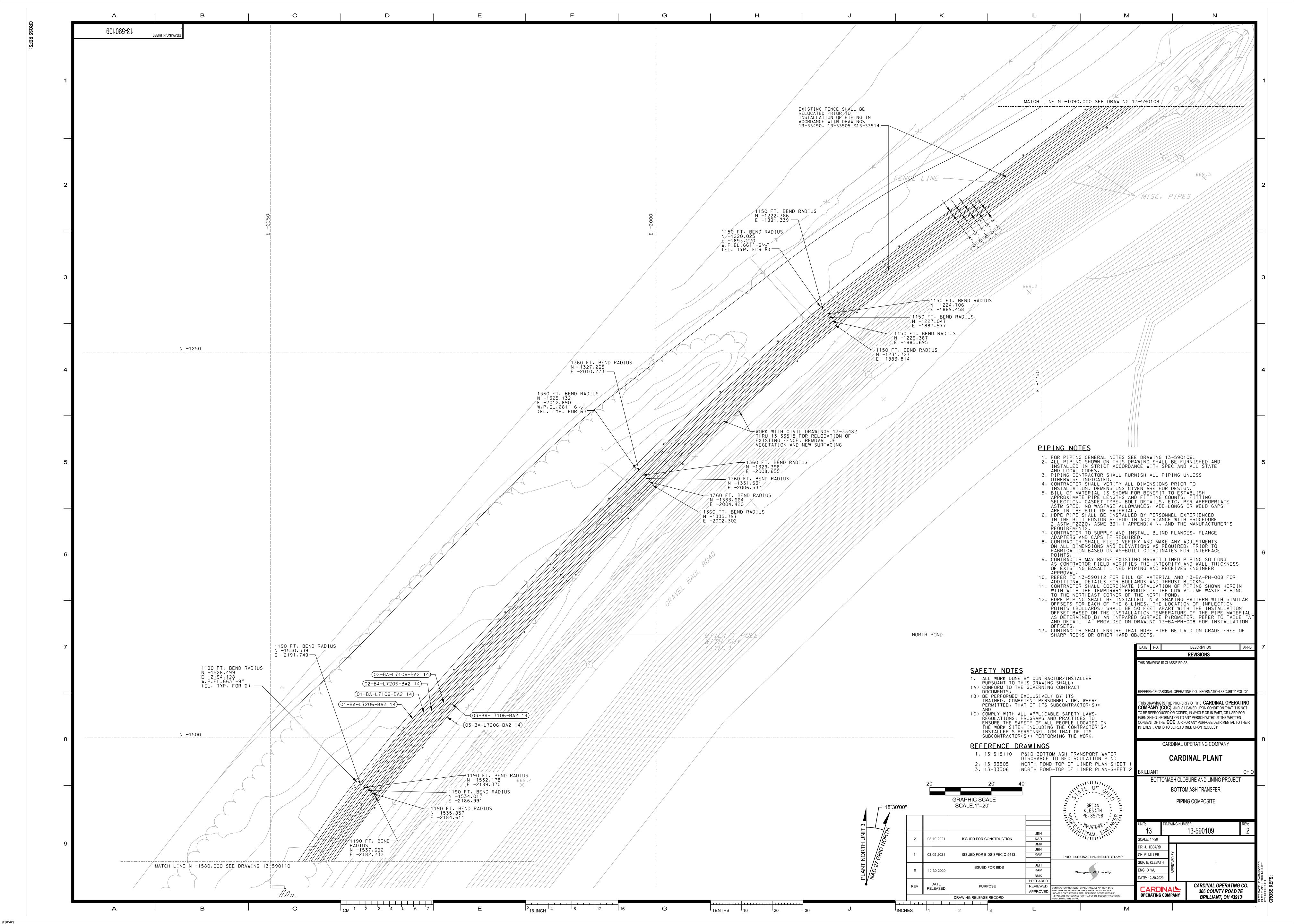
USE HDPE PIPE PER

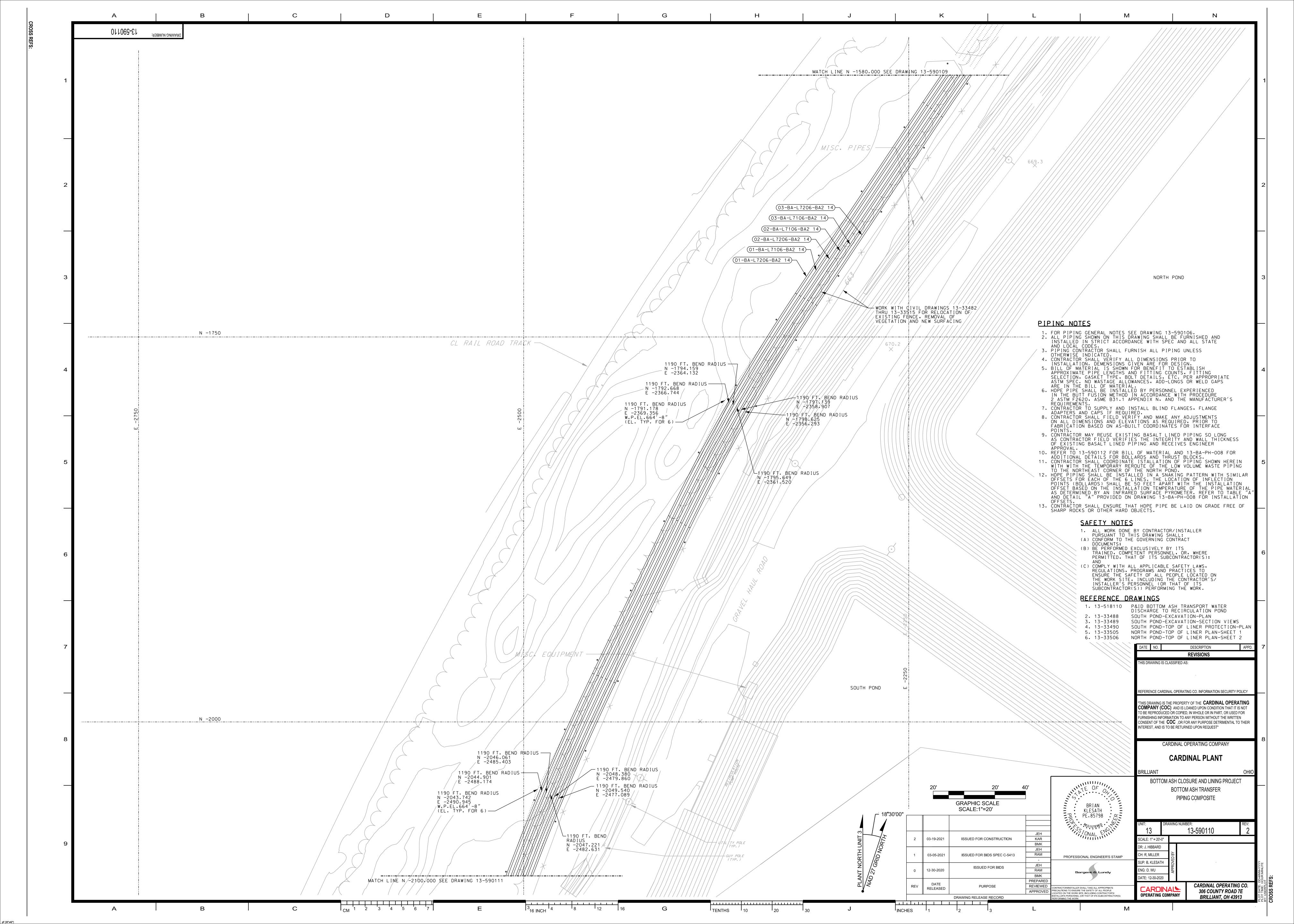
DRAWING.

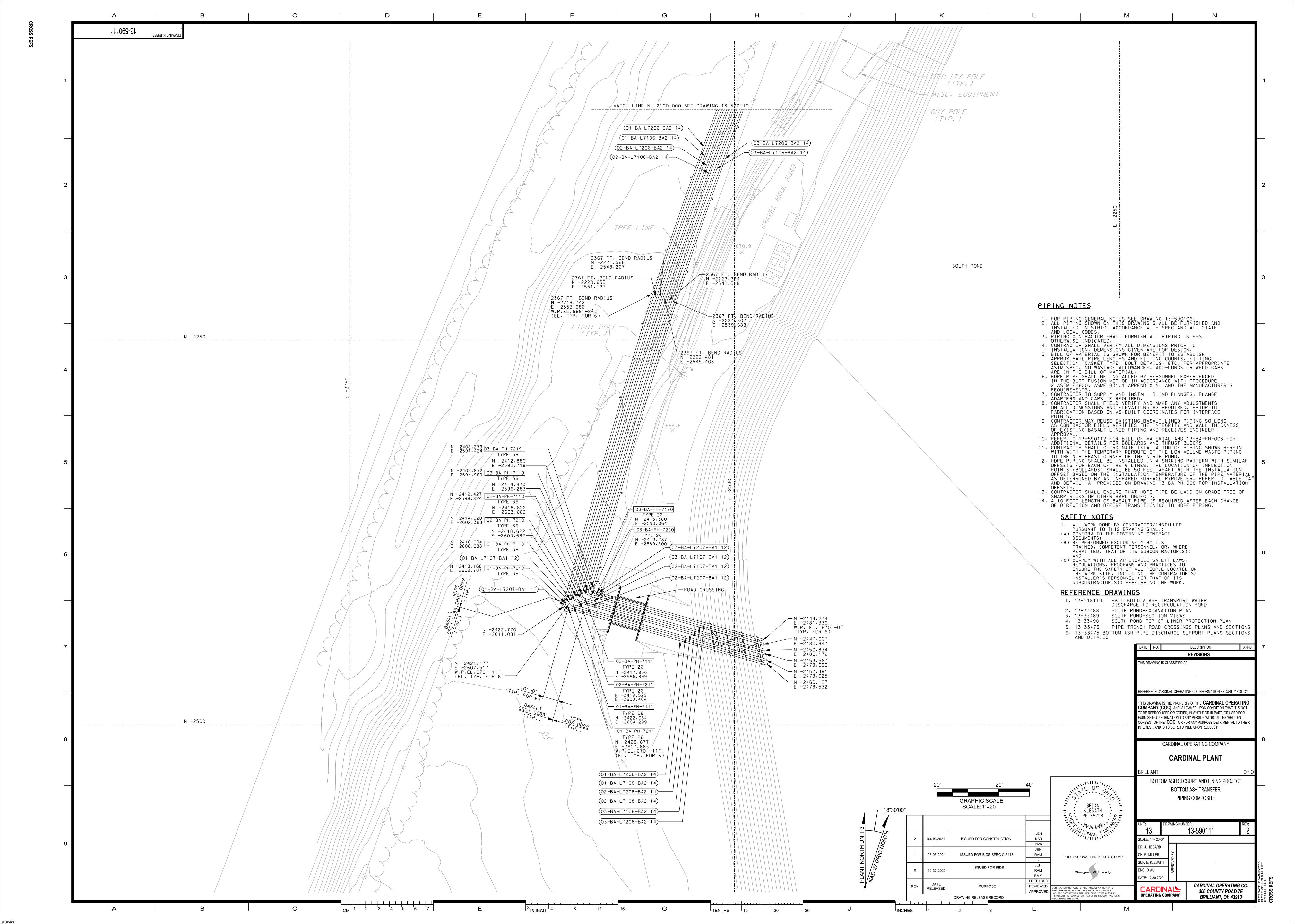
40°14'54.67" N 80°39'09.16" W elev 743 ft eye alt 10710 ft 🔘

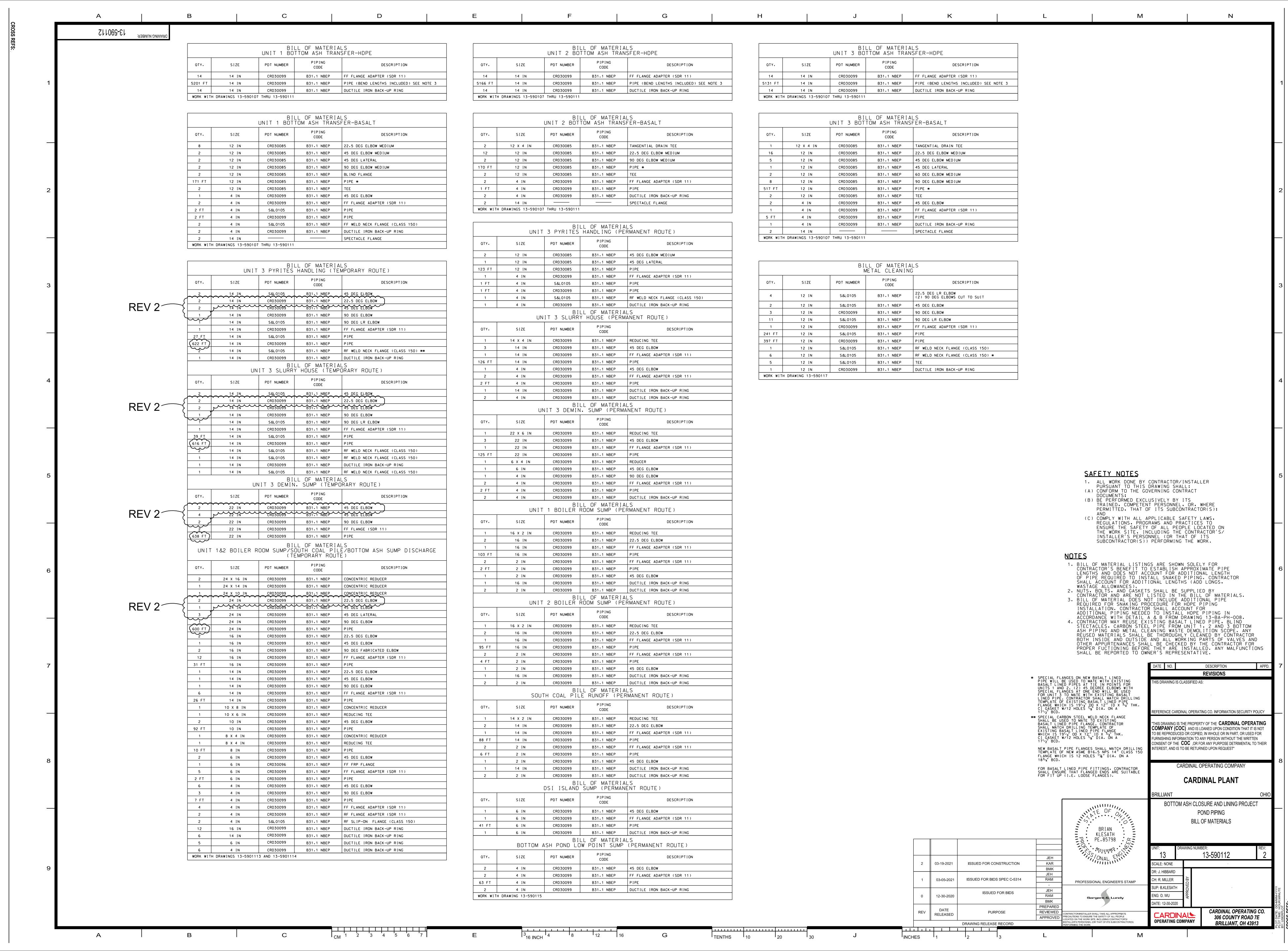
UNIT 3 BOTTOM ASH HOPPER PIT SUMP





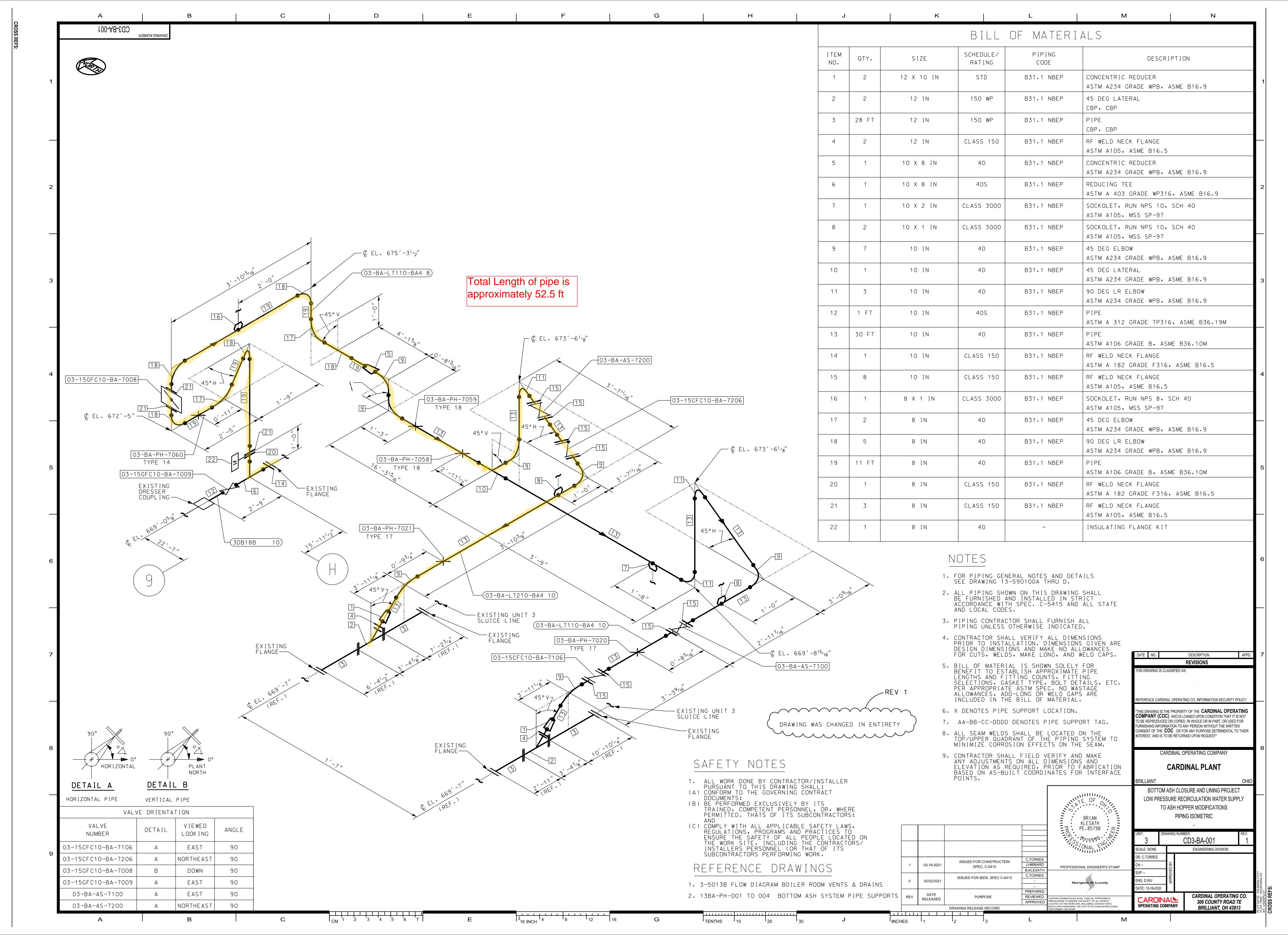








8.13 U3 Ash Hopper Pit Sump Discharge pipe to Crossover







CARDINAL GENERATING STATION

BOTTOM ASH TRANSPORT SYSTEM EVALUATION

Issue: Rev. 0, For Use Date: October 9, 2023 Project No. A13770-006

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APPENDIX B.

BOTTOM ASH SYSTEM RAINFALL ESTIMATE



ISSUE SUMMARY Form SOP-0402-07, Revision 13

	DESIGN CONTROL SUMMARY	
CLIENT:	Cardinal Operating Company UNIT NO	.: <u>1,2 & 3</u> PAGE NO.: <u>1</u>
PROJECT NAME:	Cardinal Plant	
PROJECT NO.:	A13770-006	S&L NUCLEAR QA PROGRAM
CALC. NO:	2023-02951	APPLICABLE ☐ YES ⊠ NO
TITLE:	South Bottom Ash Pond Stormwater Runoff Analysis	
EQUIPMENT NO.:	N/A	
	IDENTIFICATION OF PAGES ARRESTING FROM PERSON PAGES ARRESTING FROM PAGES ARRESTING FROM PAGES ARRESTING FROM PAGES ARRESTING	DEVIEWARTHOR
	IDENTIFICATION OF PAGES ADDED/REVISED/SUPERSEDED/VOIDED &	REVIEW METHOD
Main Calculation: 7 Attachments (6): 6		INPUTS/ ASSUMPTIONS
Total: 13 Pages		
REVIEW METHOD	. Datailed	UNVERIFIED REV: 0
	☐ SUPERSEDED BY CALCULATION, NO	
STATUS:	APPROVED SOLENGEDED BY OALCOCATION NO.	OID DATE FOR REV.: 8/18/2023
ISSUE DESCRIPTION:	For use	
PREPARER:	Nikhil Patel Nikhil Patel Digitally signed by Nikhil Patel	DATE: 8/18/2023
REVIEWER:	Vasudev Patel Vasudev Patel Digitally signed by Vasudev Patel Date: 2023.08.18 154554-45507	DATE: 8/18/2023
APPROVER:	Darrel Packard Darrel Packard 2023.08.18 16:17:28 -05'00'	DATE: 8/18/2023
	IDENTIFICATION OF PAGES ADDED/REVISED/SUPERSEDED/VOIDED &	REVIEW METHOD
		INPUTS/ ASSUMPTIONS
		☐ VERIFIED☐ UNVERIFIED
REVIEW METHOD	•	REV.:
STATUS:	APPROVED SUPERSEDED BY CALCULATION NO.	
ISSUE	-	
PREPARER:		DATE:
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ATTACHMENTS

- 1. NOAA Atlas 14 Rainfall from Reference 2.
- 2. Cardinal Plant Drawings and Input
- 3. Rainfall Volumes for 10-Year Storm for Different Durations
- 4. Rainfall Volumes for 50-Year Storm for Different Durations
- 5. Rainfall Volume for 10-Year Graph
- 6. Rainfall Volume for 50-Year Graph



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1.0 PURPOSE AND SCOPE

The EPA published a new revision of the 40 CFR 423 Effluent Limitations Guidelines (ELG) on December 31, 2020. This updated revision changed the total volume of bottom ash transport water that is allowed to be discharged from a steam electric generating plant from 0 percent to allowing up to 10 percent of the primary active wetted bottom ash system volume per day considering a 30-day rolling average per 40 CFR 423 (k)(2)(i)(A).

The purpose of this calculation is to determine stormwater rainfall contribution inflow into the South Bottom Ash Pond (BAP) through direct rainfall or onto surfaces that drain into the bottom ash transport water system for Units 1, 2, and 3 at Cardinal at Brilliant, Ohio. This information will be used to assess in part, in a separate calculation, the potential stormwater rainfall contribution to the BAP and how much BAP can be discharged, due to this type of event(s) while satisfying 40 CFR 423.

2.0 DESIGN INPUT

2.1 Rainfall Data

In 40 CFR 423.13(k)(2)(i)(A), the rule states that to discharge south BAP the Plant must "maintain system water balance when precipitation-related inflows are generated from storm events exceeding a 10-year storm event of 24-hour or longer duration (e.g., 30-day storm event) and cannot be managed by installed spares, redundancies, maintenance tanks, and other secondary bottom ash system equipment. Therefore, the quote above, the 10-year, 24-hour storm is to be evaluated, however the longer duration implies that an upper boundary should be considered when evaluating the bottom ash transport water volume. To develop an upper boundary for this calculation, in the 40 CFR 423 Preamble it states that if there is a rare precipitation event like the 100-year storm, the NPDES is more flexible to allow a bypass higher than 10% - based on this input it is reasonable to establish the upper boundary as a 50-year event, and as a result this calculation evaluates the stormwater runoff volume for rainfall events between 10-year and 50years, and for durations of each event from 6 hours to 30 days were analyzed and included in Attachments 3 and 4 to identify sensitivity with respect to duration and storm frequency. The rainfall depths used are the high, average, and low depths as published by NOAA in Attachment 1. The high and low depth are estimates as the upper and lower bounds, respectively, of the 90% confidence interval. The probability that the rainfall depths will be greater than the upper bound or less than the lower bound is 5 percent, as stated by NOAA in Note 1 on Attachment 1.



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This calculation presents in Section 6 the detailed steps to determine the runoff volume for the 10-year, 24-hour depth to outline the process used to calculate the runoff volume for each storm event and duration. For the Cardinal Plant, the 10-year, 24-hour rainfall depth value is 3.38 inches per NOAA Atlas 14 (Reference 1). Rainfall depths from NOAA Atlas 14 are included as Attachment 1 from Reference 1.

2.2 Drainage Areas

There are two separate drainage areas that comprises the BAP (Reference 2). Topographic surveying for the site was provided by Labella in August 2020. As per the as-built documents, the top of dike for BAP is set at 670.0 ft and the normal water elevation is at 665.0 ft. The south pond area is approximately 6.9 acres, and the pond bottom elevation is at 652.0 feet. Water is pumped out of the South Pond through the recirculation Pumphouse. As indicated in Reference 2, the drainage areas accounted for the calculation is the perimeter dike road around the site. This area equated to 2.1 ac.

2.3 All elevations in this analysis reference to National Geodetic Vertical Datum of 1929 (NGVD 29) (Reference 3)

3.0 ASSUMPTIONS

Following conservative assumptions are made in the analysis:

3.1 A runoff coefficient of 1.0 was utilized to calculate the runoff volumes for both areas (direct rainfall, and the perimeter dike) into the Bottom Ash Pond (BAP) System. This runoff coefficient assumes that there are no losses or infiltration of collected rainfall.

4.0 METHODOLOGY

Utilizing the existing Plant drawings and information used in Reference 2, the two contributing drainage areas were determined. Area 1 is considered the Bottom Ash Pond, Area 2 the perimeter dike road around the site.

Once the contributing equipment of the Plant's bottom ash system is understood, the area is calculated as shown in Section 2.2. At this point the runoff volume could be calculated using the 10-year, 24-hour rainfall depth, as shown in Attachment 1, and the selected runoff coefficient.

5.0 ACCEPTANCE CRITERIA

There are no acceptance criteria for this calculation.



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6.0 CALCULATIONS

The equation utilized to calculate the runoff volume from each area is shown below. Design inputs for this section are from Section 2.

Runoff Volume V = C*d*A

Where:

V= Runoff Volume (ac-ft)

C= Runoff Coefficient (as listed in Assumption 3.1)

d= Storm depth as shown on Attachment 1

A= Drainage Area (ac)

6.1 <u>Area 1 Runoff Volume</u>

Area 1 consists of south Bottom Ash Pond (BAP) with drainage area of 6.9 acres

A = 6.9 acres

10-Year, 24-hour rainfall from Attachment 1, average d = 3.38 inches

Note: lower bound is 3.14 inches and upper bound is 3.64 inches

Runoff coefficient C = 1.0

Average rainfall Runoff volume $V = 1.0 \times 3.38/12 \times 6.9 = 1.944$ ac-ft

Lower bound rainfall Runoff volume $V = 1.0 \times 3.14/12 \times 6.9 = 1.806$ ac-ft

Upper bound rainfall Runoff volume $V = 1.0 \times 3.64/12 \times 6.9 = 2.093$ ac-ft

Runoff volume for different durations is presented in Attachment 3.

6.2 Area 2 Runoff Volume

Area 2 consists of perimeter dike road with drainage area of 2.1 acres

A = 2.1 acres

10-Year, 24-hour rainfall from Attachment 1, average d = 3.38 inches

Note: lower bound is 3.14 inches and upper bound is 3.64 inches

Runoff coefficient c =1.0

Average rainfall Runoff volume $V = 1.0 \times 3.38/12 \times 2.1 = 0.592$ ac-ft

Lower bound rainfall Runoff volume $V = 1.0 \times 3.14/12 \times 2.1 = 0.550$ ac-ft

Upper bound rainfall Runoff volume V = $1.0 \times 3.64/12 \times 2.1 = 0.637$ ac-ft

Runoff volume for different durations for 50-year storm event is presented in Attachment 4.



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7.0 RESULTS

Combined Runoff Volume for South BAP is summarized below:

Storm D	Ouration	Volume (ac-ft)									
Duration Hr / Day	Days		10-Year		50-Year						
		Average	Upper Bound	Lower Bound	Average	Upper Bound	Lower Bound				
6-hour	0.25	1.890	2.146	1.680	2.566	2.902	2.258				
12-hour	0.50	2.182	2.430	1.958	2.970	3.278	2.640				
24-hour	1.00	2.536	2.730	2.356	3.382	3.622	3.112				
2-day	2.00	2.926	3.136	2.722	3.832	4.096	3.548				
3-day	3.00	3.090	3.300	2.896	4.012	4.276	3.736				
4-day	4.00	3.262	3.466	3.068	4.200	4.462	3.930				
7-day	7.00	3.832	4.058	3.622	4.852	5.130	4.560				
10-day	10.00	4.328	4.568	4.110	5.408	5.700	5.108				
20-day	20.00	5.910	6.210	5.626	7.222	7.508	6.856				
30-day	30.00	7.282	7.650	6.922	8.776	9.226	8.326				

Graphs for 10-year and 50-year storm events are presented in Attachments 5 and 6 respectively.

8.0 CONCLUSIONS

As stated above, the volumes calculated in Sections 6.1 and 6.2 were for the 10-Year, 24-hour storm duration with an average depth. The same process shown within the calculation was used to calculate various durations ranging from 6 hours to 30 days for the 10- and 50-year storm events. A table outlining these volumes for 10- and 50-year storm durations can be found in Attachments 3 and 4. Graphs outlining calculated rainfall volumes into the BAP for the high, average, and low depths of the rainfall amounts for each of the storm durations are shown in Attachment 5 and 6 for the 10- and 50-year storm events, respectively.



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As shown on Attachments 3 and 4, the largest storm event evaluated within Section 2.1 per 40 CFR 423.13(k)(2)(i)(A) was the 50-year, 30-day storm. This storm event was then used along with the surface areas that contribute to the south BAP to calculate the runoff volume for the 50-year, 30-day storm event. The south BAP was sized to contain a 1/2-PMP (Probable Maximum Precipitation) event of 16.5 inches within 24 hours to meet State of Ohio regulatory requirements for earthen dams and that volume envelopes the runoff volume generated during this 50-year, 30-day storm event, which would allow the Plant to not discharge from the south BAP during each of the stormwater events evaluated up to the 50-year, 30-day event.

9.0 REFERENCES

- National Oceanic and Atmospheric Administration (NOAA) Atlas 14, Volume 2, Version 3, Point Frequency Data Server, Location name: Brilliant, Ohio, USA.
- 2 Cardinal Operating Company, Cardinal Plant, Calculation No. CRD-BAP-C-002, Revision 0, Hydrology and Hydraulics Calculation for South Pond.
- 3 Cardinal Operating Company, Drawing No 301008, Revision A, FARI Cover and Stormwater Pond Projects, Civil General Notes, and Symbols.

Calc No. 2023-02951 Revision 0 Attachment 1 Pge 1 of 1



NOAA Atlas 14, Volume 2, Version 3 Location name: Brilliant, Ohio, USA* Latitude: 40.2527°, Longitude: -80.6526° Elevation: 729.28 ft** * source: ESRI Maps ** source: USGS



POINT PRECIPITATION FREQUENCY ESTIMATES

G.M. Bonnin, D. Martin, B. Lin, T. Parzybok, M.Yekta, and D. Riley NOAA, National Weather Service, Silver Spring, Maryland

PF tabular | PF graphical | Maps & aerials

PF tabular

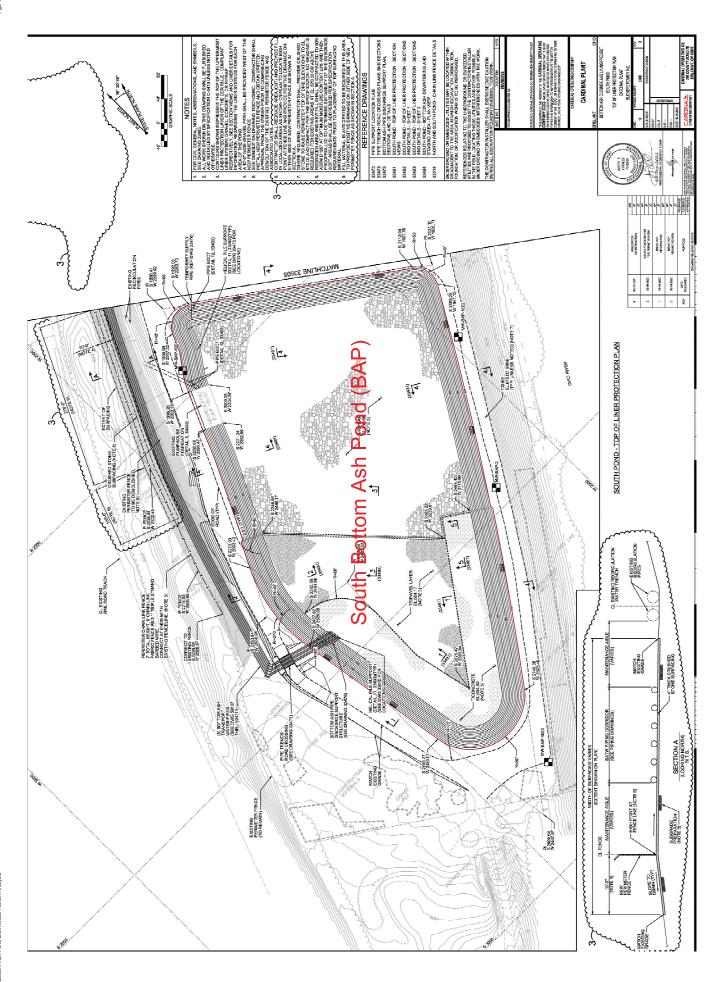
PDS-based point precipitation frequency estimates with 90% confidence intervals (in inches) ¹										
	- Buoou p	onit proof	pitation ii		ge recurrence			11101 11	<u> </u>	1100)
Duration	1	2	5	10	25	50	100	200	500	1000
5-min	0.320 (0.284-0.363)	0.382 (0.339-0.434)	0.463 (0.410-0.524)	0.524 (0.462-0.592)	0.603 (0.531-0.681)	0.663 (0.582-0.747)	0.720 (0.629-0.811)	0.779 (0.679-0.878)	0.858 (0.743-0.965)	0.915 (0.789-1.03)
10-min	0.497 (0.441-0.564)	0.597 (0.529-0.677)	0.719 (0.637-0.814)	0.808 (0.714-0.914)	0.922 (0.812-1.04)	1.00 (0.882-1.13)	1.08 (0.947-1.22)	1.16 (1.01-1.31)	1.26 (1.09-1.42)	1.33 (1.15-1.50)
15-min	0.610 (0.540-0.691)	0.730 (0.647-0.828)	0.883 (0.782-1.00)	0.994 (0.878-1.13)	1.14 (1.00-1.29)	1.24 (1.09-1.40)	1.35 (1.18-1.52)	1.45 (1.26-1.63)	1.57 (1.36-1.77)	1.67 (1.44-1.87)
30-min	0.807 (0.715-0.914)	0.977 (0.866-1.11)	1.21 (1.07-1.37)	1.38 (1.22-1.56)	1.61 (1.42-1.82)	1.78 (1.56-2.01)	1.94 (1.70-2.19)	2.11 (1.84-2.38)	2.33 (2.02-2.62)	2.50 (2.15-2.81)
60-min	0.985 (0.873-1.12)	1.20 (1.06-1.36)	1.52 (1.34-1.72)	1.76 (1.55-1.99)	2.09 (1.84-2.36)	2.34 (2.06-2.64)	2.60 (2.27-2.93)	2.87 (2.50-3.23)	3.23 (2.79-3.63)	3.51 (3.02-3.94)
2-hr	1.13 (0.995-1.30)	1.37 (1.21-1.58)	1.74 (1.52-1.99)	2.02 (1.77-2.31)	2.41 (2.10-2.75)	2.72 (2.37-3.11)	3.05 (2.64-3.46)	3.38 (2.92-3.84)	3.85 (3.29-4.36)	4.21 (3.58-4.78)
3-hr	1.20 (1.07-1.40)	1.46 (1.29-1.69)	1.84 (1.63-2.13)	2.14 (1.89-2.47)	2.56 (2.25-2.95)	2.90 (2.54-3.33)	3.25 (2.83-3.73)	3.63 (3.13-4.15)	4.14 (3.55-4.74)	4.55 (3.88-5.21)
6-hr	1.44 (1.29-1.64)	1.73 (1.54-1.97)	2.16 (1.93-2.46)	2.52 (2.24-2.86)	3.02 (2.67-3.42)	3.42 (3.01-3.87)	3.85 (3.37-4.35)	4.31 (3.75-4.85)	4.95 (4.26-5.56)	5.47 (4.67-6.13)
12-hr	1.70 (1.53-1.90)	2.03 (1.83-2.27)	2.52 (2.26-2.81)	2.91 (2.61-3.24)	3.49 (3.11-3.86)	3.96 (3.52-4.37)	4.47 (3.94-4.91)	5.00 (4.39-5.49)	5.77 (5.01-6.32)	6.40 (5.51-6.97)
24-hr	2.01 (1.88-2.18)	2.41 (2.24-2.60)	2.94 (2.74-3.18)	3.38 (3.14-3.64)	4.00 (3.70-4.30)	4.51 (4.15-4.83)	5.03 (4.62-5.39)	5.58 (5.10-5.97)	6.36 (5.77-6.79)	6.98 (6.30-7.44)
2-day	2.37 (2.21-2.54)	2.82 (2.63-3.03)	3.41 (3.19-3.67)	3.90 (3.63-4.18)	4.56 (4.24-4.89)	5.11 (4.73-5.46)	5.66 (5.23-6.05)	6.24 (5.73-6.65)	7.03 (6.42-7.49)	7.65 (6.95-8.15)
3-day	2.53 (2.38-2.71)	3.01 (2.83-3.22)	3.62 (3.40-3.87)	4.12 (3.86-4.40)	4.81 (4.49-5.12)	5.35 (4.98-5.70)	5.92 (5.49-6.30)	6.49 (6.00-6.90)	7.29 (6.69-7.74)	7.91 (7.22-8.40)
4-day	2.70 (2.55-2.87)	3.20 (3.02-3.41)	3.84 (3.61-4.08)	4.35 (4.09-4.62)	5.05 (4.73-5.36)	5.60 (5.24-5.95)	6.17 (5.75-6.55)	6.75 (6.27-7.16)	7.55 (6.96-7.99)	8.16 (7.49-8.66)
7-day	3.24 (3.07-3.43)	3.84 (3.63-4.06)	4.55 (4.30-4.82)	5.11 (4.83-5.41)	5.88 (5.54-6.21)	6.47 (6.08-6.84)	7.08 (6.64-7.48)	7.69 (7.18-8.12)	8.50 (7.90-8.98)	9.12 (8.44-9.64)
10-day	3.74 (3.55-3.94)	4.41 (4.18-4.66)	5.17 (4.91-5.46)	5.77 (5.48-6.09)	6.58 (6.23-6.94)	7.21 (6.81-7.60)	7.83 (7.38-8.26)	8.46 (7.95-8.92)	9.27 (8.67-9.78)	9.89 (9.21-10.4)
20-day	5.24 (4.99-5.50)	6.15 (5.86-6.48)	7.12 (6.78-7.49)	7.88 (7.50-8.28)	8.88 (8.43-9.32)	9.63 (9.14-10.1)	10.4 (9.81-10.9)	11.1 (10.5-11.7)	12.0 (11.3-12.6)	12.7 (11.9-13.4)
30-day	6.57 (6.26-6.92)	7.69 (7.32-8.11)	8.82 (8.40-9.29)	9.71 (9.23-10.2)	10.9 (10.3-11.4)	11.7 (11.1-12.3)	12.6 (11.9-13.2)	13.4 (12.6-14.1)	14.4 (13.6-15.2)	15.2 (14.2-16.0)
45-day	8.41 (8.03-8.80)	9.81 (9.37-10.3)	11.1 (10.6-11.6)	12.1 (11.6-12.7)	13.4 (12.8-14.0)	14.3 (13.7-15.0)	15.2 (14.5-15.9)	16.1 (15.3-16.8)	17.1 (16.2-18.0)	17.8 (16.9-18.7)
60-day	10.1 (9.72-10.6)	11.8 (11.3-12.3)	13.2 (12.7-13.8)	14.3 (13.7-15.0)	15.7 (15.1-16.4)	16.7 (16.0-17.5)	17.7 (16.9-18.4)	18.5 (17.7-19.3)	19.6 (18.6-20.4)	20.3 (19.3-21.2)

¹ Precipitation frequency (PF) estimates in this table are based on frequency analysis of partial duration series (PDS).

Numbers in parenthesis are PF estimates at lower and upper bounds of the 90% confidence interval. The probability that precipitation frequency estimates (for a given duration and average recurrence interval) will be greater than the upper bound (or less than the lower bound) is 5%. Estimates at upper bounds are not checked against probable maximum precipitation (PMP) estimates and may be higher than currently valid PMP values.

Please refer to NOAA Atlas 14 document for more information.

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Attachment 3: Runoff Volume (ac-ft) For 10-Year Storm Event South BAP

Description	Urainage Area (ac)	Runoff Coefficient	Rainfall Bound				10-Ye	ear Rainfall	10-Year Rainfall Depth (d) Inches	ches			
	(A)	(c)		6-Hour	12-Hour	24-Hour	2-day	3-day	4-day	7-day	10-day	20-day	30-day
			Average	2.52	2.91	3.38	3.90	4.12	4.35	5.11	5.77	7.88	9.71
Rainfall			High	2.86	3.24	3.64	4.18	4.40	4.62	5.41	60.9	8.28	10.20
			Low	2.24	2.61	3.14	3.63	3.86	4.09	4.83	5.48	7.50	9.23
			Average	1.449	1.673	1.944	2.243	2.369	2.501	2.938	3.318	4.531	5.583
Area 1: South Bottom Ash Pond	06.90	1.00	High	1.645	1.863	2.093	2.404	2.530	2.657	3.111	3.502	4.761	5.865
			Low	1.288	1.501	1.806	2.087	2.220	2.352	2.777	3.151	4.313	5.307
			Average	0.441	0.509	0.592	0.683	0.721	0.761	0.894	1.010	1.379	1.699
Area 2: Peripheral Road to South BAP	2.10	1.00	High	0.501	0.567	0.637	0.732	0.770	608.0	0.947	1.066	1.449	1.785
			Low	0.392	0.457	0.550	0.635	0.676	0.716	0.845	0.959	1.313	1.615
			Average	1.890	2.182	2.536	2.926	3.090	3.262	3.832	4.328	5.910	7.282
Total South BAP	9.00	1.000	High	2.146	2.430	2.730	3.136	3.300	3.466	4.058	4.568	6.210	7.650
			Low	1.680	1.958	2.356	2.722	2.896	3.068	3.622	4.110	5.626	6.922

Note:

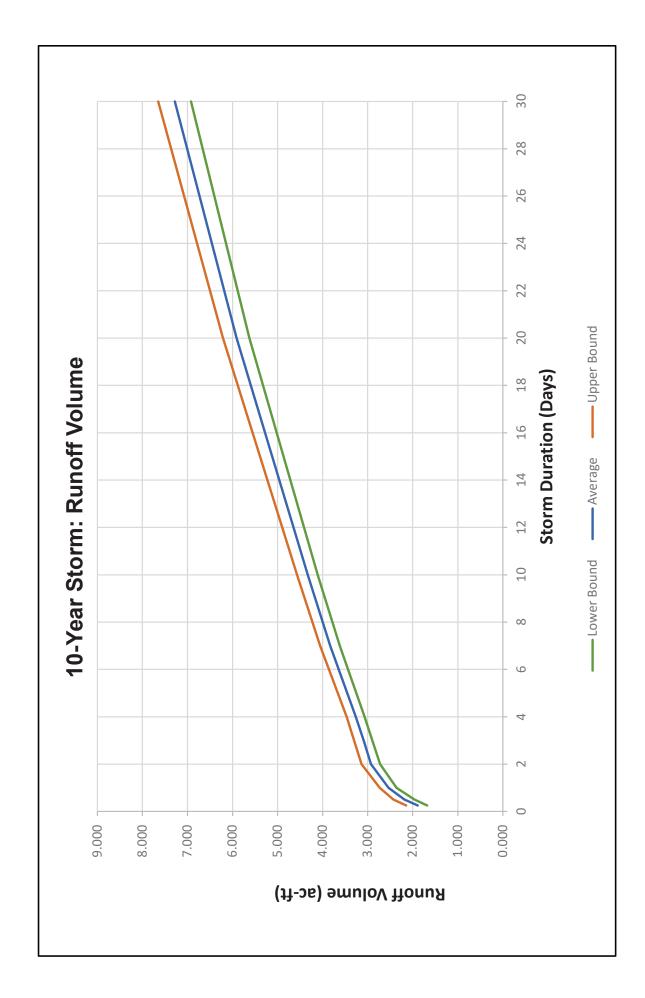
Runoff Volumes in ac-ft and rounded to three decimal

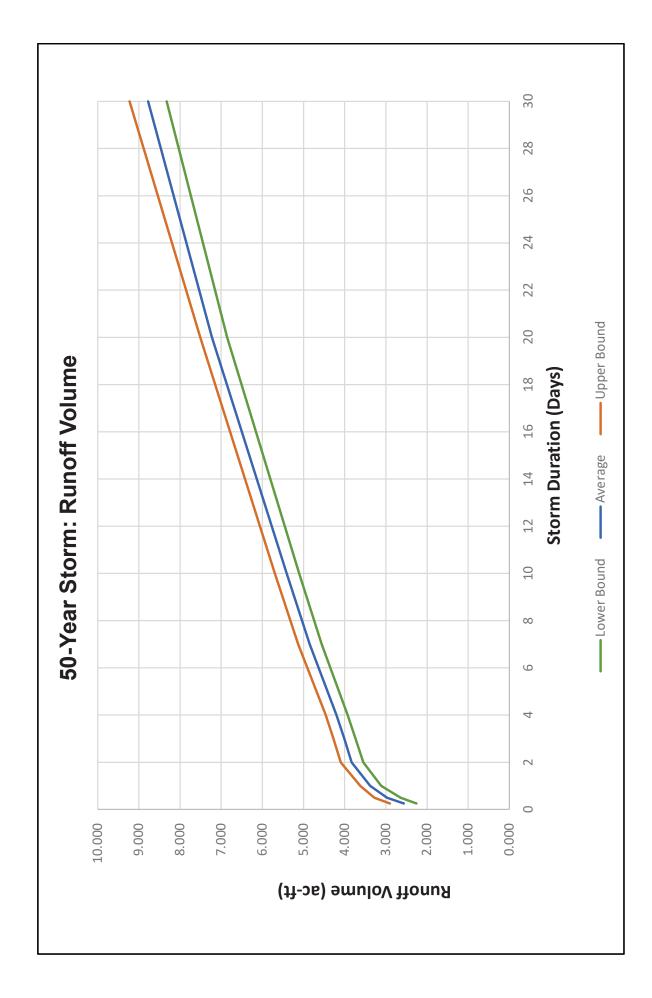
Attachment 4: Runoff Volume (ac-ft) For 50-Year Storm Event South BAP

Cocinitation	Drainage Area (ac)	Runoff Coefficient	Rainfall Round				10-Ye	10-Year Rainfall Depth (d) Inches	Depth (d) In	ches			
	(A)	(c)		6-Hour	12-Hour	24-Hour	2-day	3-day	4-day	7-day	10-day	20-day	30-day
			Average	3.42	3.96	4.51	5.11	5.35	5.60	6.47	7.21	9.63	11.70
Rainfall			High	3.87	4.37	4.83	5.46	5.70	5.95	6.84	7.60	10.01	12.30
			Low	3.01	3.52	4.15	4.73	4.98	5.24	80.9	6.81	9.14	11.10
			Average	1.967	2.277	2.593	2.938	3.076	3.220	3.720	4.146	5.537	6.728
Area 1: South Bottom Ash Pond	06.9	1.00	High	2.225	2.513	2.777	3.140	3.278	3.421	3.933	4.370	5.756	7.073
			Low	1.731	2.024	2.386	2.720	2.864	3.013	3.496	3.916	5.256	6.383
			Average	0.599	0.693	0.789	0.894	0.936	0.980	1.132	1.262	1.685	2.048
Area 2: Peripheral Road to South BAP	2.10	1.00	High	0.677	0.765	0.845	0.956	0.998	1.041	1.197	1.330	1.752	2.153
			Low	0.527	0.616	0.726	0.828	0.872	0.917	1.064	1.192	1.600	1.943
			Average	2.566	2.970	3.382	3.832	4.012	4.200	4.852	5.408	7.222	8.776
Total South BAP	00.6	1.000	High	2.902	3.278	3.622	4.096	4.276	4.462	5.130	5.700	7.508	9.226
			Low	2.258	2.640	3.112	3.548	3.736	3.930	4.560	5.108	6.856	8.326

Note:

Runoff Volumes in ac-ft and rounded to three decimal









CARDINAL GENERATING STATION

BOTTOM ASH TRANSPORT SYSTEM EVALUATION

Issue: Rev. 0, For Use Date: October 9, 2023 Project No. A13770-006

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APPENDIX C.

BOTTOM ASH PURGE WATER SUSPENDED SOLIDS ESTIMATE

Buckeye Power Cooperative

Cardinal Generating Station, Unit 1,2,&3

Document Number: 2023-02785 Bottom Ash Purge Water Suspended Solids Estimate

Rev. 0 August 15, 2023





ISSUE SUMMARY

Form SOP-0402-07, Revision 15

			DESIGN C	ONTROL SUMMARY							
CLIENT:		Buckeye Power Cooperative			UNI	T & NO.: 1,2,&3	3			Page No.:	2
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Bottom Ash Purge Water Suspended Solids Estimate

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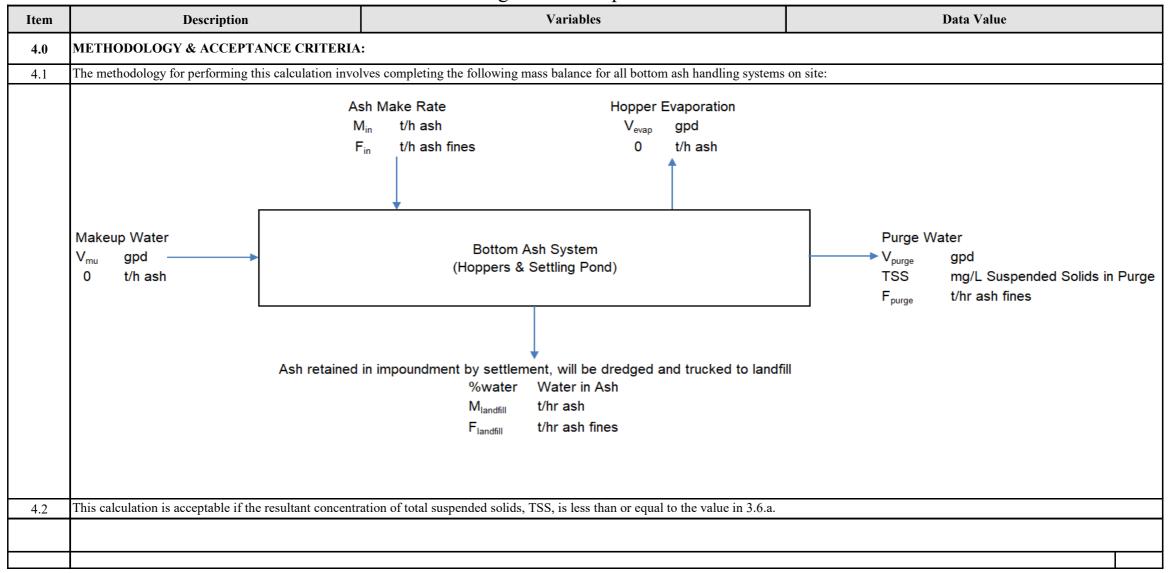


Bottom Ash Purge Water Suspended Solids Estimate

1.00	PURPOSE AND SCOPE:				
1.01	The Cardinal Generating Station is a coal fired unit lo	cated in Brilliant, OH			
1.02		n ash purge water discharge to maintain TSS concentration SS samples. TSS concentration will be maintained at or b			on damage
Item	Description	Reference	Unit of Measure	Data Value	Input (V/UV/ EJ)
2.0	DESIGN INPUTS:				
2.1	Bottom Ash Handling System Inputs				
2.1.a	Unit 1 ash make rate, M _{in1}	Bottom Ash Closure and Lining Project Design Basis,	t/hr	4.2	UV
2.1.b	Unit 2 ash make rate, M _{in2}	-CAR-DB-0002, Rev 0	t/hr	4.2	UV
2.1.c	Unit 3 ash make rate, M _{in3}	-C/IR DD 0002, Rev 0	t/hr	4.8	UV
2.1.d	Primary Active Wetted Bottom Ash System Volume, V	2020-03682, Wetted Bottom Ash Transport Water Volume Estimate	gallons	657,345	V
2.3	Bottom Ash Particle Size Distribution				
2.3.a	Fraction of bottom ash particles <75 µm, %fines	EPA-600/7-80-067, Table 8, pg 38	%wt	1.8%	UV
2.4	Bottom Ash System Purge Water Total Suspended So				
2.4.a	Fines concentration to protect bottom ash system pumps from excessive abrasion damage based upon ash water recirculation pump discharge TSS samples, TSS	99% confidence interval of Ash Water Recycle Pump Discharge Water Quality total suspended solids data, October 25, 2022 through July 19, 2023.	mg/L	19.7	UV
Item	Description ASSUMPTIONS:	Reference	Unit of Measure	Data Value	
3.0		settled in the settlement pond is assumed based upon reulation pumps, %removed	%	99.95%	EJ
3.2		r evaporated from the hopper and dewatering bins, V_{evap}			EJ
3.3	Evaporation from hopper and bottom ash pond based on previous project experience prorated by unit nameplate MW, V _{evap}	N/A	gpd	2995	EJ
3.4		from the ash south pond. This amount of water, when ave	eraged over the life of the p	lant, is considered negligible.	EJ
3.5	All particles other than fines are completely removed	by settlement in the bottom ash pond			EJ
1					



Bottom Ash Purge Water Suspended Solids Estimate





Bottom Ash Purge Water Suspended Solids Estimate

Item	Description	Reference	Unit of Measure	Equation	
5.0	CALCULATIONS:		•	•	
5.1	Input of ash into system, M _{in}		t/hr	$M_{in} = (M_{in1} + M_{in2} + M_{in3})$	
	Cardinal Units 1, 2, & 3		t/hr	13.2	
5.2	Input of fines into system, F _{in}		t/hr	$F_{in} = M_{in} x \% fines$	
	Cardinal Units 1, 2, & 3		t/hr	0.24	
5.3	Fines included in the bottom ash purge water, F_{purge}		t/hr	$F_{purge} = F_{in} \times (1-\% removed)$	
	Cardinal Units 1, 2, & 3		t/hr	0.00012	
5.4	Concentration of suspended solids in bottom ash purge water, recirculating water, and water entrained in ash to landfill, TSS.		mg/L	$TSS = F_{purge} / (V_{purge} / (2000 \times 24) \times 8.338) \times 1,000,000$	00
	Cardinal Units 1, 2, & 3		mg/L	20	
5.5	Bottom ash purge water flow, V _{purge}		gpd	$V_{purge} = (F_{purge} / TSS) \times 10^6 \times 2000 \times 24 / 8.338$	
	Cardinal Units 1, 2, & 3		gpd	34690.4	
5.6	Average fraction of primary wetted volume discharged per day, %PVW		%	$% PVW = V_{purge} / V$	
	Cardinal Units 1, 2, & 3		%	5.3%	
Item	Description	Reference	Unit of Measure	Equation	Accept (Y/N)
6.0	RESULTS:				
6.1	30-day rolling average discharge of bottom ash purge concentration in Combined Unit 6 bottom ash system,	water from bottom ash system required to control fines %PWV	%PWV/day	5.3%	YES
7.0	REFERENCES:	0.65			
7.1	Program No. 03.2.435-16.0, Microsoft Excel for Offic Bottom Ash Volume Calculation, 2021-03195	2 365			
7.3		h Particles in Water: Trace Metal Leaching and Ash Settl	inσ		
7.4	Bottom Ash Closure and Lining Project Design Basis	<u> </u>	5		
		,			
8.0	ATTACHMENTS:				
8.1	AWRP discharge water quality data, October 25, 2022	through July 19, 2023.			



Bottom Ash Purge Water Suspended Solids Estimate Attachment 8.1: Ash Water Recirculation Pump Water Quality Data

Data	TSS
Date	
10/25/2022	10
11/15/2022	10
11/29/2022	21.5
12/14/2022	19
12/21/2022	12
1/5/2023	7.5
1/9/2023	4
1/16/2023	11.5
1/23/2023	8
2/1/2023	7
2/9/2023	4.5
2/16/2023	6
2/22/2023	7.5
3/2/2023	8.5
3/8/2023	3.5
3/16/2023	5.5
3/23/2023	12
4/3/2023	13
5/2/2023	9
6/2/2023	7.5
7/19/2023	5.5
Min	3.5
Average	9.2
Max	21.5
99% CL	19.7



CARDINAL GENERATING STATION

BOTTOM ASH TRANSPORT SYSTEM EVALUATION

Issue: Rev. 0, For Use Date: October 9, 2023 Project No. A13770-006

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APPENDIX D.

CHART FROM EPA "BEHAVIOUR OF COAL ASH PARTICLES IN WATER: TRACE METAL LEACHING AND ASH SETTLING"

EPA-600/7-80-067, MARCH 1980, PG 17

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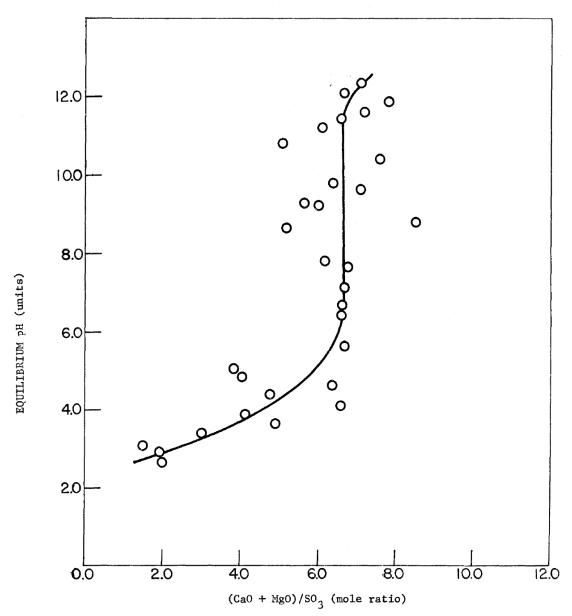


Figure 2. Relationship between the equilibrium pH of ash/water mixture and the mole ratio of CaO plus MgO to ${\rm SO_3}$ contained in dry fly ashes.